

THERMODYNAMIC MODELING OF THE SRS EVAPORATORS: PART IV. INCORPORATION OF HIGH CAUSTIC ALUMINOSILICATE SOLUBILITY DATA (U)

C. M. Jantzen, J.M. Pareizs, and T.B. Edwards

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EXECUTIVE SUMMARY

Accumulations of two solid phases (a nitrated aluminosilicate) and sodium diuranate, in the form of scale, caused the SRS 2H Evaporator pot to become completely inoperable in October 1999. The accumulation of the sodium diuranate phase, which selectively precipitated with the aluminosilicate phase, caused criticality concerns in the 2H Evaporator. In order to understand the role of steady state saturation on the scale formation, solutions processed from the SRS 2H, 2F, and 3H Evaporators were evaluated with a commercially available thermodynamic equilibrium code known as Geochemist's Workbench (GWB).

Reactive oxides, soluble silicates, and soluble aluminates in caustic solution can form a sodium aluminosilicate gel (NAS_{gel}) at ambient temperature when the solution stoichiometry of the aluminate and silicate species is ~1:1. The NAS_{gel} converts to Zeolite-A under hydrothermal conditions similar to those existing in the SRS evaporators. The nitrated-cancrinite/sodalite formed in the SRS 2H Evaporator was found to have formed from NAS_{gel} and Zeolite-A. Zeolite-A and hydroxysodalite formation from NAS_{gel} has also been observed in evaporators used in the wood pulp industry while formation of NAS_{gel} and transformation into Zeolite-A→sodalite→cancrinite has been observed in the Bayer aluminum process. Solubility data for NAS_{gel} , Zeolite-A, nitrated sodalite, and nitrated cancrinite in SRS high caustic solutions containing nitrate, nitrite and excess $\text{Al}(\text{OH})_4^-$ were recently generated for SRS by researchers at the University of Southern Australia. The new solubility data have been incorporated into the process control model for the SRS evaporators and documented in this study.

The potential to form the NAS_{gel} phase in the evaporator was modeled because this phase is the primary phase from which all the other aged crystalline product species are derived. In addition, the formation of the NAS_{gel} phase is kinetically the most rapid step in the formation sequence [species in solution]→ NAS_{gel} →Zeolite-A→sodalite→cancrinite. Modeling the denser crystalline phases, which are more thermodynamically stable but less soluble than the NAS_{gel} , would unnecessarily constrict the solution chemistry range of the SRS evaporators. New kinetic data developed by researchers at the Pacific Northwest National Laboratory are shown to validate the use of the NAS_{gel} precursor phase as the basis for the process control modeling.

Nominal and expanded evaporator process control models are presented in this study based on calculated NAS_{gel} supersaturations performed using Geochemist's Workbench. The nominal process control model covers the last 7 years of SRS evaporator operation over a narrower composition range than the expanded model. The nominal evaporator model assumes a nominal 40% evaporation (defined as 40% loss of the weight of water) at operating temperature ranges of 120-140°C. The sensitivity of the nominal model to temperature is shown to be minimal while the sensitivity to evaporation is somewhat greater. The expanded evaporator process control model covers the wider tank farm compositional region expected to be processed in the future for the following types of evaporator operating conditions:

- 0-80 wt % evaporation
- 100°C to 180°C

Both the nominal and the expanded process models are based on solubility data of the NAS_{gel} phase determined by researchers at the University of Southern Australia. The new solubility data were carefully determined in simulated SRS evaporator solutions including the following:

- solid products were “quenched” and chemically analyzed
- solutions varied from 6M to 12M caustic
- runs were reversed to demonstrate that equilibrium had been achieved
- once the solubility data were entered into Geochemist’s Workbench, $\log(Q/K)_{\text{NAS}}$ values were calculated for the solutions at various temperatures and concentrations; values of ~0 verified that equilibrium had, indeed, been achieved

The stoichiometry of the NAS_{gel} phase is $\text{Na}_{12}\text{Al}_{12}\text{Si}_{12}\text{O}_{48} \bullet 27\text{H}_2\text{O}$ in the high caustic SRS simulated evaporator solutions and not $\text{Na}_{12}\text{Al}_{12}\text{Si}_{14}\text{O}_{52} \bullet 31\text{H}_2\text{O}$ used in previous models developed based on the data from the Bayer aluminium industry. The NAS_{gel} was more soluble in the simulated high caustic SRS evaporator solutions than the Bayer solutions. The use of the newly generated solubility data demonstrated that the previous evaporator process control models had underestimated the importance of the OH^- term in modeling due to this enhanced solubility.

The revised nominal process control model was derived which takes the form of

$$\log(Q/K)_{\text{NAS } 120-140^\circ\text{C} / 40\% \text{ evap}} = \frac{37.4848 + 1.0949(12\log[\text{Al}(M)] + 12\log[\text{Si}(M)])}{-12\log[\text{OH}(M)]}$$

Where $\log(Q/K)_{\text{NAS } 120-140^\circ\text{C} / 40\% \text{ evap}}$ on the LHS of the equation is the supersaturation that will be experienced in the evaporator pot between 120-140°C after a 40% evaporation of water from an evaporator solution. The compositional dependencies of the initial solution concentrations to the 40% evaporation are represented by the parameters on the RHS of the equation, which are measurements taken at room temperature before evaporation. The RHS of the nominal process control model in () is hereafter referred to as $\log Q(\text{NAS})_{25^\circ\text{C}}$. Thus, the LHS of the equation represents saturation in the evaporator after a given percent evaporation and the RHS of the equation represents the feed tank chemistry.

The nominal process control model is based on SRS evaporator feed tank data analyzed only at SRTC and is validated using an Orthogonal Latin Hypercube (OLH) statistical design of simulated evaporator solutions. The OLH for validation of the statistical process control is performed in molar composition space since the solution compositions being modeled exhibited a Gaussian distribution over the 7 year time period (1995-2002) being modeled. The OLH design created some unrealistic combinations of evaporation and sodium content. For example, the OLH may have an evaporation of 40% for a starting sodium content of 16 M. This evaporation would yield an unachievable high final sodium concentration. Therefore, a screening tool was developed to eliminate these unrealistic combinations, e.g. $\text{Max Evap} = 1 - \frac{\text{Na}(M)}{19}$, where $\text{Na}(M)$ is the initial sodium content before evaporation.

Equations similar to the nominal process control model can be derived for various combinations of operating temperature and percent evaporation. When these equations are solved at $\log(Q/K) = 0$, which represents saturation with respect to NAS_{gel} , a family of $\log Q(NAS)_{25^\circ C}$ values are derived and the relationship between the tank chemistry ($\log Q(NAS)_{25^\circ C}$), operating temperature and percent evaporation takes the form

$$\log Q(NAS)_{25^\circ C} = -32.1114 - 0.1119(\% \text{Evaporation}) + 0.0165(\text{Operating Temp } ^\circ C)$$

$$\text{where } \log Q(NAS)_{25^\circ C} = (12\log[Al(M)] + 12\log[Si(M)] - 12\log[OH(M)])$$

The coefficients in this equation demonstrate that evaporation and operating temperature have opposite effects. Increased evaporation causes decreased solubility of components while increased temperature causes increased solubility of components. In addition, the coefficients demonstrate that evaporation is a factor of 10 more significant than operating temperature. Due to the insignificance of the temperature term, and the fact that higher temperature causes increased solubility of components, the temperature term can be eliminated from the above equation, which then becomes:

$$\log Q(NAS)_{25^\circ C} = -29.9434 - 0.1092 (\% \text{Evaporation})$$

The above relation between $\log Q(NAS)_{25^\circ C}$ and percent evaporation can be used to control scaling in the SRS evaporators at a variety of temperatures if the percent evaporation can be monitored. However, this process control approach is only valid over the compositional range of solutions modeled, e.g. the historic composition range experienced between 1995 and 2002.

An expanded process control model was developed using an OLH lognormal experimental design since the composition space over the historic 28 year operational period of the tank farm (1973-2002) indicated a lognormal distribution. As with the OLH validation experimental design, the screening tool was applied to eliminate unrealistic combinations. Half of the remaining 401 data points, randomly chosen, were used to develop the expanded process control model and the remaining half were used for validation. The expanded process control model takes the form

$$\log(Q/K)_{NAS} = \frac{9.8691 + 13.04\log[Al(M)] + 11.09\log[Si(M)] - 13.51}{\log[OH(M)] + 15.84Density + 0.0163Temp(^{\circ}C)}$$

The usage of the expanded process control model does not entail monitoring of the percent evaporation since the fitted coefficients of $\log Al(M)$, $\log Si(M)$, $\log OH(M)$, density, and operating temperature compensate for the missing parameter because they are all related to percent evaporation.

Both the nominal and the expanded process control models have coefficients for the $\log Al(M)$, $\log Si(M)$, and $\log OH(M)$ that are close to the parameters 12:12:-12 developed from the

thermodynamic equation governing the phase boundary between NAS_{gel} and AlOOH which in turn is governed by the stoichiometry of the NAS_{gel} :



When the expanded process control model is related to the past 7 years of SRS evaporator operating history it demonstrates that normal operation has been at $\log(Q/K)_{\text{NAS}} < 0$ in the undersaturated NAS_{gel} region, e.g. values in the -15 to -10 range for the 2H evaporator when it was not scaling and for the 2F and 3H evaporators, historically. $\log(Q/K)_{\text{NAS}}$ has been in the -7 to -5 range for recent 3H evaporator operation.

Therefore, a $\log(Q/K)_{\text{NAS}} < 0$ process control limit can be set for implementation of the expanded process control model based on operational history or a process control limit of $\log(Q/K)_{\text{NAS}} = 0$ can be implemented except during process upset conditions. The limit of $\log(Q/K)_{\text{NAS}} = 0$ separates the 7 years (1995-2002) of SRS Evaporator operation modeled into two populations, hereafter referred to as “normal operation” and “process upset operation.”

Operation “just at saturation,” e.g. $\log(Q/K)_{\text{NAS}} = 0$, is an attractive approach because of the following:

- silicate solutions can be >200% supersaturated at a given elevated temperature and not precipitate until the solutions are cooled
- precipitation of NAS_{gel} historically only occurred during process upset conditions, e.g. when the feed pump for the 2H evaporator was in the Zone of Turbidity (ZOT) and the evaporator was receiving frequent silica rich frit SME carryovers from DWPF

This demonstrates that it is only necessary to control at $\log(Q/K)_{\text{NAS}} < 0$ if there are known process upsets that could cause increased Si such as the following:

- evaporator feeds exposed to silica rich frit carryovers from the DWPF Slurry Mix Evaporator
- evaporator feeds pumped when the feed pump was too close to the sludge or in the Zone of Turbidity (ZOT) as defined in Parts I and II of this study
- evaporator feeds containing high silica and/or zeolite seeds such as the HEME/HEPA digests from DWPF
- sludge wash water that may contain elevated levels of silica from degradation of IE-95 resin which liberates 11 moles of SiO_2 for every mole of degraded resin, e.g. Tank 19 or Tank 18 wash water

Control at $\log(Q/K)_{\text{NAS}} = 0$ allows credit to be taken for keeping the feed pumps 40” above the sludge or 20” above the ZOT, so that receipt of silica rich material from the ZOT cannot occur. Due to stratification of the chemistry in the tanks, samples for process control should be taken at the height of the feed pump in feed tanks or at variable depths in tanks about to be qualified as evaporator feed.

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LIST OF ACRONYMS

ACT-2:	ACTivity Diagram Subroutine in GWB
DOE:	United States Department of Energy
GDL:	Gravity Drain Line
GWB:	The Geochemist's Workbench Software
HLW:	High Level Waste
LHS:	Left Hand Side
LLNL:	Lawrence Livermore National Laboratory
NAS:	Sodium Aluminosilicate gel
OLS:	Ordinary Least Squares
OLH:	Orthogonal Latin Hypercube
ORNL:	Oak Ridge National Laboratory
PNNL:	Pacific Northwest National Laboratory
REACT:	Reaction Path Subroutine in GWB
RHS:	Right Hand Side
RMSE:	Root Mean Square Error
RW-0333P:	DOE Level of Quality Assurance
SME:	Slurry Mix Evaporator
SRS:	Savannah River Site
SRTC:	Savannah River Technology Center
TDS:	Total Dissolved Solids
TTT:	Time-Temperature-Transformation
USA:	University of Southern Australia
VDS:	Variable Depth Samples
WSRC:	Westinghouse Savannah River Company
ZOT:	Zone of Turbidity

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1.0 INTRODUCTION

Accumulations of two solid phases (nitrated aluminosilicates^f and sodium diuranate^{*}) formed scale deposits in the Savannah River Site (SRS) 2H Evaporator system.^{1, 2} The sodium aluminosilicate (NAS) scale deposits caused the evaporator pot to become inoperable in October 1999. Accumulations of the diuranate phase have caused criticality concerns in the SRS 2H Evaporator. In Part I of this study,³ thermodynamically derived activity diagrams, also known as stability diagrams, were used on historic 2H feed tank (Tank 43) and drop tank (Tank 38) chemistries in order to understand the effects of tank chemistry on solids formation in the 2H Evaporator system. Evaluation of the 2F feed tank (Tank 26) and drop tank (Tank 46) chemistries evaluated in Part I of this study showed that the SRS 2F Evaporator system had not and was not near saturation with respect to aluminosilicate scale. In order to ensure that similar deposits had not and were not depositing in the SRS 3H Evaporator system, a similar evaluation was performed specific to the feeds processed from Tank 32 (feed tank) and Tank 30 (drop tank) in Part II of this study.⁴

A commercially available computer code, Geochemist's Workbench (GWB), was modified to include solubility data for species found in SRS evaporators in high ionic strength solutions. Activity diagram representation was used to evaluate whether an evaporator feed tank composition fell in the formation (stability) field of the undesirable aluminosilicate species, e.g. was a given evaporator solution saturated or supersaturated with respect to the undesirable aluminosilicate species that caused scaling. The operational history of all the SRS evaporators was shown to coincide with the phase fields on the activity diagrams. The SRS 2H Evaporator was inoperable and scaled periodically when the solutions fed to the evaporator were saturated with respect to the sodium aluminosilicate gel (NAS_{gel}) phase. The SRS 2H, 2F, and 3H Evaporators were operational as long as the solutions being processed were saturated with respect to aluminum hydroxide phases such as gibbsite ($\text{Al}(\text{OH})_3$) or diasporite (AlOOH), since the kinetics of formation of the aluminum hydroxides is on the order of 2 weeks while the evaporator residence times are on the order of 8-12 hours.

^f a mixture of nitrated cancrinitite, $\text{Na}_8\text{Al}_6\text{Si}_6\text{O}_{24}(\text{NO}_3)_2 \bullet 4\text{H}_2\text{O}$, and nitrated sodalite, $\text{Na}_8\text{Al}_6\text{Si}_6\text{O}_{24}(\text{NO}_3)_2$

* $\text{Na}_2\text{U}_2\text{O}_7$

Modeling the deposition of the aluminosilicates and sodium diuranate in the SRS evaporators entailed calculations in the complex Na-N-Si-Al-U-H₂O system at elevated temperatures and at high ionic strengths (I~8.5). Modeling accuracy was evaluated against the following parameters:

- quality of the chemical data available from the feed and drop tanks
- how representative the analytic dip samples from the feed tank are of the feed actually entering the evaporator due to tank chemistry stratification
- the quality of the solution density approximations used to convert from molar to molal units
- quality of the approximations that must be made to determine the activity coefficients for high ionic strength solutions.

The quality of the solution density approximations is discussed in Appendix A. The quality of the approximations made to determine the activity coefficients are discussed in Part I of this study.³ The quality of the chemical data available for the SRS 2H and 2F Evaporators between 1992 and 2000 is also discussed in Part I³ while the quality of the chemical data for the SRS 3H Evaporator for the same time period is discussed in Part II.⁴ The quality of tank data analyzed between 2001 and 2002 is discussed in Part III.⁵ The quality of all the data used in the development of a process control model is discussed in this study (Part IV).

A process control strategy was developed in Part I of this study³ to relate the ambient temperature chemistry in an evaporator feed tank to the saturation of that feed in the evaporator pot at elevated temperature during a nominal 40 wt % evaporation. In Part III⁵ of this study the usage of the process control strategy was expanded to various temperatures (120-180°C) and evaporations (0-60%) based on the extrapolated (from 4M NaOH to 8M NaOH) solubility data of Bayer aluminum industry liquors⁶ and wood pulp industry liquors.⁷

In this study (Part IV) the process control approach is modified from that presented in Parts I,³ II,⁴ and III⁵ of this study as follows:

- solubilities of all of the sodium aluminosilicate phases (NAS_{gel}, Zeolite-A, nitrated sodalite and nitrated cancrinite) as measured by Mensah et. al.⁸ in simulated SRS Evaporator liquors from 3-12M NaOH are added to the GWB database replacing the aluminosilicate solubility data from the Bayer aluminum industry and the data from the wood pulp industry (see Appendix B and Part V⁹)
- the analyzed SRS evaporator feed tank data are used to develop a nominal process control model at 40% evaporation and operation between 120-140°C
 - the form of the model, in terms of solution chemistry, is shown to be dependent on the stoichiometry of the NAS_{gel} phase as shown in Parts I, II, and III of this study
 - variable depth sample data analyzed at SRTC are used exclusively in modeling
 - F-Area laboratory data were shown to be biased high with respect to Si due to high dilution of the solutions being analyzed^{3,4}

- F-Area laboratory data were shown to be biased low with respect to Al since detection limit values were being measured when high Al canyon waste was being fed³
- the drop tank data are shown to be lower in concentration with respect to the feed tank data since salts such as NaNO₃, NaAlO₂, and aluminosilicates crystallize in the drop tank
- the process control model derived in Part I and Part III is shown to underestimate the importance of the OH⁻ concentration since the newly measured solubility of the NAS phases is shown to be a strong function of the OH⁻ concentration⁸
- the nominal process control model is validated using a set of statistically designed orthogonal latin hypercube (OLH) simulated evaporator solutions which lie within the compositional range of the tank data modeled in this study
- the effects of variations in temperature and evaporation are demonstrated on the nominal process control model using the SRS feed tank data measured by SRTC
- an expanded process control model is developed to include evaporations between 0% and 80% and temperatures between 120-180°C based on a set of statistically designed orthogonal latin hypercube (OLH) solutions which lie within the broader compositional range of the tank data being considered for future processing in the SRS 2F and 3H evaporators
 - the process control model can then be expressed as a function of the solution concentrations (log[Al], log[Si], log[OH]) in the tank, operating temperature of the evaporator, and final percent evaporation
 - alternatively the process control model can be expressed as a function of the solution concentrations (log[Al], log[Si], log[OH]) in the tank, operating temperature of the evaporator, and final evaporator liquor density
 - the form of the model, in terms of solution chemistry, is dependent on the stoichiometry of the NAS_{gel} phase consistent with the process models developed in Parts I, II, and III of this study
 - the expanded OLH process model is then tied to SRS evaporator operating history

Validation of the GWB calculational approach in simple one component systems and in the complex Na-N-Si-Al-U-H₂O system, based on the new aluminosilicate solubility data,⁸ is discussed in Part V⁹ of this study. The validation of the basis for the SRS evaporator process control model, the activity diagrams, is also discussed in Part V⁹ of this study.

2.0 BACKGROUND

2.1 Operation of SRS Evaporators

For ~40 years, the SRS tank farm evaporators have run with only occasional operational problems, e.g., salt (NaNO_3) buildup has caused difficulty in draining evaporators but these deposits are water soluble and easily removed by flushing with hot water. The SRS 2F and 3H Evaporators continue to operate with only occasional salt buildup. However, operation of the SRS 2H evaporator had become problematic due to the formation of aluminosilicate scale between 1997 and 1999.

A new 2H Evaporator pot was installed and began receiving waste in January 1996. From mid 1996 until August 1997 the SRS 2H Evaporator was increasingly hard to control. When the evaporator was shut down in August 1997 for cleaning, deposits of the sodium aluminosilicate and sodium uranate phases were found in the gravity drain line (GDL).¹⁰ The GDL was pressure washed in the direction of the drop tank. The line remained clean and the evaporator showed minimal deposits on the walls or in the lines from August 1997 to June 1998. In June 1998 the GDL needed to be pressure washed a second time and deposits were observed in the evaporator cone, on the vessel walls and on the warming tubes. The GDL was pressure washed in the direction of the evaporator and in the direction of the drop tank to ensure that it was clean. Operation continued, with difficulty, from June 1998 until October 1999, when the evaporator was shut down. At this time, significant accumulations of the aluminosilicate scale and sodium diuranate deposits were found on many of the exposed surfaces of the evaporator pot. The scale in the 2H Evaporator was cleaned using a depleted uranyl nitrate solution in August 2001¹¹ and began operating again in October 2001.

Several important changes have been made in the handling of wastes entering the SRS evaporators in the last decade.* Prior to the mid 1990's, high activity waste was stored for >1 year before being processed in the evaporators so that the short lived radionuclides could decay before waste was concentrated. This also allowed any solids or colloidal species in the wastes to settle to the bottom of the tank before being processed. When the SRS reactors shut down and wastes were less radioactive, the one year hold strategy was no longer required.

In addition, the evaporators discharged to alternate drop tanks. When one drop tank was filled it was left to settle, and cool, and a second drop tank was used. Typically recycles to the feed tank were made from the passive drop tank and not from the active drop tank. This allowed any particulates or colloids in a given drop tank to settle before being recycled to the feed tank again for further concentration. The active/passive drop tank practice had to be discontinued in the early 1990's since there was no longer enough salt drop space in the concentrate receipt tanks.

In 1997, the 1st inter-area waste transfers were made between the SRS H-area and the SRS F-area waste tanks for the purpose of volume reducing the waste. This allowed co-mingling of wastes of different chemistries.

* Synopsis by Kent Gilbreath, Mark Mahoney, and Thomas Caldwell (May, 2001)

More recently, a decision was made to evaporate canyon and back-log waste in the 2F evaporator for initial salt separation. This occurs when the hydroxide molarity exceeds 6-8M. Then the desalted liquor is routed to the 3H evaporator for final dehydration, which can drive the hydroxide molarity above 12M.[‡]

These changes in operational strategy and co-mingling of waste have caused concerns that the aluminosilicate scaling problems experienced with the operation of the SRS 2H Evaporator could now become system wide. Thus a process control strategy was developed³ using Geochemist's Workbench (GWB) to prevent aluminosilicate scale formation in the SRS evaporators. Control of the aluminosilicate scale formation controls any criticality concerns caused by the adherent sodium diuranate, which is partially enriched ^{235}U .

2.2 Geochemist's Workbench (GWB)

The Geochemist's Workbench (GWB) database was modified to include various solids including stable and metastable aluminosilicate minerals such as Zeolite-A, nitrated-sodalite, nitrated-cancrinite, and NAS_{gel} (see Appendix B and Reference 9). Modifications to the solid aluminate species had previously been made as well.³ The solubility data incorporated into the database for the aluminosilicate and aluminate species had been measured at high Na molarity which then allowed the GWB code to be used for modeling solutions such as those in the SRS evaporators. In addition the GWB software has the following attributes:

- ability to estimate activity coefficients for high ionic strength solutions such as those in the evaporator
 - ability to improve the basis upon which the activity coefficients are estimated
- usage of Lawrence Livermore National Laboratory (LLNL) extensive database for minerals and aqueous species used to model the performance of waste forms in the High Level Waste (HLW) Repository
 - includes sodium diuranate and aqueous uranate species
- ability to calculate the relative stability of multiple solid phases simultaneously
- ability to graphically represent the relative stability of multiple phases in terms of three parameters simultaneously on activity or stability diagrams, e.g. Si, Al, and pH of a solution
- ability to perform polythermal reaction paths, e.g. reaction path can vary temperature linearly from an initial to a final value
- ability to simulate evaporation by removing a percentage of the water from the calculation, e.g. base the calculation on 0.6 kg of water rather than on the default of 1 kg of water for a simulated 40 wt % evaporation
- ability to calculate a supersaturation index for a given solid phase expressed as a ratio of the reaction quotient (Q) over the solubility product (K), e.g. $\log(Q/K)$
- ability to calculate the amount of the solid phase (in $\text{g}_{(\text{solid})}/\text{kg}_{(\text{soln})}$) that will form at the given supersaturation if precipitation to equilibrium proceeds.

[‡] HLW System Plan, Rev. 12

Two subroutines in GWB were used to model the precipitation of solids in the complex Na-N-Si-Al-U-H₂O system pertinent to the SRS 2H Evaporator; e.g. REACT and ACT2. The REACT subroutine models equilibrium states and processes of solids in equilibrium with aqueous fluids. The program calculates the following:

- equilibrium distribution of aqueous species in a fluid
- the fluid's saturation state with respect to mineral phases
- the fugacities of the gases dissolved in the fluid

During the process control modeling of scale formation in SRS evaporators only the REACT subroutine was used. All mineral formation (precipitation) was suppressed so that a saturation index ($\log Q/K$) could be calculated. Positive values of $\log (Q/K)$ are supersaturated while negative values are undersaturated with respect to the solid phase that could precipitate.

2.3 Orthogonal Latin Hypercube (OLH) Statistical Analysis

The statistical perspective of design problems involving computer experimentation, such as GWB, has been explored in references 12,13,14,15. These references identify and discuss the unique aspects of this type of design and analysis problem. A method for generating Orthogonal Latin Hypercube designs (OLHs)^{*} and their advantages for such problems are presented in Reference 15. An advantage of a Latin Hypercube approach is that it facilitates each of the input variables having all portions of its range represented.¹⁵ Thus, the approach provides a “space-filling” (for the factor space of interest, i.e., the concentrations, temperature, and percent evaporation) set of design points. Also, the estimates of linear effects of all factors are uncorrelated with each other, and the orthogonal Latin hypercube designs “guarantee that the estimates of quadratic effects and bilinear interaction effects are uncorrelated with estimates of linear effects. However, the estimates of quadratic and bilinear interaction effects are correlated with each other.”¹⁵

From Reference 15, an OLH consisting of n rows can be constructed when n is a power of 2 or a power of 2 plus 1 (i.e., 2^m or 2^m+1). A method is provided in Reference 15 for constructing and optimizing such an OLH with $2m-2$ columns. The value of $2m-2$ must be equal to or greater than the number of factors of interest. A value of 9 was used for m (with $2m-2 = 16$, which is greater than the 14 factors used for this study.^f A value of m=9 leads to a value for n of 512 or 513. For this design, a value of 513 was selected; thus, the interval of possible values for each input was divided into 513 equal sub-intervals.

Following the guidance provided in Reference 15, a minimax criterion was applied to random permutations of the design to provide a test matrix where the minimum Euclidean distance

* This class of orthogonal Latin hypercubes preserves orthogonality among columns, i.e., any two columns \mathbf{u} and \mathbf{v} of the OLH satisfy $\mathbf{u}^T \mathbf{v} = 0$ where \mathbf{u}^T is the transpose of \mathbf{u} .

^f The 14 factors were derived from the 16 parameters shown in Figure 1 by combining the concentrations nitrate with nitrite as nitrate and carbonate with oxalate as carbonate. This was done since GWB can only handle one nitrogen and one carbon species as input at a time. The 14 parameters included 12 composition parameters, temperature, and percent evaporation

between any pair of design vectors is a maximum. Such an approach was used to generate the test matrix (or experimental design) to support this study. Figure 1 provides an illustration of the space filling and pairwise orthogonality of the resulting test matrix used in this study with concentrations expressed as the molar concentrations. Brown¹⁶ provides the details of the design approach.

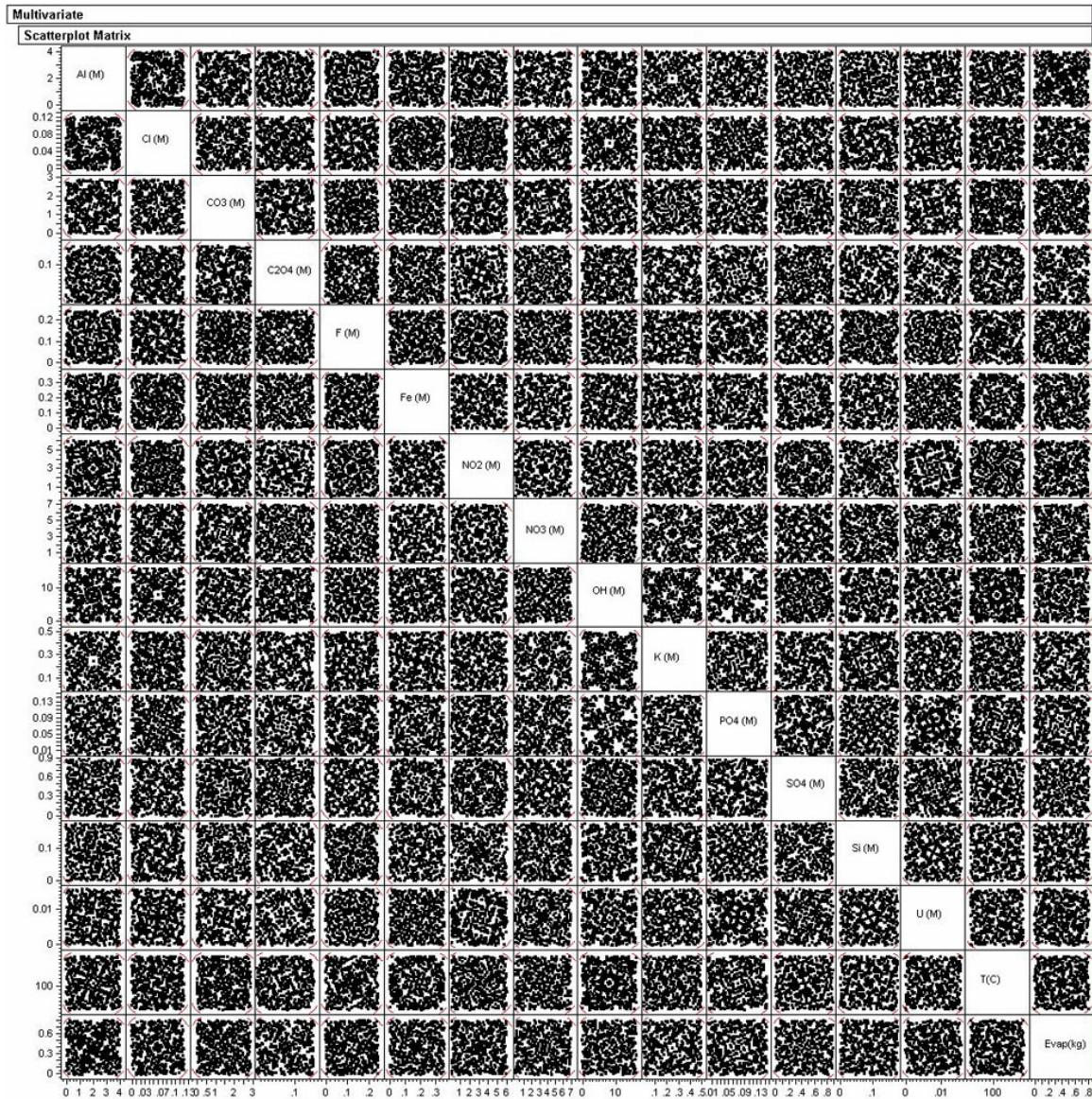


Figure 1. Scatterplot matrix for the Optimized OLH Design.

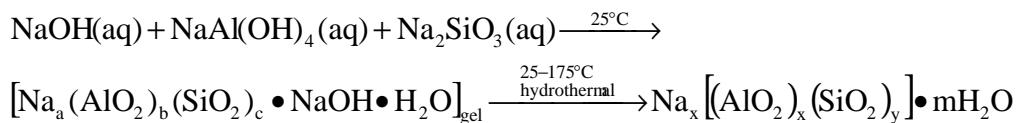
2.4 The Role of Kinetics in Thermodynamic Modeling

Thermodynamic modeling, when applied to processes that operate for relatively short time durations, is considered to be thermodynamically at steady state with respect to whatever phase is precipitating. Therefore, the kinetics of the formation of the deposits must be understood to determine which steady state phase is the appropriate phase(s) to model. Nitrated sodalites and nitrated cancrinite were found in the SRS evaporators. However, these phases are known to age in aqueous environments by dewatering and densification from a structurally related phase known as Zeolite-A. In turn, the Zeolite-A structure is known to form by any of the following mechanisms:

- from a gel process where the reactants are reactive oxides, soluble silicates, and soluble aluminates in a caustic solution (Figure 2)
- from conversion of clay minerals (specifically kaolin and meta-kaolin) in the presence of soluble silicates and caustic
- by reaction of silica sols, natural SiO₂, amorphous minerals, and volcanic glass in the presence of caustic (Figure 3).³

The gel reactions from solution and/or the silica sol reactions are the most significant of these mechanisms for SRS evaporator modeling although small traces of clay minerals could be introduced via the process water used in the evaporators. The gel reaction from solution assumed in this study takes the form:

Equation 1



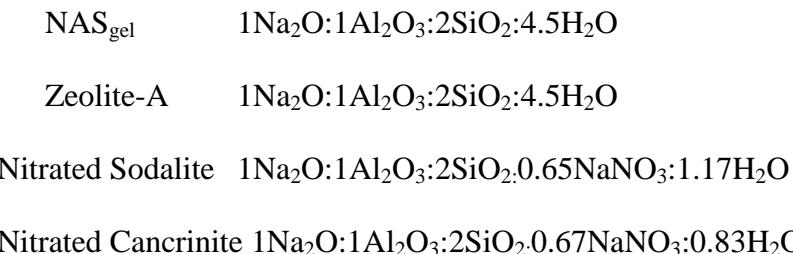
Formation from silica sols would substitute an $\equiv\text{Si}-\text{OH}$ (silanol) term into Equation 1 instead of Na₂SiO₃(aq).

Zeolites are synthesized industrially from solution using the gel process shown in Equation 1. Upon mixing sodium silicate and sodium aluminate at high pH, an amorphous sodium aluminosilicate gel (NAS_{gel}) phase forms. Transformation of the gel to the zeolite can take hours or days depending upon the synthesis conditions. Industrial synthesis of solid Zeolite-A involves precipitation from solutions of 4.0M NaOH to keep the crystallization times short and allow effective recycling of the excess NaOH.¹⁷

Gels are amorphous, as they are colloids in which the disperse phase has combined with the continuous phase to produce a semisolid material such as a jelly.¹⁸ As a gel deters or ages, it will form a denser gel and/or a crystalline solid phase. This is independent of the route of formation of the gel. Whether the NAS_{gel} forms from solution via a hydrogel process or whether

it forms from a sol (solid particles in liquid)¹⁹ via a sol-gel process, the aging sequence of the NAS_{gel} to denser sodalite and still denser cancrinite species will typically follow an aging path such as that shown in Figure 2 according to Barnes, Mensah and Gerson²⁰ and Gerson and Zheng.²¹ Note that the densification of the phases agrees with the following literature:

- Mensah, et. al.⁸ made phase pure NAS_{gel} , Zeolite-A, nitrated sodalite, and nitrated cancrinite and then measured the solubility in SRS-type evaporator solutions: the chemically analyzed stoichiometry of the phases are



- Bayer²² and Ejaz⁶ found that the NAS gels would transform to Zeolite-A. Ejaz experimentally determined the composition of the precursor gel at NaOH concentrations of 3-4.5M to be $0.93\text{Na}_2\text{O}:1\text{Al}_2\text{O}_3:2.32\text{SiO}_2:5.15\text{H}_2\text{O}$.
- Barrer²² found that the NAS gels would transform to Zeolite-A at pH values >10 in 2-3 hours at 110°C (the approximate temperature of the SRS evaporators)
- Buhl and Lons²³ showed that nitrated sodalite and nitrated cancrinite could best be made by starting with a Zeolite-A precursor in concentrated NaOH at various temperatures
- Wilmarth²⁴ showed that the Zeolite-A forms as a precursor but the nitrated cancrinite forms on the order of 3-5 hours at 110°C in simulated 2H Evaporator solutions
- Gasteiger et al.⁷ found that hydroxysodalite $\text{Na}_8[\text{Al}_6\text{Si}_6\text{O}_{24}](\text{OH})_2 \bullet (1.5\text{H}_2\text{O})$ and sodalite ($\text{Na}_8[\text{Al}_6\text{Si}_6\text{O}_{24}](\text{Cl})_2$) formation was >99% complete in 24 hours at 95°C and that the sodalites formed via a Zeolite-A precursor
- Subotic, et. al.²⁵ demonstrated that aluminosilicate gels that have a Si/Al = 1 form Zeolite-A at lower NaOH concentrations in solution at 85°C which then transforms into hydroxysodalite; at higher NaOH concentrations the gel can transform into hydroxysodalite without the Zeolite-A precursor formation
- Bosnar and Subotic²⁶ demonstrated that Zeolite-A forms from an amorphous aluminosilicate precursor ($1.03\text{Na}_2\text{O} \bullet \text{Al}_2\text{O}_3 \bullet 2.38\text{SiO}_2 \bullet 1.66\text{H}_2\text{O}$) and the Zeolite-A growth is governed by the Davies-Jones model of growth and dissolution (growth of Zeolite-A from solution coupled with dissolution of the amorphous phase); growth rate decreases with increasing alkalinity

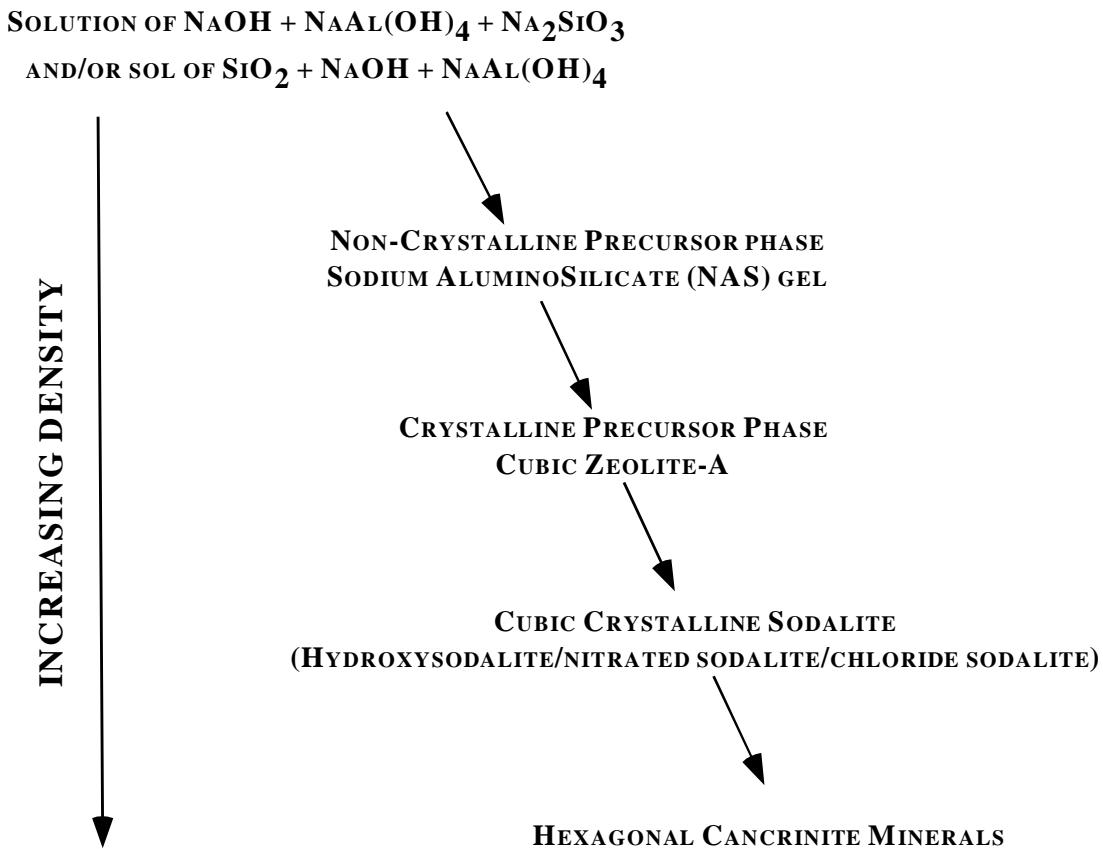


Figure 2. Typical formation and aging (densification) sequence of $\text{NAS}_{\text{gel}} \rightarrow$ Zeolite-A \rightarrow sodalite \rightarrow cancrinite phases depending on the relative concentration of OH^- , Cl^- , NO_3^- , and/or $\text{CO}_3^{=}$ in the solution in contact with the NAS_{gel} (after Gerson, et.al.)^{20,21}

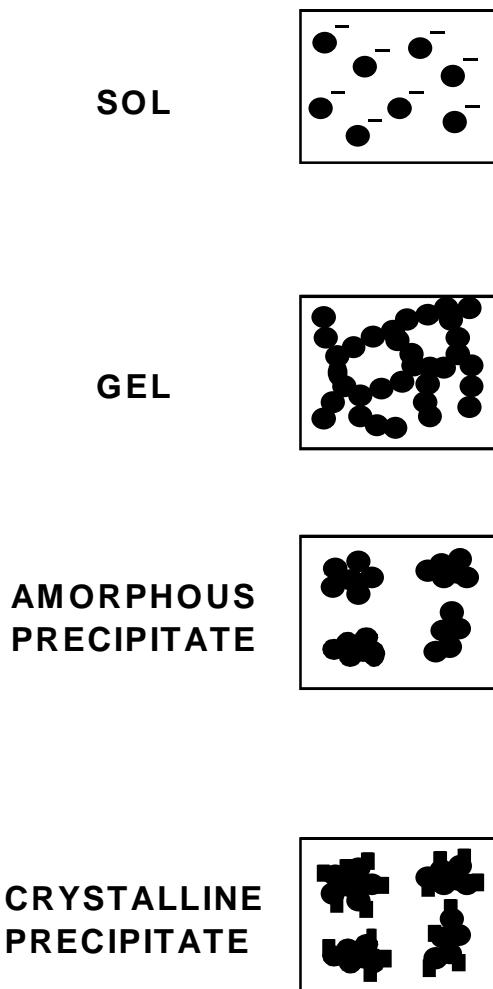


Figure 3. Pictorial diagram showing the differences between a sol, gel, and precipitate (after references 27 and 28).

As expected due to long aging times, solids isolated from the SRS 2H Evaporator were identified as nitrated sodalite and nitrated cancrinite. In Part I³ of this study the activity diagram modeling indicated that the precursor phase most pertinent to deposition in SRS evaporators was the NAS_{gel} due to the short residence times of waste solutions in the evaporators. This was confirmed by kinetic testing performed at ORNL²⁹ and further supported by kinetic testing performed at PNNL.³⁰

One set of PNNL kinetic data is plotted as a sequence of overlays showing the activity boundaries for NAS_{gel} , Zeolite-A, nitrated sodalite and nitrated cancrinite generated using the solubility data of Mensah (Figure 4). This figure demonstrates that when a solution is saturated with respect to NAS_{gel} at 80°C it first precipitates as the gel, followed by slow dissolution of the gel and formation of Zeolite-A, followed by dissolution of gel and Zeolite-A to form nitrated sodalite as a function of time.

The metastable persistence of an amorphous phase, assumed^f to be NAS_{gel} , and the metastable persistence of sodalite with time complicates using this kinetic data to validate the positions of the phase boundaries based on the Mensah data.⁸ However, in general, the precipitation of Zeolite-A only occurs within its phase field, and the precipitation of cancrinite only occurs within its phase field, confirming that the persistence of the NAS_{gel} and sodalite is a metastable phenomenon. More detailed discussion of this data can be found in Part V⁹ and in the following paragraphs.

Plotting the PNNL NAS_{gel} saturated solutions as a function of both time and temperature substantiates the presence of the NAS_{gel} at elevated temperatures. This graphical representation is known as a time-temperature-transformation (TTT) diagram and is shown in Figure 5. The phase fields represented on the TTT curve obey c-curve kinetics and Hardy's general rule³¹ that the appearance of a more stable decomposition product causes the dissolution of its immediate precursor. The c-shaped curvature of a stable or metastable phase field on a TTT diagram arises from a competition between the driving force for crystallization which increases with decreasing temperature, and the molecular mobility, which decreases with decreasing temperature.³² At low temperature, the activation energy for nucleation approaches zero and the low temperature part of the c-curve is approximately linear with a slope of Q/R . The numerator, Q , is the activation energy of a jump process across an interface and R is the gas constant.³³ At low temperatures, the linear portion of the c-curve represents the "retardation temperature" of the nucleation rate and defines a rate curve for a precipitation or reversion reaction³⁴ in the absence of nucleating heterogeneities. Hence, the c-curve kinetics define a "nose" in the TTT curve which represents the minimum time required for a given volume fraction to crystallize (precipitate).

The data for all the solutions in Figure 5 indicate that the NAS_{gel} persists along with the Zeolite-A and sodalite. With increasing time, the mass percent of the NAS_{gel} decreases as the mass percent of the crystalline species increases in obeiance of Hardy's law.³¹ The data from solutions #1 and #2 in Figure 5 indicate that the phase field of Zeolite-A may persist metastably, e.g. the field of Zeolite-A is truncated by the more stable phase field of NAS_{gel} plus sodalite.

^f In the absence of a chemical analysis of the amorphous phase the exact identity of this phase cannot be determined by x-ray diffraction analyses alone, for example it could be amorphous cancrinite or amorphous sodalite depending on the anion content and/or on the water of hydrations per unit cell.

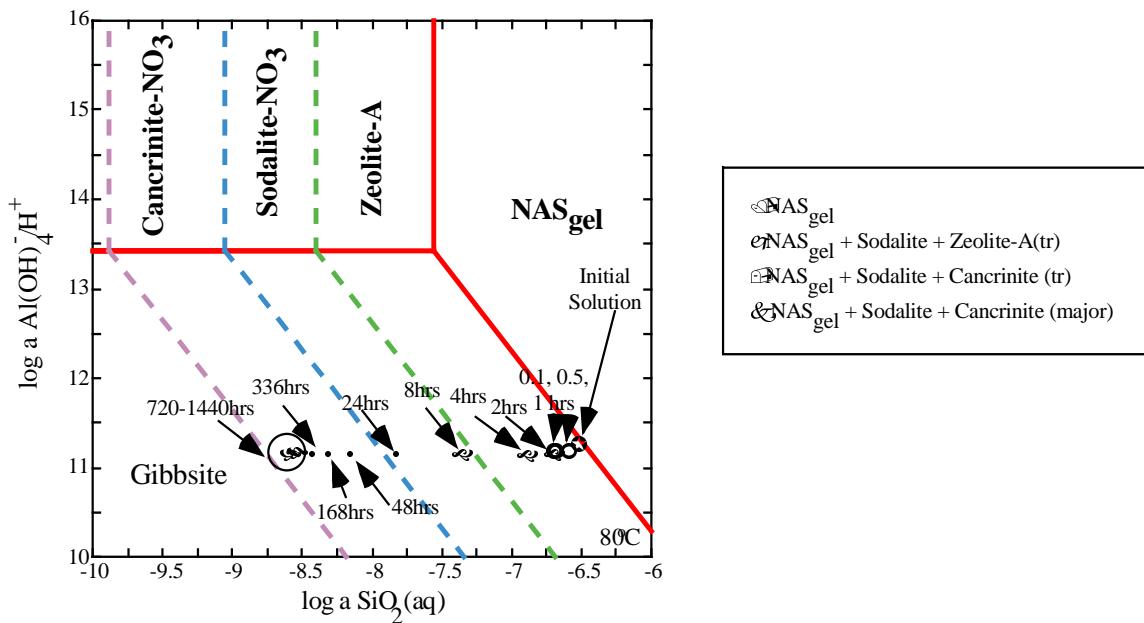


Figure 4. Overlays of the activity diagrams for NAS_{gel} , Zeolite-A, nitrated sodalite and nitrated cancrinite showing the kinetic data of Mattigod from PNNL.

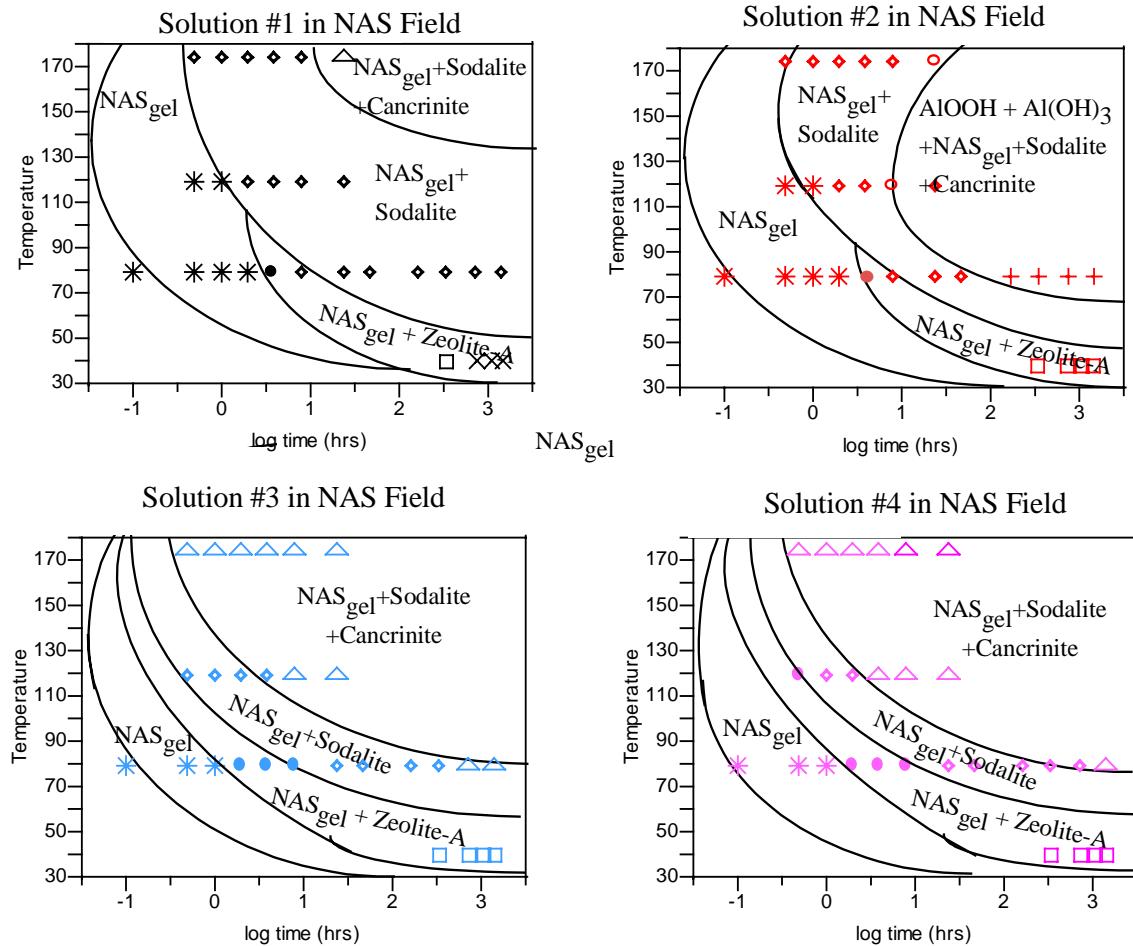


Figure 5. Time-Temperature-Transformation (TTT) diagram of the kinetic data developed by PNNL in support of SRS evaporator modeling. The phase field designations are as follows: * = NAS_{gel} ; ● = $\text{NAS}_{\text{gel}} + \text{Sodalite} + \text{Zeolite-A}$; ◇ = $\text{NAS}_{\text{gel}} + \text{Sodalite}$; ∇ = $\text{NAS}_{\text{gel}} + \text{Sodalite} + \text{Cancrinite}$; ≡ = $\text{NAS}_{\text{gel}} + \text{Zeolite-A}$; + = $\text{Al}(\text{OH})_3$, gibbsite; ! = $\text{NAS}_{\text{gel}} + \text{boehmite} + \text{gibbsite}$

However, as the OH^- concentration is increased (solutions #3 and #4) it becomes apparent that the Zeolite-A phase persists up to 120°C and may persist at higher temperatures as indicated in Figure 5. The shorter time, higher temperature intervals are under investigation at PNNL.

Based on the kinetic analysis above, it is clear that the NAS_{gel} forms first, and that once formed (once a solution is supersaturated with respect to the NAS_{gel}), the NAS_{gel} phase can persist at the elevated temperatures in the evaporator along with the more thermodynamically stable sodalite and cancrinite crystalline phases. It is the function of the process control model to prevent the evaporator solutions from ever becoming supersaturated with respect to the NAS_{gel} ; thus preventing the precipitation of the NAS_{gel} and all subsequent stable crystalline NAS phases.

3.0 RECENT ANALYTIC DATA AVAILABLE FOR EVAPORATOR MODELING

3.1 Availability of Analytic Data

A compilation of molar chemical analyses for Tanks 30, 32, 26, 46, 43, and 38 that were used in the modeling and validation in this study appears in Table I, Table II, and Table III for the time period January 1995 to June 2002. All of this data was analyzed at SRTC where the silicon analyses represent the entire sample instead of one aliquot (one pipette volume). While there is historic data from 1992 available from SRTC, the silicon analyses associated with these historic samples were only measured from one pipette volume, which is inadequate when inhomogeneously dispersed colloidal silica is present. There were sparse and incomplete data for many minor cations and anions. When data for these minor cation species (e.g. Fe and K) were missing or below the analytical detection limit, $\frac{1}{2}$ the instrument detection limit was substituted assuming that a small concentration below the detection limits was probably present. The latter accounts for errors of 100-200% for a concentration at or near the instrument detection limit.

Sodium analyses, when available, were added into Table I, Table II, and Table III using data from various SRTC reports by Wilmarth (documented in the tables).^{35, 36} Conversely, Wilmarth did not analyze for the cation K^+ nor several anions, e.g. Cl^- , CO_3^{2-} , F^- , PO_4^{3-} , SO_4^{2-} . When minor anion species such as these were missing or below the analytical detection limit, $\frac{1}{2}$ the instrument detection limit was substituted. Occasionally, data from F-Area laboratory was substituted from samples taken on the same day as the SRTC samples or averaged from F-Area laboratory analyses that bracketed the missing data, e.g. usually taken 3 months before and 3 months after the missing data.

All available tank data modeled were measured at ambient ($\sim 25^\circ C$) laboratory conditions and not at the tank temperature at the time of sampling. Bulk supernate temperatures can vary from $30^\circ C$ to $75^\circ C$. Possible changes in solution composition upon cooling of the tank samples were not accounted for during the measurements. However, temperature affects are accounted for during modeling at elevated temperatures with GWB.

3.2 Consistency of Analytic Data

In order to use the chemical analyses compiled in Table I, Table II, and Table III for modeling, the data had to be made internally consistent, e.g., anion and cation charges were balanced. Since few measured Na^+ molarities were available no adjustments were made to the molarities of the three principal anions, OH^- , NO_3^- , and NO_2^- to balance against measured Na^+ concentrations. The charge balance calculations assumed a single ionic species; most importantly, Al was modeled as $Al(OH)_4^-$ and Si as $H_2SiO_4^{2-}$.

The GWB software uses molality instead of molarity when performing the basic thermodynamic calculations. If molarity is entered instead of molality, GWB uses a default density of 1 gm/cm^3 or the user has to specify both a density and total dissolved solids (TDS). Rather than specify a solution density and TDS, the molar concentration data in Table I, Table II, and were converted

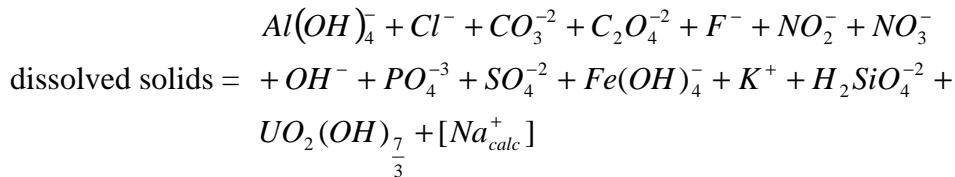
to molalities (see Section 4.0). The molalities are based on calculated solution densities and total weight of the solutes (Equation 2).³⁷ The solution densities were calculated from a calculated Na⁺ molarity, $[Na^+]_{calc}$, using Equation 3 derived in Appendix A from over 1800 supernate samples taken over a period of 29 years (1973-2001) and measured at ambient laboratory conditions.

$$\text{Equation 2} \quad m = M \left(\frac{\text{weight solution}}{(\text{weight solution} - \text{total weight solutes})} \right) \left(\frac{1}{\text{density}_{calc}} \right)$$

where m = molality

M = molarity

$$\text{weight solutes} = \frac{\text{dissolved solids (g/L)}}{1000L}$$



$$\text{Equation 3} \quad \text{density}_{calc} \equiv \rho = 1.0133 + 0.05701[Na^+]_{calc} - 0.001725[Na^+]_{calc}^2$$

where ρ is the calculated solution density (see Appendix B) in g/cm³ and $[Na^+]_{calc}$ is the calculated molar Na⁺ concentration from Equation 4.

$$\begin{aligned} & NaAl(OH)_4 + NaCl + Na_2CO_3 + Na_2C_2O_4 + NaF + \\ \text{Equation 4} \quad Na_{calc}^+ = & NaNO_2 + NaNO_3 + NaOH + Na_3PO_4 + Na_2SO_4 + NaFe(OH)_4^- \\ & - KOH + Na_2H_2SiO_4 + Na(UO_2)_3(OH)_7 \end{aligned}$$

The molal contributions from CO₃⁻² and C₂O₄⁻² were summed as a total CO₃⁻² contribution, e.g. one mole of C₂O₄⁻² was considered to be two moles of CO₃⁻² since Geochemist's Workbench can only accommodate one carbon species at a time. The NO₂⁻ and NO₃⁻ were summed as NO₃⁻ since Geochemist's Workbench can only accommodate one nitrogen species at a time.

In addition to reporting molar concentrations, Table I, Table II, and Table III compare calculated and measured solution densities. Solution densities were calculated from Equation 3. The majority (>75%) of the measured and calculated densities agreed within 5%.

3.3 Quality of Analytic Data

The SRTC and the F-area laboratories both analyzed samples taken between February 2001 and July 2002. The two laboratories never measured the same sample taken on the same day so no comparisons of the analytic bias between the two laboratories can be made for this set of data. However, in Parts I³ and Part II⁴ of this study it was shown that the 210X dilution performed by the F-area laboratory always caused their Si analyses to be biased high compared to those of SRTC. The lower the actual Si concentration (Part II⁴) the higher the bias (compare to Part I³). In addition, samples taken during the receipt of high Al-containing canyon waste in the 2H Evaporator were analyzed³ as being at the detection limit for Al which is impossible.

SRTC has developed a method by which the entire sample (70 mL) is filtered so that the total amount of Si (both soluble and colloidal) can be more accurately determined. The filtrate, representing the soluble silicon, is homogeneous and can be accurately measured by ICP. The colloidal silicon on the filter is dissolved and measured separately. The two are added together for a final total silicon analysis that is representative of the entire sample^{35,36} rather than a few milliliters of solution in a pipette. Because of the high bias in the F-area laboratory Si analyses, only the Si analyses reported by Wilmarth were used for modeling in Part I³ and Part II⁴ of this study. This is the method used to determine the silica for all samples used in modeling in Table I, Table II, and Table III. Recently, a warm acid strike treatment for silicon analyses of evaporator solutions has been developed³⁸ which was determined to be as accurate as the filtration method described above.

Table I. Analytic data from SRTC for Evaporator Feed Tank 32 Used For Modeling

Date	Description/ Reference	Height (inches)	Al (M)	Cl (M)	CO ₃ (M)	C ₂ O ₄ (M)	F (M)	NO ₂ (M)	NO ₃ (M)	OH (M)	PO ₄ (M)	Fe (M)	K (M)	Si (M)	U (M)	Na Calc (M)	Na Meas (M)	wt salt, g/L	Dens calc g/ml	Dens meas g/ml	
Tank 32																					
9/4/00	WSRC-TR-2000-00339	dip(250)	0.79	1.18E-02	2.00E-02	2.90E-03	4.03E-03	1.44	3.42	4.86	8.05E-03	1.51E-02	1.43E-05	5.15E-02	7.37E-04	1.85E-05	10.58	10.57	685.37	1.42	1.38
8/21/00	WSRC-TR-2000-00339	dip(209)	0.53	1.18E-02	2.00E-02	2.85E-03	4.03E-03	0.84	1.39	4.45	8.05E-03	1.51E-02	5.66E-04	5.15E-02	6.68E-04	1.85E-05	7.27	7.26	424.00	1.34	1.34
2/1/00	TK32H-SI(WSRC-TR-2000-00112)	dip	0.56	1.18E-02	2.00E-02	2.85E-03	4.03E-03	1.05	1.62	3.37	8.05E-03	1.51E-02	1.81E-04	5.15E-02	2.85E-04	1.22E-05	6.66	6.66	418.45	1.32	1.28
2/1/00	TK32H-SI(WSRC-TR-2000-00112)	dip	0.57	1.18E-02	2.00E-02	2.85E-03	4.03E-03	1.07	1.66	3.46	8.05E-03	1.51E-02	1.86E-04	5.15E-02	2.85E-04	1.18E-05	6.84	6.83	429.29	1.32	1.28
9/4/00	WSRC-TR-2000-00339	120	0.80	1.18E-02	2.00E-02	2.85E-03	4.03E-03	1.57	2.91	5.15	8.05E-03	1.51E-02	5.91E-04	5.15E-02	8.33E-04	2.45E-05	10.49	10.48	663.91	1.42	1.46
9/4/00	WSRC-TR-2000-00339	90	0.35	1.18E-02	2.00E-02	2.85E-03	4.03E-03	1.24	3.25	4.18	8.05E-03	1.51E-02	3.56E-04	5.15E-02	6.91E-04	9.71E-04	9.08	9.07	578.34	1.39	1.40
8/21/00	WSRC-TR-2000-00339	120	0.62	1.18E-02	2.00E-02	2.85E-03	4.03E-03	0.95	1.74	5.21	8.05E-03	1.51E-02	5.00E-04	5.15E-02	6.00E-04	1.45E-05	8.58	8.57	502.16	1.38	1.34
8/21/00	WSRC-TR-2000-00339	90	0.63	1.18E-02	2.00E-02	2.85E-03	4.03E-03	1.06	1.82	5.00	8.05E-03	1.51E-02	3.19E-04	5.15E-02	6.87E-04	9.71E-04	8.58	8.57	510.28	1.38	1.33
9/4/00	WSRC-TR-2000-00339	70	0.73	1.18E-02	2.00E-02	2.85E-03	4.03E-03	1.25	3.13	4.23	8.05E-03	1.51E-02	2.19E-03	5.15E-02	7.39E-04	2.83E-05	9.41	9.40	616.21	1.40	1.40
8/21/00	WSRC-TR-2000-00339	70	0.62	1.18E-02	2.00E-02	2.85E-03	4.03E-03	0.95	1.75	5.24	8.05E-03	1.51E-02	4.15E-04	5.15E-02	6.20E-04	1.54E-05	8.62	8.61	504.72	1.38	1.34
2/1/00	TK32H-SI(WSRC-TR-2000-00112)	89	0.56	1.18E-02	2.00E-02	2.85E-03	4.03E-03	0.92	2.00	3.69	8.05E-03	1.51E-02	2.51E-04	5.15E-02	9.83E-04	1.60E-05	7.23	7.22	454.79	1.34	1.30
2/1/00	TK32H-SI(WSRC-TR-2000-00112)	89	0.52	1.18E-02	2.00E-02	2.85E-03	4.03E-03	0.86	1.88	3.47	8.05E-03	1.51E-02	3.31E-04	5.15E-02	9.04E-04	1.51E-05	6.79	6.79	427.03	1.32	1.27
2-Jun	HTK-505 ³⁹	196.5	1.10	1.49E-02	5.00E-03	2.85E-03	1.70	1.20	5.30	9.10E-03	1.59E-02	5.59E-04	6.10E-02	1.42E-03	3.11E-05	9.33	-	567.99	1.39	-	
2-Jun	HTK-506 ³⁹	89	0.93	1.49E-02	5.00E-03	2.85E-03	2.10	1.60	6.20	9.10E-03	1.59E-02	5.59E-04	6.10E-02	1.67E-03	3.11E-05	10.87	-	645.56	1.43	-	
2-Jun	HTK-507 ³⁹	77	1.00	1.49E-02	5.00E-03	2.85E-03	2.50	1.90	7.30	9.10E-03	1.59E-02	5.59E-04	6.10E-02	1.64E-03	3.11E-05	12.74	-	750.90	1.46	-	

Table II. Analytic data from SRTC for Evaporator Feed Tanks 43 and 26 Used For Modeling (Continued)

Date	Description/ Reference	Height (inchs)	Al (M)	Cl (M)	CO ₃ (M)	C ₂ O ₄ (M)	F (M)	NO ₂ (M)	NO ₃ (M)	OH (M)	PO ₄ (M)	SO ₄ (M)	Fe (M)	K (M)	Si (M)	U (M)	Na Meas (M)	Na Calc (M)	wt salt, g/L	Dens calc g/ml	Dens meas g/ml
Tank 26																					
1/95/1/96	Composite ¹⁰	Dip	0.23	1.63E-02	8.33E-02	3.40E-03	6.50E-03	1.54	2.00	6.44	8.70E-03	1.72E-02	5.0E-03	5.93E-02	4.04E-03	1.88E-04	10.41	7.18	576.59	1.42	.
6/01	FTF-042 ⁴⁰	261"	0.35	1.50E-02	5.00E-03	3.40E-03	2.70E-03	0.94	1.42	5.75	7.80E-03	3.00E-02	3.87E-04	5.00E-02	9.26E-04	3.30E-05	8.53	9.45	465.16	1.37	1.32
6/01	FTF-043 ⁴⁰	166"	0.32	1.50E-02	5.00E-03	3.40E-03	2.70E-03	0.89	1.33	5.26	7.80E-03	3.00E-02	3.42E-04	5.00E-02	3.36E-03	3.57E-05	7.87	8.10	431.43	1.35	.
6/01	FTF-044 ⁴⁰	65"	0.74	1.50E-02	5.00E-03	3.40E-03	2.70E-03	1.91	1.51	10.30	7.80E-03	3.00E-02	1.01E-03	5.00E-02	1.52E-03	4.14E-05	14.53	14.00	768.23	1.48	.
7/02	FTF-089 ⁴¹	VDS	0.40	1.49E-02	5.00E-03	3.50E-03	2.70E-03	1.47	2.11	7.04	9.10E-03	1.59E-02	5.59E-04	4.60E-02	1.85E-03	3.11E-05	11.07	12.00	616.37	1.43	.
7/02	FTF-090 ⁴¹	VDS	0.50	1.49E-02	5.00E-03	3.50E-03	2.70E-03	1.54	2.08	7.51	9.10E-03	1.59E-02	5.59E-04	4.60E-02	2.60E-03	3.11E-05	11.68	12.78	649.35	1.44	.
7/02	FTF-091 ⁴¹	VDS	0.50	1.49E-02	5.00E-03	3.50E-03	2.70E-03	1.56	2.04	8.56	9.10E-03	1.59E-02	5.59E-04	4.60E-02	2.60E-03	3.11E-05	12.71	12.46	689.33	1.46	.
Tank 43																					
1/16/00	W+P(WSRC-TR-2000-00208)-dip	dip	0.11	3.10E-03	1.30E-01	3.40E-03	2.65E-03	0.80	1.13	2.60	5.88E-03	1.66E-02	2.09E-04	1.23E-02	3.08E-03	7.31E-05	4.96	4.96	286.81	1.25	1.19
10/1/97	HTF-029		0.13	5.60E-03	2.40E-01	3.40E-03	2.65E-03	0.95	0.94	3.90	1.10E-02	6.30E-03	5.0E-03	2.40E-02	1.53E-03	9.12E-05	6.43	.	346.13	1.31	.
2/2/00	W+P(WSRC-TR-2000-00208)100"	100	0.19	6.52E-03	2.23E-01	3.40E-03	9.09E-03	1.37	1.94	4.53	1.28E-02	2.84E-02	4.87E-04	2.66E-02	4.49E-03	5.13E-05	8.58	8.57	495.02	1.38	1.31
2/2/00	W+P(WSRC-TR-2000-00208) ³ 'above sludge	64	0.50	6.39E-03	2.19E-01	3.40E-03	8.92E-03	1.34	1.90	4.44	1.25E-02	2.78E-02	3.58E-01	2.61E-02	1.44E-01	2.36E-03	9.36	9.35	595.07	1.40	1.39
10/97	HTF-028(Wilmart et.al. ¹⁰)	VDS	0.12	5.60E-03	2.40E-01	3.40E-03	2.65E-03	0.90	0.89	3.70	1.10E-02	6.30E-03	5.0E-03	2.40E-02	1.51E-03	8.65E-05	6.13	6.10	329.69	1.30	.

Table III. Analytic data from SRTC for Evaporator Drop Tanks 30, 46, 38 Used For Model Validation

Date	Description/Reference	Height (inches)	Al (M)	Cl (M)	C ₂ O ₄ (M)	CO ₃ (M)	F (M)	NO ₂ (M)	NO ₃ (M)	OH (M)	PO ₄ (M)	SO ₄ (M)	Fe (M)	K (M)	Si (M)	U (M)	Na Calc (M)	Na Meas (M)	wt salt, g/L	Dens calc g/ml	Dens meas g/ml
Tank 30																					
12/1/00	303surface#f388	dip(170")	0.79	1.49E-02	5.00E-03	2.85E-03	2.65E-03	1.40	2.80	5.05	9.10E-03	1.59E-02	5.59E-04	6.10E-02	4.41E-04	2.00E-05	10.07	.	636.76	1.41	1.08
8/21/00	Tk30H-S1	dip(348")	0.79	1.49E-02	5.00E-03	2.85E-03	2.65E-03	1.66	2.79	4.54	9.10E-03	1.59E-02	5.55E-04	6.10E-02	3.69E-04	1.77E-05	9.81	9.83	633.19	1.41	1.40
12/1/00	1.03non HTF390	240	0.80	1.49E-02	5.00E-03	2.85E-03	2.65E-03	1.33	2.83	4.99	9.10E-03	1.59E-02	4.87E-03	6.10E-02	3.44E-04	6.60E-05	9.98	.	633.61	1.41	1.44
12/1/00	2.03nonHT389	200	0.79	1.49E-02	5.00E-03	2.85E-03	2.65E-03	1.35	2.85	4.96	9.10E-03	1.59E-02	3.68E-04	6.10E-02	3.35E-04	4.30E-05	9.99	.	634.31	1.41	1.14
2/1/00	Tk30H-VDS	VDS	0.64	1.49E-02	5.00E-03	2.85E-03	2.65E-03	1.31	2.78	4.87	9.10E-03	1.59E-02	8.67E-04	6.10E-02	6.41E-04	2.23E-05	9.64	9.66	604.30	1.40	1.34
8/21/00	Tk30H-S2	VDS	0.79	1.49E-02	5.00E-03	2.85E-03	2.65E-03	1.39	2.95	5.17	9.10E-03	1.59E-02	3.65E-04	6.10E-02	3.35E-04	4.37E-05	10.34	10.35	633.87	1.42	1.41
2-Jan	HTK-480 ⁴²	VDS	1.10	1.49E-02	5.00E-03	2.85E-03	2.65E-03	1.72	1.26	9.73	9.10E-03	1.59E-02	5.59E-04	6.10E-02	1.64E-03	3.11E-05	13.85	.	751.68	1.47	.
2-Jan	HTK-481 ⁴²	VDS	0.60	1.49E-02	5.00E-03	2.85E-03	2.65E-03	1.76	1.26	9.42	9.10E-03	1.59E-02	2.85E-03	6.10E-02	2.85E-03	3.11E-05	13.08	.	683.22	1.46	.
2-Jan	HTK-482 ⁴²	VDS	1.10	1.49E-02	5.00E-03	2.85E-03	2.65E-03	1.92	1.37	9.58	9.10E-03	1.59E-02	5.59E-04	6.10E-02	2.67E-03	3.11E-05	14.01	.	768.98	1.47	.
2-Jun	HTK-508 ³⁶	221.9	1.10	1.49E-02	5.00E-03	2.85E-03	2.65E-03	1.70	1.25	9.70	9.10E-03	1.59E-02	5.59E-04	6.10E-02	2.42E-03	3.11E-05	13.79	.	748.36	1.47	.
2-Jun	HTK-509 ³⁶	156	0.83	1.49E-02	5.00E-03	2.85E-03	2.65E-03	1.20	0.92	6.70	9.10E-03	1.59E-02	5.59E-04	6.10E-02	1.89E-03	3.11E-05	9.69	.	533.89	1.40	.
2-Jun	HTK-511 ³⁶	4	0.97	1.49E-02	5.00E-03	2.85E-03	2.65E-03	1.14	0.85	6.20	9.10E-03	1.59E-02	5.59E-04	6.10E-02	1.28E-03	3.11E-05	9.19	.	520.24	1.39	.
Tank 46																					
12/7/98	WSRC-TR-99-0049	Dip	0.78	1.19E-02	3.22E-01	2.80E-03	2.60E-03	1.76	1.49	9.78	2.60E-03	1.55E-02	5.0E-03	7.05E-02	1.40E-03	3.59E-05	14.44	.	770.45	1.48	1.45
1/95/1/96	Composite ¹⁰	Dip	0.33	2.21E-02	7.32E-02	3.40E-03	6.50E-03	1.69	1.69	8.98	1.13E-02	1.06E-02	5.0E-03	7.80E-02	3.00E-03	3.01E-05	12.86	7.55	673.51	1.46	1.49
6/01	FTF-045 ⁴⁰	252"	0.77	1.50E-02	5.00E-03	3.40E-03	2.70E-03	1.35	1.09	11.70	7.80E-03	3.00E-02	6.34E-04	5.00E-02	1.66E-03	3.98E-05	14.98	14.70	733.15	1.48	1.50
6/01	FTF-046 ⁴⁰	199"	0.91	1.50E-02	5.00E-03	3.40E-03	2.70E-03	1.35	1.09	11.70	7.80E-03	3.00E-02	7.34E-04	5.00E-02	2.54E-03	3.83E-05	15.12	18.30	769.46	1.48	1.64
6/01	FTF-047 ⁴⁰	145"	0.70	1.50E-02	5.00E-03	3.40E-03	2.70E-03	1.35	1.09	11.70	7.80E-03	3.00E-02	5.28E-04	5.00E-02	2.15E-03	1.67E-05	14.91	13.70	744.94	1.48	1.53
7/02	FTF-092 ⁴³	VDS	0.50	1.49E-02	5.00E-03	3.50E-03	2.70E-03	1.77	1.63	8.28	9.10E-03	1.59E-02	5.59E-04	4.60E-02	2.49E-03	3.11E-05	12.23	14.40	657.75	1.45	.
7/02	FTF-093 ⁴³	VDS	0.60	1.49E-02	5.00E-03	3.50E-03	2.70E-03	1.89	1.52	9.44	9.10E-03	1.59E-02	5.59E-04	4.60E-02	2.60E-03	3.11E-05	13.50	11.90	714.90	1.47	.
7/02	FTF-094 ⁴³	VDS	0.60	1.49E-02	5.00E-03	3.50E-03	2.70E-03	1.83	1.58	8.86	9.10E-03	1.59E-02	5.59E-04	4.60E-02	2.03E-03	3.11E-05	12.92	12.20	692.58	1.46	.
Tank 38																					
10/1/97	HTF-30 ^W	VDS	0.23	9.00E-03	2.20E-01	3.40E-03	6.50E-03	1.31	1.24	4.84	1.65E-02	1.02E-02	5.0E-03	3.70E-02	1.45E-03	6.61E-05	8.11	8.38	445.85	1.36	.
10/1/97	HTF-31 ^W	dip	0.10	9.00E-03	2.20E-01	3.40E-03	6.50E-03	1.31	1.24	4.84	1.65E-02	1.02E-02	5.0E-03	3.70E-02	1.32E-03	5.81E-05	7.98	6.09	430.52	1.36	.

4.0 MODELING APPROACH

The molar tank compositions given in Table I, Table II, and Table III were converted into molal units which are the units of preference in the GWB software. The conversion formula takes the form⁵

$$[\text{i}^{+/-}]_m = \frac{[\text{i}^{+/-}]_M}{\rho - \sum \rho_{\text{solute}}}$$

where $[\text{i}^{+/-}]_M$ and $[\text{i}^{+/-}]_m$ are the molar and molal concentrations of ionic species i, respectively, ρ is the solution density in kg/L, and $\sum \rho_{\text{solute}}$ is the sum of the partial densities of the dissolved solids. The solution density is calculated using Equation 3. For each ionic species, the partial dissolved solids density is the product of its molarity and its ionic weight in g/mole. Ionic weights for the most prevalent species in basic solutions such as the SRS evaporators are used. These are Al(OH)_4^- , Cl^- , CO_3^{2-} , F^- , NO_2^- , NO_3^- , OH^- , PO_4^{3-} , SO_4^{2-} , Fe(OH)_4^- , K^+ , $\text{H}_2\text{SiO}_4^{2-}$, $(\text{UO}_2)_3(\text{OH})_7^-$, and Na^+ .

There is limited solubility data for amorphous SiO_2 and Al(OH)_3 in very basic, high ionic strength solutions such as those in the SRS evaporators. This is discussed in more detail in Part I.³ Comparison with available SiO_2 solubility data in the literature showed that the solubility data used in GWB appeared to adequately represent amorphous SiO_2 equilibrium in basic solutions. GWB has the mononuclear silicate species H_4SiO_4 called $\text{SiO}_2(\text{aq})$, H_3SiO_4^- and $\text{H}_2\text{SiO}_4^{2-}$ of which the $\text{H}_2\text{SiO}_4^{2-}$ species is the most prevalent at pH values >13.⁴⁴ GWB also contains the two most abundant^{45,44} polynuclear silicate species, the tetrameric $\text{H}_4(\text{H}_2\text{SiO}_4)_4^{4-}$ and $\text{H}_6(\text{H}_2\text{SiO}_4)_4^{2-}$ of which the tetrameric $\text{H}_4(\text{H}_2\text{SiO}_4)_4^{4-}$ is the most prevalent species at pH values >13.⁴⁴ Polynuclear Si(IV) species are only significant at pH>10 and at total dissolved Si concentrations larger than 10^{-3}M .⁴⁶ In addition, the significance of the polynuclear Si(IV) species tends to decrease with increasing temperature.⁴⁷ Since the SRS Evaporator Si concentrations are in the 10^{-4}M range (Table I, Table II, and Table III) and the polynuclear Si(IV) species are of minimal importance at the elevated evaporator operating temperatures (>120°C), the absence of the remaining polynuclear Si(IV) species in the GWB database is not considered to significantly impact the modeling.

Examination of the gibbsite solubility data in GWB with that in the literature indicated that Russell's⁴⁸ solubility data at a sodium molality of 8.5 would be more appropriate for modeling at the high ionic strength of the SRS Evaporators. The Russel solubility data for gibbsite (alpha aluminum trihydrate)^f and diaspore (alpha aluminum monohydrate)^ø were added to GWB database and designated as "gibbsite-M" and "diaspore-M" to distinguish these modified aluminum hydroxides from the gibbsite and diaspore solubility already in GWB. The Russel gibbsite-M and diaspore-M were used for modeling the SRS 3H Evaporator solutions. The data for the solubility of NaAlO_2 and AlO_2^{2-} of Reynolds and Herting⁴⁹ were also added to GWB for

^f bayerite is the gamma aluminum trihydrate

^ø boehmite is the gamma aluminum monohydrate

completeness. Detailed descriptions of the manner in which the data were added to the GWB database appear in Part I.³

The SRS solubility specific data of Mensah et al⁸ were added to the database for the NAS_{gel} , Zeolite-A, nitrated sodalite, and nitrated cancrinite. The manner in which the aluminosilicate data were added to the GWB is discussed in Appendix B for the NAS_{gel} and Zeolite-A which are discussed in this study. The database modifications for the nitrated aluminosilicates are discussed in Part V.⁹

5.0 PROCESS MODELING FOR NOMINAL EVAPORATOR OPERATION

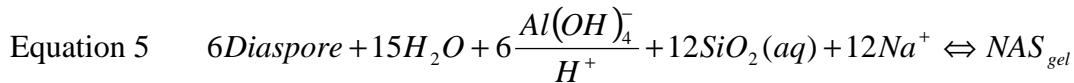
The new solubility data for NAS_{gel} precipitation developed by Mensah et al⁸ of the University of Southern Australia (USA) have been incorporated into a revised thermodynamic model for the SRS evaporators. A nominal evaporation model is developed with a pooled operating temperature data set (120°C for the 2H and 2F Evaporators and 140°C for the 3H Evaporator) in order to understand the importance of temperature on the model. The nominal process model is examined at a nominal 40% evaporation. The nominal evaporation model is based on 27 feed tank data points analyzed at SRTC including data from 1995 to 2002 from all three SRS evaporators (Tables in Part I,³ Part II,⁴ and this study). In Sections 5.2 and 5.3 it is shown that the model is relatively insensitive to evaporator operating temperature but more dependent on the percent evaporation. In Section 6.1 the model is validated with an orthogonal latin hypercube (OLH) design in the 120-140°C range at the nominal evaporation of 40% and in Section 6.2 with drop tank data. This demonstrates that tank chemistry can be simulated using the OLH approach when the solution concentration distributions (Gaussian or lognormal) and chemical ranges are matched.

In Section 7.0 a final evaporator model is developed over a wider composition region to accommodate future evaporator liquors to be processed. A temperature term and percent evaporation or evaporator solution density is added to the final process model as well. The final model is based on ~200 simulated evaporator solutions calculated over the wider composition region, broader temperature and percent evaporation intervals via an orthogonal latin hypercube (OLH) design.

The stoichiometry of the reaction that forms the NAS_{gel} from solution or from silica sols governs the process control model, e.g. the abscissa. The amorphous aluminosilicate gel precursor of Ejaz⁶ was the stoichiometry used in the first SRS evaporator process model (0.93Na₂O:1Al₂O₃:2.32SiO₂:5.15H₂O) which is Na₁₂Al₁₂Si₁₄O₅₂•31H₂O stoichiometry. It is very similar to that reported by Bosnar and Subotic²⁶ but not identical (see Section 2.4). Mensah et. al.⁸ chemically analyzed the NAS_{gel} and it was this gel that was subsequently used for solubility testing in SRS simulated evaporator solutions up to 12M NaOH. His composition, is 0.996Na₂O:Al₂O₃:1.994SiO₂:4.5H₂O which in this study is rounded to Na₂O:Al₂O₃:2SiO₂:4.5H₂O or Na₁₂Al₁₂Si₁₂O₄₈•27H₂O.

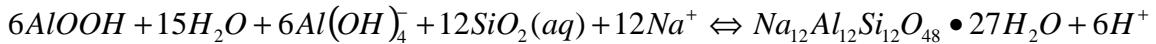
Geochemist's Workbench assumes that the NAS_{gel} is formed from solution species, since the database does not have any solubility data for a silica sol. The equations that represent the saturation of the solution with respect to the NAS_{gel} are defined by the steady state equilibrium

boundary on the activity diagrams which separates the field of AlOOH (diaspore) from the field of NAS_{gel} at elevated temperatures. The equation of that boundary as given in GWB is shown by Equation 5.



Equation 5 can be rewritten as

Equation 6



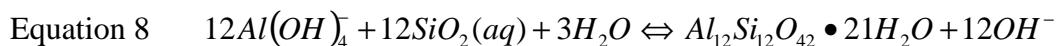
where the NAS_{gel} formula $Na_{12}Al_{12}Si_{12}O_{48} \bullet 27H_2O$ is the chemical composition from Mensah et. al.⁸ as given in Section 2.4 above.

Use of Equation 6 for the development of the process control algorithm would have resulted in relying on a measurement of the pH which is inherently inaccurate at pH values of >13 ,^{7, 50} the pH values reported for the SRS evaporator feeds. Since free hydroxide is routinely measured for the SRS evaporators and it is a more accurate measurement than the pH this term was substituted in Equation 6. Likewise, the Na^+ should be expressed as NaOH consistent with Equation 1 and the work of Mattigod and McGrail.⁵¹ Since the kinetics of the formation of AlOOH is slow, on the order of hours to days, all the aluminum species can be represented as Al(OH)_4^- and Equation 6 rewritten in terms of the hydroxide species as shown in Equation 7:



There is a high statistical co-linearity between $\log Na(M)_{calc}$ and $\log OH(M)$ in the SRS evaporator solutions modeled in this study since $\log OH(M)$ is the major component in the equation defining $Na(M)_{calc}$ (see Equation 4 where $OH(M)$ is expressed as NaOH). This is not surprising since the main component of the evaporator solutions is NaOH.

Because of the co-linearity of $\log Na(M)_{calc}$ and $\log OH(M)$, Equation 7 is rewritten subtracting out the NaOH term:



The K_{sp} for this reaction is

$$\text{Equation 9} \quad K_{sp}(NAS_{gel}) = \frac{[NAS_{gel}][OH^-]^{12}}{[Al(OH)_4^-]^{12}[SiO_2(aq)]^{12}[H_2O]^3}$$

Equation 9 can be further simplified since the NAS_{gel} and the water are in their standard states and equal to 1 as shown in Equation 10

$$\text{Equation 10} \quad K_{sp}(NAS_{gel}) = \frac{[OH^-]^{12}}{[Al(OH)_4^-]^{12}[SiO_2(aq)]^{12}}$$

or in logarithmic form

$$\text{Equation 11} \quad \log K_{sp}(NAS_{gel}) = 12\log[OH^-] - 12\log[Al(OH)_4^-] - 12\log[SiO_2(aq)]$$

Rewriting Equation 11 in terms of the species measured in the SRS Evaporator feed tanks, e.g. Al(M), Si(M), OH(M), multiplying both sides by -1 , gives the following equation:

$$\text{Equation 12} \quad -\log Q(NAS_{gel})_{25^\circ C} = 12\log[Al(M)] + 12\log[Si(M)] - 12\log[OH(M)]$$

Equation 12 represents the formation of the aluminosilicate “cage” structure of the NAS_{gel} . Basing the SRS evaporator process control model on Equation 12 allowed an ordinary least squares (OLS) correlation of the measured ambient feed tank concentrations to their potential to saturate in the evaporator pot after a 40 wt % nominal evaporation (Figure 6). This nominal model is based only on three compositional parameters that are routinely measured in the tank farm, e.g. $\log[Al(M)]$, $\log[Si(M)]$, and $\log[OH(M)]$ at a nominal evaporation of 40% and an operating temperature interval of 120-140°C. The OLS correlation between evaporator pot saturation and ambient feed tank chemistry is given in Equation 13 and defined as the nominal SRS evaporator model derived from the SRS specific solubility data.⁸

$$\text{Equation 13} \quad \log(Q/K)_{NAS_{120-140^\circ C / 40\% evap}} = \frac{37.4848 + 1.0949(12\log[Al(M)] + 12\log[Si(M)])}{-12\log[OH(M)]}$$

where the tank chemistry is expressed on the RHS of Equation 13, hereafter referred to as $\log Q(NAS)_{25^\circ C}$, and the supersaturation index of the feed in the evaporator pot is expressed on the LHS, hereafter referred to as $\log(Q/K)_{NAS}$. Note that the temperature affects on the solution concentrations are taken into account by GWB during the calculation of the LHS of the equation. The R^2 of the OLS correlation given Equation 13 is 0.93 based on variable depth data analyzed only by SRTC for the evaporator feed tanks, a total of 27 data points (Figure 6). The intercept includes the evaporation term, the numeric conversions from molar to molal concentrations, corrections for the activity coefficients, and temperature corrections for the solubility of the solid species, diaspore and NAS_{gel} . The stoichiometry of the x-axis is defined by the stoichiometry of the NAS_{gel} and cannot be applied to phases with other stoichiometry.

5.1 Comparison of Evaporator Models Based on Mensah vs. Ejaz

The SRS evaporator model generated based on the data of Ejaz (Parts I,³ II,⁴ and III⁵ of this study) versus the model developed based on the SRS evaporator specific solubility data⁸ is shown in Figure 7. The NAS_{gel} measured by Mensah et al⁸ is more soluble than the NAS_{gel} measured by Ejaz⁶ and the solubility is a strong function of $OH^- (M)$ concentration. Therefore, the dependency of the process control model using the data of Ejaz had a factor of 6 log OH^- while the model based on the data of Mensah has a factor of 12 dependency. This can be seen by the comparison of the solubilities shown in Appendix B (Figure B-1).

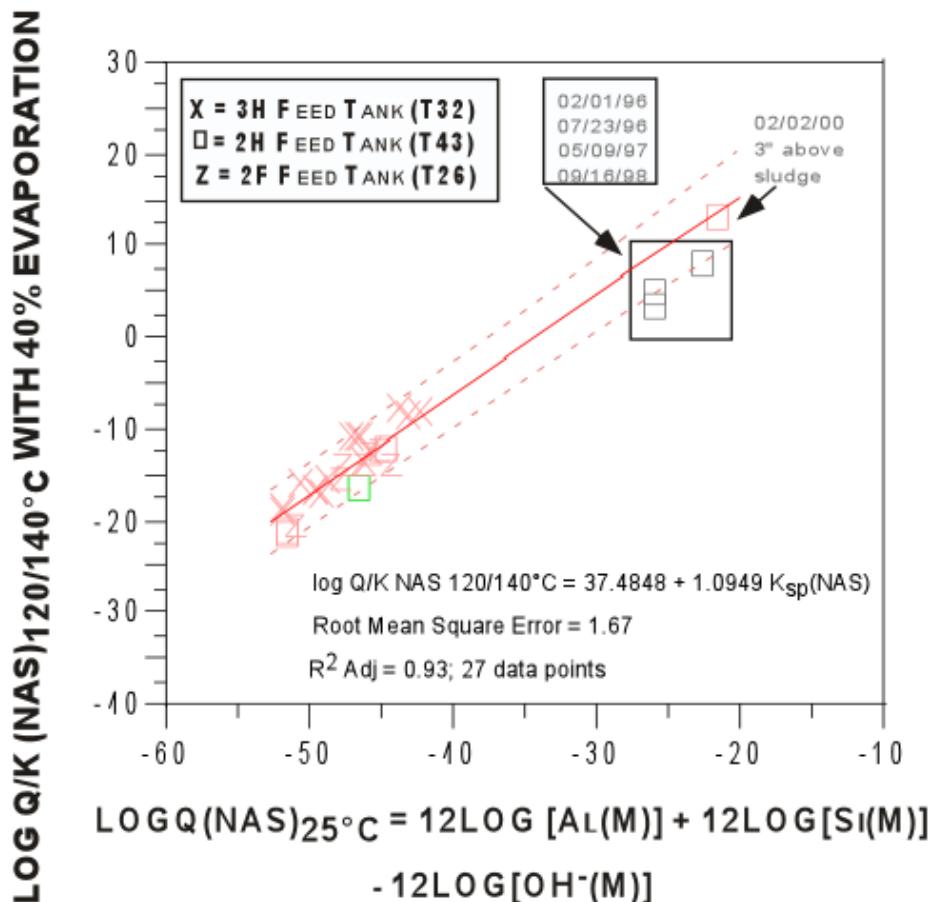


Figure 6. Nominal process control model for the SRS evaporators based on the solubility data of Mensah.⁸ The model is based on the equilibrium between diasporite and NAS_{gel} represented on the activity diagrams in Part I³ and Equation 13. It provides a correlation between ambient feed tank chemistry and saturation of the feed tank solutions in the evaporator assuming a nominal 40 wt % evaporation at temperatures in the range of 120-140°C.

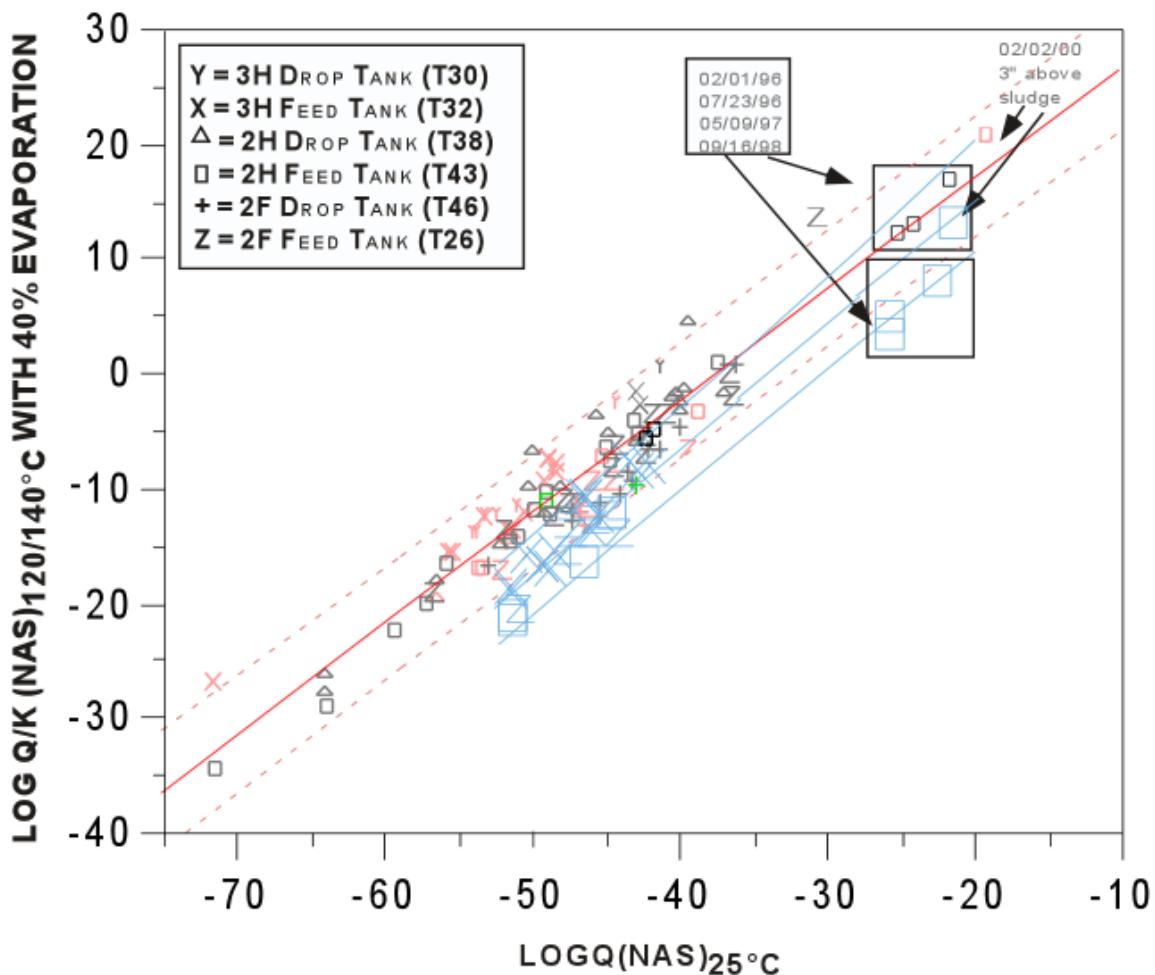


Figure 7. Comparison of the evaporator process control model based on the data of Ejaz⁶ (red) generated from the Bayer alumina industry aluminosilicate solubility and the data of Mensah et al.⁸ (blue) generated in SRS simulated evaporator solutions.

Since the NAS_{gel} solubility measured by Mensah et.al.³ is higher than those measured by Ejaz, the evaporator solutions are more undersaturated with respect to NAS_{gel} when modeled using the Mensah et. al.⁸ data. This is demonstrated on the activity diagram representation where it can be seen that the boundary between the NAS_{gel} and AlOOH has shifted to higher $\log \text{SiO}_2(\text{aq})$ activities (see Figure 8). This is also seen on the $\log Q/K(\text{NAS})_{120/140^\circ\text{C} \text{with } 40\% \text{ evaporation}}$ vs. $\log Q(\text{NAS})_{25^\circ\text{C}}$ where the process model based on the Mensah data is always calculated to have lower (more negative) $\log Q/K(\text{NAS})_{120/140^\circ\text{C} \text{with } 40\% \text{ evaporation}}$ undersaturated values compared to the Ejaz data (see Figure 7).

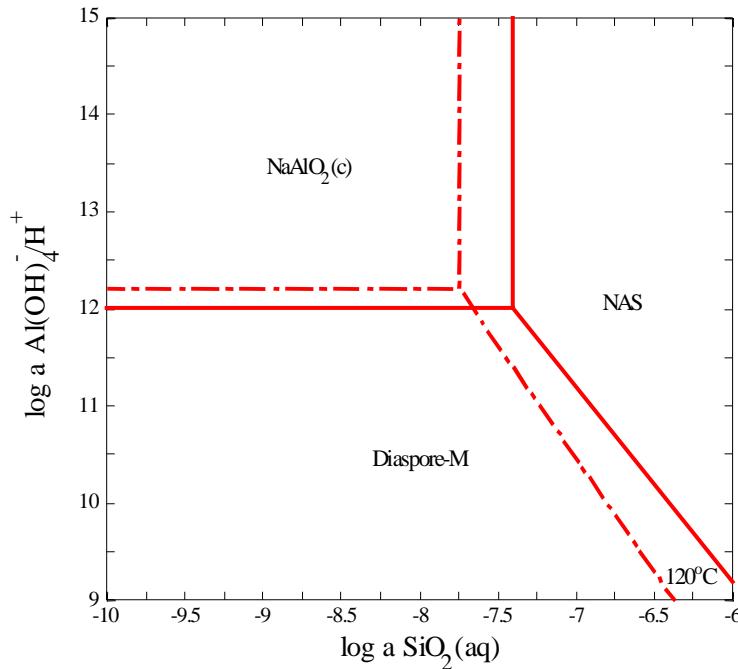


Figure 8 Shift of the NAS_{gel} -diaspore boundary based on the solubility data of the NAS_{gel} in SRS simulated evaporator solutions as measured by Mensah et. al. (solid lines)⁸ compared to the solubility boundary calculated using the data of Ejaz (dashed line). Diagram generated with composition of evaporator solution FTF-046.

5.2 Sensitivity to Evaporator Operating Temperature

The nominal evaporator process model was generated using a pooled temperature data set where some of the $\log(Q/K)_{\text{NAS}}$ values had been calculated at 120°C and some had been calculated at 140°C. The $\log(Q/K)_{\text{NAS}}$ saturation values had been calculated at 120°C for the SRS 2H and 2F Evaporator feed tanks since these evaporators ran at ~120°C^f during the time period modeled in Part I³ of this study. The $\log(Q/K)_{\text{NAS}}$ saturation values had been calculated at 140°C for the SRS 3H Evaporator since it ran between 135-140°C (data from Kent Gilbreath March 2001) during the time period modeled in Part I³ of this study. The pooled data set was used for the following reasons:

- The pooled data spanned the actual operating temperatures of the evaporation that had been performed
- Figure B-1 in Appendix B demonstrates that the solubility of the NAS_{gel} as taken from the literature is a linear function of $1/T(K)$ for the data examined.

^f Between 1996 and 1999 when the 2H evaporator was shut down, it ran at a nominal temperature of 120-125°C but ranged from a low of 99°C (12/06/97 morning report) to a high of 139°C (5/16/98 morning report).

Currently, the 3H Evaporator is running at temperatures as high as ~180°C. Therefore, the applicability of the model over the range of operating conditions for all SRS evaporators, e.g., from 100°C to 180°C, was investigated to further evaluate the dependency of the $\log(Q/K)_{\text{NAS}}$ saturation values in Figure 6 to temperature.

In order to evaluate the solution equilibrium at elevated temperatures, the solution temperature was incrementally increased in GWB. These calculations simulated evaporation by a stepwise removal of 40 wt % of the water from the solution. This amount of evaporation changes the solution density from about 1.4 g/cm³ to about 1.6 g/cm³, the latter number being the operational target density for the SRS Evaporators.

The temperature variation was evaluated by fitting OLS models to the 27 feed compositions (representing all the evaporator systems) at 120°C, 140°C, 160°C, and 180°C. A comparison was then made of the upper and lower temperature bounds to the nominal evaporator process model developed with the pooled 120°C/140°C data set (Equation 13). The relation of the upper temperature bound to the lower temperature bound was also evaluated.

Usage of the Mensah⁸ solubility data at temperatures above 130°C is complicated by the rapidity of the kinetics of the formation of NAS_{gel} . However, Figure 5 demonstrates that the NAS_{gel} persists up to 175°C while the crystalline species are forming. Mensah et. al.⁸ found that they could not “quench” phase pure NAS_{gel} samples rapidly enough to prevent the formation of Zeolite-A at temperatures above 130°C in 6M Na solutions nor above 65°C in 12M Na solutions. Therefore, the data for NAS_{gel} input into Geochemist’s Workbench (see Appendix B) is an extrapolation of solubility data derived by Mensah et. al.⁸ at 30°C, 65°C and 130°C in 6M Na solutions and extrapolations of NAS_{gel} solubility at 30°C and 65°C in 12M Na. An increasingly large field of crystalline NaAlO_2 intersects the field of NAS_{gel} on the activity (stability) diagrams as temperature is increased (see Figure 9). This can be potentially important when modeling drop tank compositions that are higher in Na^+ and Al(OH)_4^- composition as illustrated by the blue stability diagram in Figure 9 overlain on the red feed tank stability diagram. However, Equation 13 applies to both the stable and the metastable equilibrium between AlOOH and NAS_{gel} as shown by the dashed lines on Figure 9. This means that the nominal process model assumes that any evaporator solution in the field of NaAlO_2 can metastably precipitate NAS_{gel} more rapidly than the stable NaAlO_2 phase. Although kinetics on the precipitation of NaAlO_2 is not available, the rapidity of the kinetics of NAS_{gel} precipitation observed by Mensah et. al.⁸ and the researchers at ORNL²⁹ supports this assumption.

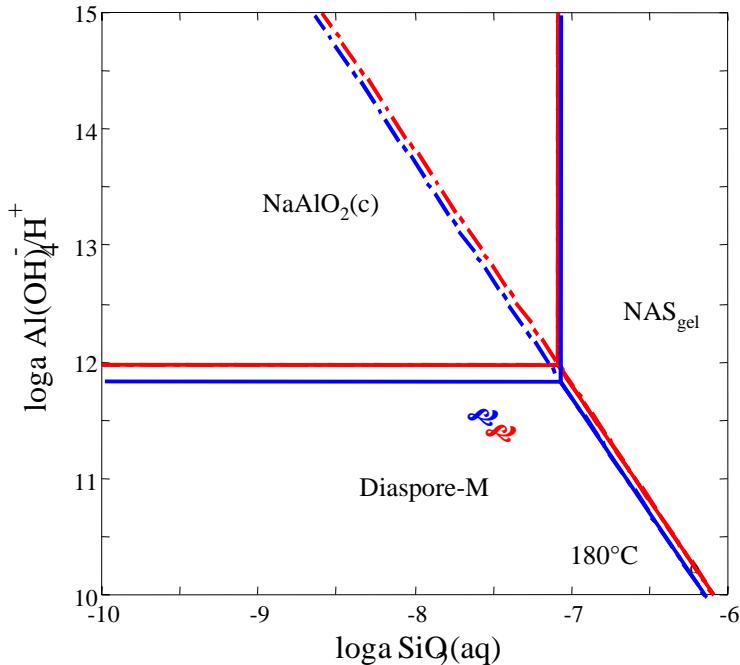


Figure 9. Metastable extension of the equilibrium between AlOOH and NAS_{gel} into the stability field of NaAlO_2 for feed tank samples HTK-480-482 (red) and drop tank samples HTK-505-507 (blue) at 180°C.

In order to evaluate the temperature effects on the nominal process control model, the $\log(Q/K)_{\text{NAS}}$ values were calculated at 120°C for the 27 feed tank compositions. The 120°C temperature represents the lower bounding temperature at 40 wt % evaporation (Equation 14). Similarly, the $\log(Q/K)_{\text{NAS}}$ values were computed for all feed tank compositions at 180°C and 40 wt % evaporation to provide an upper bound for evaporator operations (Equation 17). Calculations at 140°C and 160°C and 40 wt % evaporation are provided as intermediate cases (Equation 15 and Equation 16).

$$\text{Equation 14} \quad \log Q/K_{\text{NAS} @ 120^\circ\text{C}} = 37.1861 + 1.1012 \log Q(\text{NAS})_{25^\circ\text{C}}; R^2=0.96$$

$$\text{Equation 15} \quad \log Q/K_{\text{NAS} @ 140^\circ\text{C}} = 38.0360 + 1.1000 \log Q(\text{NAS})_{25^\circ\text{C}}; R^2=0.96$$

$$\text{Equation 16} \quad \log Q/K_{\text{NAS} @ 160^\circ\text{C}} = 37.7169 + 1.0926 \log Q(\text{NAS})_{25^\circ\text{C}}; R^2=0.96$$

$$\text{Equation 17} \quad \log Q/K_{\text{NAS} @ 180^\circ\text{C}} = 35.6447 + 1.0781 \log Q(\text{NAS})_{25^\circ\text{C}}; R^2=0.96$$

Comparison of Equation 13 to Equation 14 and Equation 15 indicates that the response of Equation 13 is intermediate between Equation 14 and Equation 15 since 12 solution $\log(Q/K)_{\text{NAS}}$ values were calculated at 120°C while the remaining 15 solution $\log(Q/K)_{\text{NAS}}$ values were calculated at 140°C. Comparison of Equation 14 and Equation 15 indicates that the slopes of the low temperature (120°C) saturation correlation and the high temperature (180°C) saturation correlation differ by 0.023. The main difference in the prediction of saturation at the lower

temperature (120°C) and upper temperature (180°C) evaporator operating temperature bound is expressed in the intercept term that is 1.54 smaller at the higher temperature, e.g. the NAS_{gel} is more soluble at higher temperature.

Due to the similarity of the slopes of Equation 13 through Equation 17, one can solve these equations at a fixed log Q(NAS)_{25°C} and demonstrate that the 120°, 140°C, 160°C, and 180°C variation in log Q/K_(NAS) varies little with temperature (see Table IV). In this case a log Q(NAS)_{25°C} of -30.00 was chosen to demonstrate that there is little impact on the calculated log Q/K_(NAS)_{25°C} between 120-180°C. The lack of a strong dependency of the aluminosilicate saturation on temperature was previously demonstrated in Part III⁵ of this study.

Table IV. Sensitivity of Log (Q/K)_{NAS} at Varying Evaporator Operating Temperatures

Temperature	Equations Used	Corresponding Log Q/K _(NAS) at log Q(NAS) _{25°C} of -30.00
140°C	Equation 15	+5.04
160°C	Equation 16	+4.94
120/140°C pooled	Equation 13	+4.64
120°C	Equation 14	+4.15
180°C	Equation 17	+3.30

5.3 Sensitivity to Percent Evaporation

The nominal evaporator process model given in Equation 13 was generated assuming an evaporation of 40 wt %. During routine operation the evaporators do not always achieve 40 wt %. This is especially true when the evaporator solutions approach their operational target density of 1.6 g/cm³. Therefore, upper and lower bounds on evaporation were calculated spanning 0 wt% to 60 wt % evaporation. Since the temperature effects on the model were shown (see Section 5.2) to be minimal, the varying evaporation percentages are calculated using the pooled 120°C/140°C data set. The calculation for the 27 data points from the evaporator feed tanks gives the following equations for a variety of other evaporation rates:

$$\text{Equation 18} \quad \text{Log } Q/K_{(\text{NAS}) @ 0 \text{ wt \% evaporation}} = 32.9085 + 1.0832 \log Q (\text{NAS})_{25^\circ\text{C}}; R^2=0.94$$

$$\text{Equation 19} \quad \text{Log } Q/K_{(\text{NAS}) @ 10 \text{ wt \% evaporation}} = 33.8403 + 1.0856 \log Q (\text{NAS})_{25^\circ\text{C}}; R^2=0.94$$

$$\text{Equation 20} \quad \text{Log } Q/K_{(\text{NAS}) @ 20 \text{ wt \% evaporation}} = 34.8898 + 1.088 \log Q (\text{NAS})_{25^\circ\text{C}}; R^2=0.94$$

$$\text{Equation 21} \quad \text{Log } Q/K_{(\text{NAS}) @ 30 \text{ wt \% evaporation}} = 36.0886 + 1.0913 \log Q (\text{NAS})_{25^\circ\text{C}}; R^2=0.94$$

$$\text{Equation 22} \quad \text{Log } Q/K_{(\text{NAS}) @ 50 \text{ wt \% evaporation}} = 39.1522 + 1.0992 \log Q (\text{NAS})_{25^\circ\text{C}}; R^2=0.94$$

$$\text{Equation 23} \quad \text{Log } Q/K_{(\text{NAS}) @ 60 \text{ wt \% evaporation}} = 41.2160 + 1.1045 \log Q (\text{NAS})_{25^\circ\text{C}}; R^2=0.94$$

Due to the similarity of the slopes of Equation 13 and Equation 18 through Equation 23, one can solve these equations at a fixed $\log Q(\text{NAS})_{25^\circ\text{C}}$ (see Table V). As with the temperature sensitivity analysis a $\log Q(\text{NAS})_{25^\circ\text{C}}$ of -30.00 was chosen to demonstrate that the 10-60% evaporation data fell within the 95% error bands associated with Equation 13. There is a stronger dependency of the aluminosilicate saturation on evaporation than on temperature as was demonstrated in Part III⁵ of this study.

The sensitivity of aluminosilicate saturation to evaporation can also be accessed by solving Equation 13 and Equation 18 through Equation 23 at $\log Q/K_{(\text{NAS})} = 0$ and fitting an OLS regression to the calculated $\log Q(\text{NAS})_{25^\circ\text{C}}$ (see Figure 10). The OLS regression takes the form

Equation 24 $\log Q(\text{NAS})_{25^\circ\text{C}} = -32.1114 - 0.1119(\% \text{Evaporation}) + 0.0165(\text{Operating Temp } ^\circ\text{C})$
with an $R^2=0.95$ and RMS of 0.52.

The coefficients in Equation 24 demonstrate that evaporation and operating temperature have opposite effects, increased evaporation causes decreased solubility of components while increased temperature causes increased solubility of components. The coefficients in Equation 24 demonstrate that evaporation is a factor of 10 more significant than operating temperature. Due to the insignificance of the temperature term, and the fact that higher temperature causes increased solubility of components, the temperature term can be eliminated from Equation 24 which then becomes:

Equation 25 $\log Q(\text{NAS})_{25^\circ\text{C}} = -29.9434 - 0.1092 (\% \text{Evaporation})$

with an $R^2=0.93$ and RMS of 0.57.

Equation 25 can be implemented once the chemistry of a given solution is known by monitoring percent evaporation.

Table V. Sensitivity of Log $(Q/K)_{\text{NAS}}$ at Varying Evaporations

Percent Evaporation	Equations Used	Corresponding Log $Q/K_{(\text{NAS})}$ at $\log Q(\text{NAS})_{25^\circ\text{C}}$ of -30.00
60	Equation 23	+8.08
50	Equation 22	+6.18
40% nominal	Equation 13	+4.64
30	Equation 21	+3.35
20	Equation 20	+2.24
10	Equation 19	+1.27
0	Equation 18	+0.41

Table VI. Sensitivity of Aluminosilicate Supersaturation to Evaporation and Temperature

Temperature (°C)	Percent Evaporation	Equations Used	Corresponding log Q(NAS) _{25°C} at Log Q/K _(NAS) of Zero
120/140 pooled*	60	Equation 23	-37.32
120/140 pooled*	50	Equation 22	-35.62
120	40% nominal	Equation 14	-33.77
120/140 pooled*	40% nominal	Equation 13	-34.24
140	40% nominal	Equation 15	-34.57
160	40% nominal	Equation 16	-34.52
180	40% nominal	Equation 17	-33.06
120/140 pooled*	30	Equation 21	-33.07
120/140 pooled*	20	Equation 20	-32.06
120/140 pooled*	10	Equation 19	-31.17
120/140 pooled*	0	Equation 18	-30.38

* an average value of 130°C is used to generate Figure 10

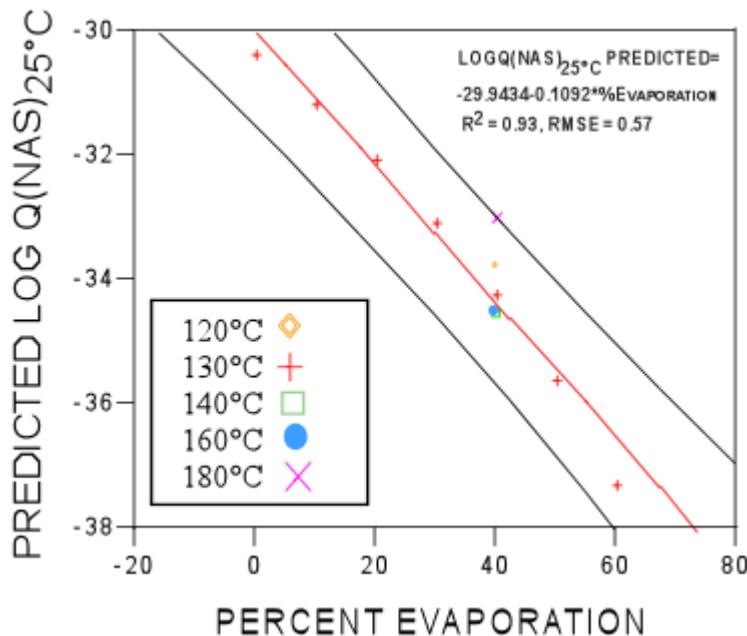


Figure 10. Relation of log Q (NAS)_{25°C} to percent evaporation and evaporator operating temperature.

6.0 VALIDATION OF NOMINAL PROCESS CONTROL MODEL

6.1 Orthogonal Latin Hypercube (OLH) Analysis

The maximum and minimum values given in Table VII were used to generate the nominal process model given in Equation 13 and shown in Figure 6. In order to validate Equation 13, an Orthogonal Latin Hypercube (OLH) matrix was developed using the maximum and minimum compositions and temperatures shown in Table VII. A nominal evaporation of 40% was used for all the calculations.

Table VII. Ranges Modeled in Section 5.0 (Feed Tank Data from 1995-2002)

	Minimum (M)	Maximum (M)
Al (M)	0.11	1.1
Cl (M)	0.003	0.02
CO ₃ (M)	0.005	0.43
C ₂ O ₄ (M)	0.0025	0.0063
F (M)	0.0027	0.01
Fe (M)	0.005	0.36
NO ₂ (M)	0.80	2.5
NO ₃ (M)	0.89	3.42
OH (M)	1.95	10.4
K (M)	0.01	0.085
PO ₄ (M)	0.006	0.013
SO ₄ (M)	0.0063	0.03
Si (M)	2.00E-05	0.143
U (M)	1.07E-05	0.002
Na _{calc} (M)	5.21	17.67
Temperature (°C)	120	140
Evaporation Fraction	0.4	0.4

Note that in the reprotoed minimum [Fe] in the feed tank was 0.0M. Therefore, one half the detection limit for this element was substituted for the minimum [Fe]. The Na⁺_{calc}(M) values shown in Table VII are defined by the remaining solution species via the relationship given in Equation 4.

During this study it was determined that design of the OLH factor space was dependent upon whether the solution concentrations exhibited a lognormal or Gaussian distribution. If the solution concentrations are lognormal, then the Orthogonal Latin Hypercube (OLH) designs should be developed using log([]) values. If the solution concentrations are Gaussian in nature then the OLH designs should be developed on the molar compositions shown in Table VII and not the log of these values. In order to validate the nominal process control model (Equation 13), the distribution of the 27 SRTC feed solutions in terms of OH⁻(M) and Na⁺_{calc}(M) values calculated from measured analyses were examined. Figure 11 demonstrates that the distributions of the measured data were Gaussian and hence the validation was performed by designing the

OLH simulated solutions based on the molar concentrations in Table VII and not the log of the concentrations.

An OLH design of 513 simulated solutions at temperatures varying between 120-140°C at 40% nominal evaporation was calculated. The OLH design can, however, create unrealistic combinations of evaporation and sodium content. For example, the OLH may have an evaporation of 40% for a starting sodium content of 16 M. This evaporation would yield an unachievable high final sodium concentration. Therefore, a screen was developed to eliminate these unrealistic combinations.

First, it is assumed that the highest possible final sodium concentration in the evaporators is 19 M. This corresponds to 50%wt NaOH in water. Second, the maximum possible evaporation is calculated from the starting sodium concentration:

Equation 26

$$\text{Max Evap} = 1 - \frac{\text{Na}(M)}{19}$$

where $\text{Na}(M)$ is the initial sodium content.

Finally, the calculated maximum evaporation is compared to the evaporation in the OLH. If the OLH evaporation is higher than the calculated maximum, this combination of evaporation and composition is excluded from the OLH.

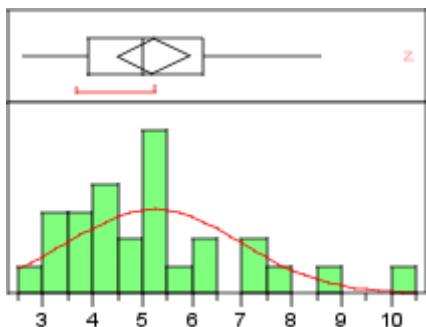
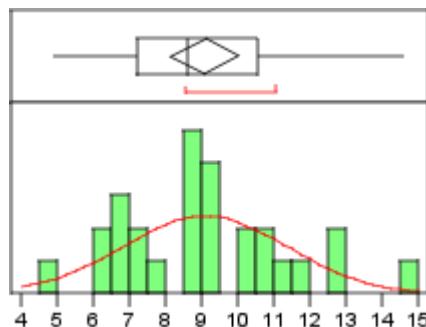
 $\text{OH}^-(\text{M})$ in Feed Tank Solutions Used in Development of Equation 13 **$\text{Na}^{+}_{\text{calc}}(\text{M})$ in Feed Tank Solutions Used in Development of Equation 13**

Figure 11. Gaussian distribution of $\text{OH}^-(\text{M})$ and $\text{Na}^{+}_{\text{calc}}(\text{M})$ in feed tank solutions used to define the nominal process model. The red line represents an ideal Gaussian distribution.

The Equation 26 screening tool eliminated 258 of the 513 OLH simulated solutions leaving another 255 for validation of the nominal process model, Equation 13. $\text{LogQ}(\text{NAS}_{\text{gel}})_{25^\circ\text{C}}$ values were calculated for the 255 simulated solutions from Equation 12 and these were fitted to the

255 calculated $\log(Q / K)_{NAS\ 120-140^{\circ}C / 40\% evap}$ values determined from GWB via an ordinary least squares (OLS) analysis. The OLS generated the validation Equation 27 given below:

$$\text{Equation 27} \quad \log(Q / K)_{NAS\ 120-140^{\circ}C / 40\% evap} = \frac{37.3584 + 1.0839(12\log[Al(M)] + 12\log[Si(M)])}{-12\log[OH(M)]}$$

Equation 13 the nominal process control model is shown below to be very similar in slope and intercept.

$$\text{Equation 13} \quad \log(Q / K)_{NAS\ 120-140^{\circ}C / 40\% evap} = \frac{37.4848 + 1.0949(12\log[Al(M)] + 12\log[Si(M)])}{-12\log[OH(M)]}$$

To assess how well Equation 13 fits the validation data generated by the OLH, the residuals calculated from the difference between this equation and the GWB OLH predictions can be assessed (see Figure 12). The distribution of the residuals are shown to be Gaussian and to vary around the prediction by $\pm 4 \log(Q / K)_{NAS\ 120-140^{\circ}C / 40\% evap}$.

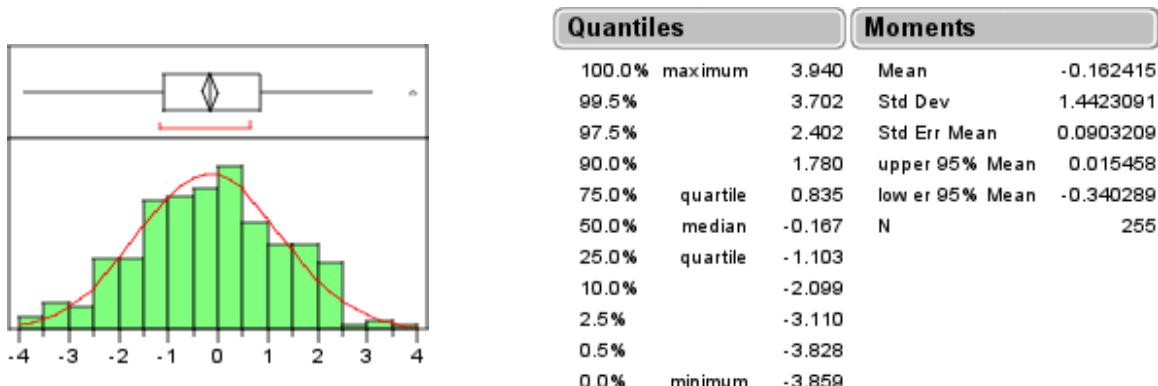


Figure 12 Assessment of the nominal process control model (Equation 13) to the OLH validation data.

The nominal process control model generated via the OLH analysis, e.g. Equation 27, is also compared to the nominal feed tank process control model, e.g. Equation 13, for the 27 feed tank compositions used to generate the nominal process control model (see Figure 13). Figure 13 indicates a slope of ~ 1 and an intercept of ~ 0 and an $R^2=1.0$ for an OLS regression between Equation 13 and Equation 27. Figure 13 validates the nominal process control model based on the highly leveraged feed tank data and demonstrates that the OLH statistical approach can be used to translate between statistically designed simulated SRS evaporator solutions and actual tank data.

6.2 Drop Tank Data

The nominal process model given in Equation 13] and shown in Figure 6 was generated using the 27 feed tank solutions analyzed by SRTC (see Table I and Table II). The corresponding 22 drop tank solution analyses generated by SRTC (see Table III) were used to validate the nominal process model developed from the 27 feed tank solutions. The OLS fit to the 22 drop tank solutions analyzed between 1995-2002 gives the following equation of best fit with an R^2 of 0.85:

$$\text{Equation 28} \quad \log(Q/K)_{\text{NAS } 120-140^\circ\text{C} / 40\% \text{ evap}} = \frac{35.1973 + 1.0306(12\log[Al(M)] + 12\log[Si(M)])}{-12\log[OH(M)]}$$

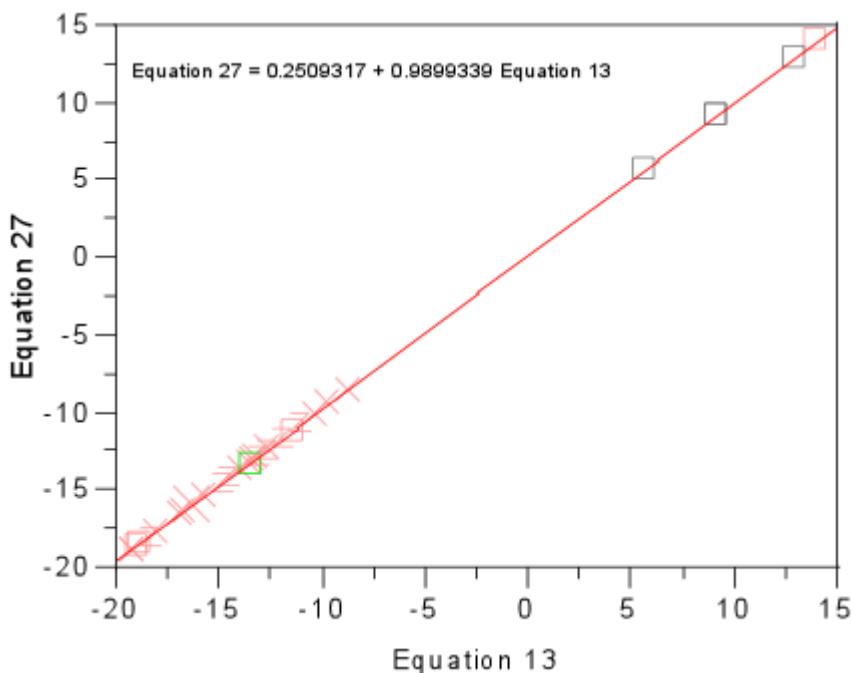


Figure 13. Correlation between the nominal process control model developed based on SRS evaporator feed tank data between 1995-2002 (Equation 13) and a set of simulated evaporator solutions generated by a composition and temperature space filling OLH design (Equation 27).

Comparison of Equation 13, the nominal process control model based on the feed tanks, to Equation 28, the nominal process control model based on the drop tanks, indicates a slope of <1.0, e.g. 0.94 and an intercept of ~0 (Figure 14). The slope <1.0 demonstrates a bias in the data from the drop tanks relative to the feed tanks.

The bias in the drop tank data is also shown in Figure 15 where the distribution of the differences in the predictions between Equation 13 (the nominal process control model) and the GWB predictions for the drop tank validation chemistries shows that the drop tanks are less supersaturated with respect to NAS_{gel} , e.g. undersaturated with respect to $\log(Q/K)$. This

indicates that a feed tank close to saturation, e.g. $\log(Q/K)_{\text{NAS}} \sim 0$ may supersaturate at the elevated evaporator temperatures with respect to NAS_{gel} but then precipitate in the drop tank. This is confirmed by recent findings of NAS crystalline products in the evaporator drop tanks.^{52,53} Precipitation in the evaporator is precluded since the $\log(Q/K)_{\text{NAS}}$ for these solutions is undersaturated at the evaporator operating temperature. Due to these complexities, the drop tank data was used for validation rather than for modeling.

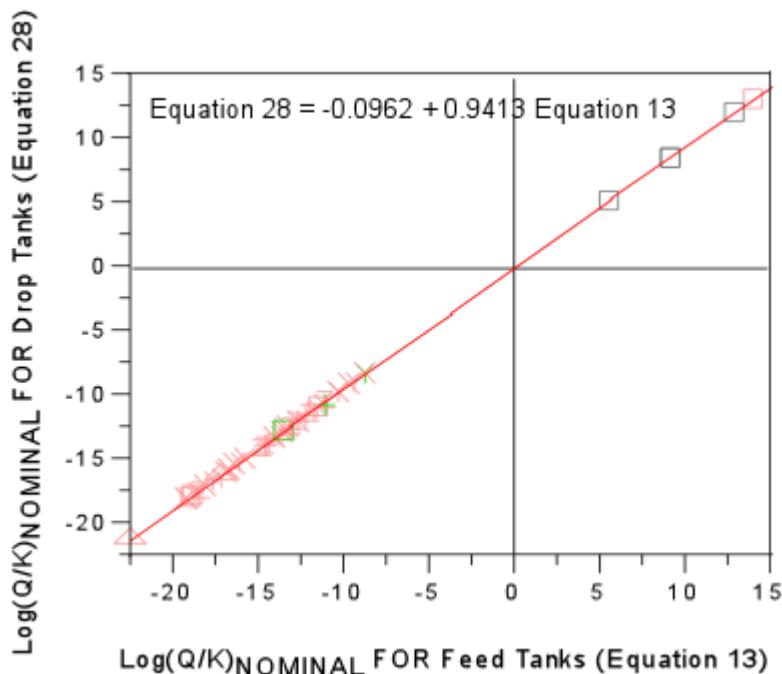


Figure 14. Bias in supersaturation between drop tank and feed tank data.

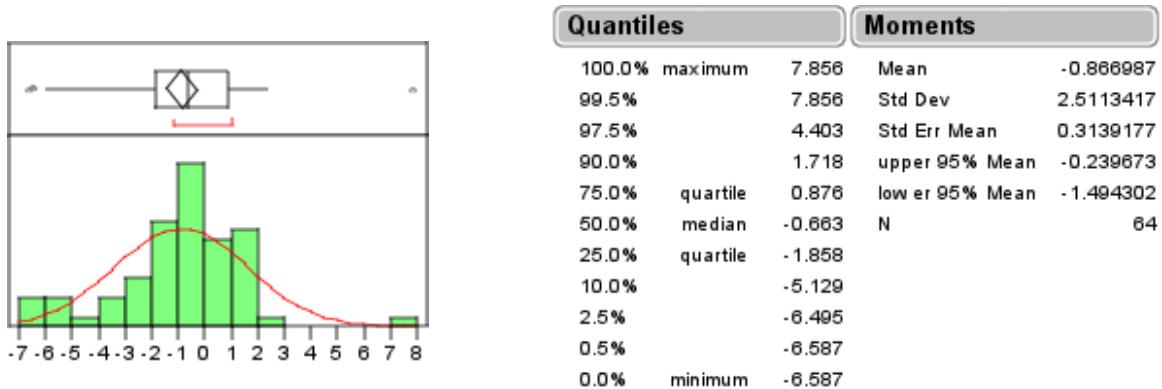


Figure 15. Assessment of the nominal process control model (Equation 13) to the drop tank validation data.

7.0 DEVELOPMENT OF AN EXPANDED EVAPORATOR PROCESS CONTROL MODEL

7.1 Orthogonal Latin Hypercube Design

The validation of the nominal process control model discussed in Section 6.1 demonstrates that the OLH statistical approach can be used to translate between statistically designed simulated SRS evaporator solutions and actual tank data. Since the exact evaporation and temperatures could only be approximated in the nominal evaporator process control model, a second expanded OLH statistical design can be used to incorporate wider composition ranges, temperature sensitivity, and percent evaporation sensitivity into an expanded process control model.

Reasonable maximum concentrations for $[NO_2]$, $[NO_3]$, and $[OH]$ in the tank farm were determined^f to be 4M, 7M, and 16M, respectively. Somewhat wider upper concentration bounds for $[NO_2]$, $[NO_3]$, and $[OH]$ of 6M, 7M, and 16M were used in modeling to investigate the expansion of this range. In addition, the temperature was varied between 100°C and 180°C and the evaporation percentage between 0 and 80%.

During this study it was determined that design of the OLH factor space was dependent upon whether the solution concentrations exhibited a lognormal or Gaussian distribution. If the solution concentrations are lognormal, then the Orthogonal Latin Hypercube (OLH) designs should be developed using $\ln([])$ values. If the solution concentrations are Gaussian in nature then the OLH designs should be developed on the molar compositions shown in Table VII and not the log of these values. For the nominal evaporator model based on SRTC data from 1995-2002, it was determined that the solution concentrations were Gaussian rather than lognormal and the OLH design was calculated in molar concentrations.

An analysis of the long term variation of tank farm concentrations between 1973-2001 (see data in Appendix A) demonstrated that the evaporator solution concentrations were lognormal (see Figure 16). Therefore, the OLH space filling designs for the expanded evaporator model were developed using $\ln([])$ values. These are provided in Table VIII (where because the minimum $[Fe]$ was 0.0, the minimum concentration for all those shown in the table—which is that for $[U]$ —was substituted for the minimum $[Fe]$).

^f D.T. Hobbs of SRTC

$\text{OH}^-(\text{M})$ in Feed Tank Solutions Over the Last 28 Years $\text{Na}^+_{\text{calc}}(\text{M})$ in Feed Tank Solutions Over the Last 28 Years

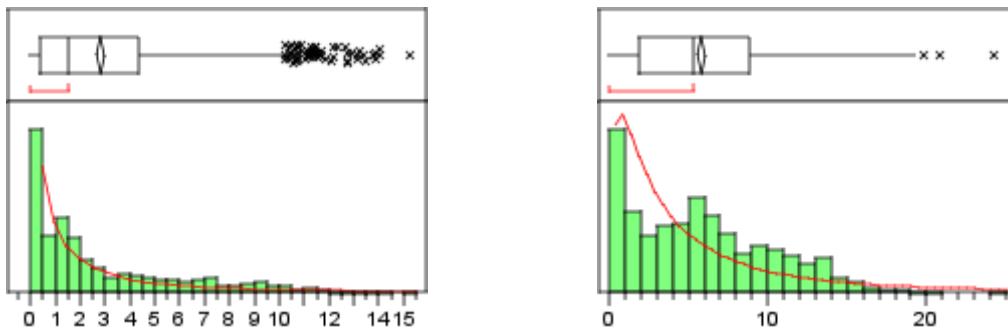


Figure 16. Lognormal distribution of tank farm solutions over 28 years (1973-2001).

Table VIII. Tank Farm Bounding Regions Including Logarithmic Transformations Used in the OLH Statistical Analysis

	Min	Min (log)	Max	Max (log)
Al (M)	0.005	-2.3010	4	0.6021
Cl (M)	0.00020	-3.6990	0.12	-0.9208
CO_3 (M)	0.005	-2.3010	2.875	0.4586
C_2O_4 (M)	0.0005	-3.3010	0.15	-0.8239
$[\text{CO}_3] + [\text{C}_2\text{O}_4]$	0.0055	-2.2596	3.025	0.4807
F (M)	0.00000526	-5.2840	0.2415	-0.6171
Fe (M)	0	-6.3010	0.3581021	-0.4460
NO_2 (M)	0.0921	-1.0357	6.0	0.7782
NO_3 (M)	0.0173	-1.7620	7.0	0.8451
$[\text{NO}_2] + [\text{NO}_3]$	0.1094	-0.9610	13	1.1139
OH (M)	0.01	-2.000	16	1.2041
K (M)	0.001215	-2.9154	0.5	-0.3010
PO_4 (M)	0.0005	-3.3010	0.145	-0.8386
SO_4 (M)	0.0005	-3.3010	0.8875	-0.0518
Si (M)	0.00002136	-4.6716	0.1785714	-0.7482
U (M)	5.00E-07	-6.3010	0.0155	-1.8097
Na (M)	0.2015	-0.6957	23	1.3617
Temperature($^{\circ}\text{C}$)	100		180	
Evap. Fraction	0		0.8	

The molar concentrations in the design matrix were then transformed into the corresponding molal concentrations per Equation 2 through Equation 4 and then the molal concentrations were analyzed with the REACT subroutine of GWB.

As shown in Section 6.1, the OLH design can create unrealistic combinations of evaporation and sodium content. For example, the OLH may have an evaporation of 40% for a starting sodium content of 16 M. This evaporation would yield an unachievable high final sodium concentration. Therefore, a screen was developed to eliminate these unrealistic combinations.

First, it is assumed that the highest possible final sodium concentration in the evaporators is 19 M. This corresponds to 50 wt% NaOH in water. Second, the maximum possible evaporation is calculated from the starting sodium concentration from :

$$\text{Equation 26} \quad \text{Max Evap} = 1 - \frac{\text{Na}(M)}{19}$$

where Na(M) is the initial sodium content.

Finally, the calculated maximum evaporation is compared to the evaporation in the OLH. If the OLH evaporation is higher than the calculated maximum, this combination of evaporation and composition is excluded from the OLH.

This maximum evaporation screening tool eliminated 122 of the original 513 design points. The GWB results for the remaining 401 data points are provided in Figure 17. The results do an excellent job of covering the saturation points (i.e., $\log(Q/K)_{\text{NAS}} = 0$) for the NAS_{gel} phase as shown in Figure 17. Also the biases in the model predictions appear to be reasonably distributed for the optimized design; noting that all deviations shown are biases and not the random measurement errors normally associated with such plots.

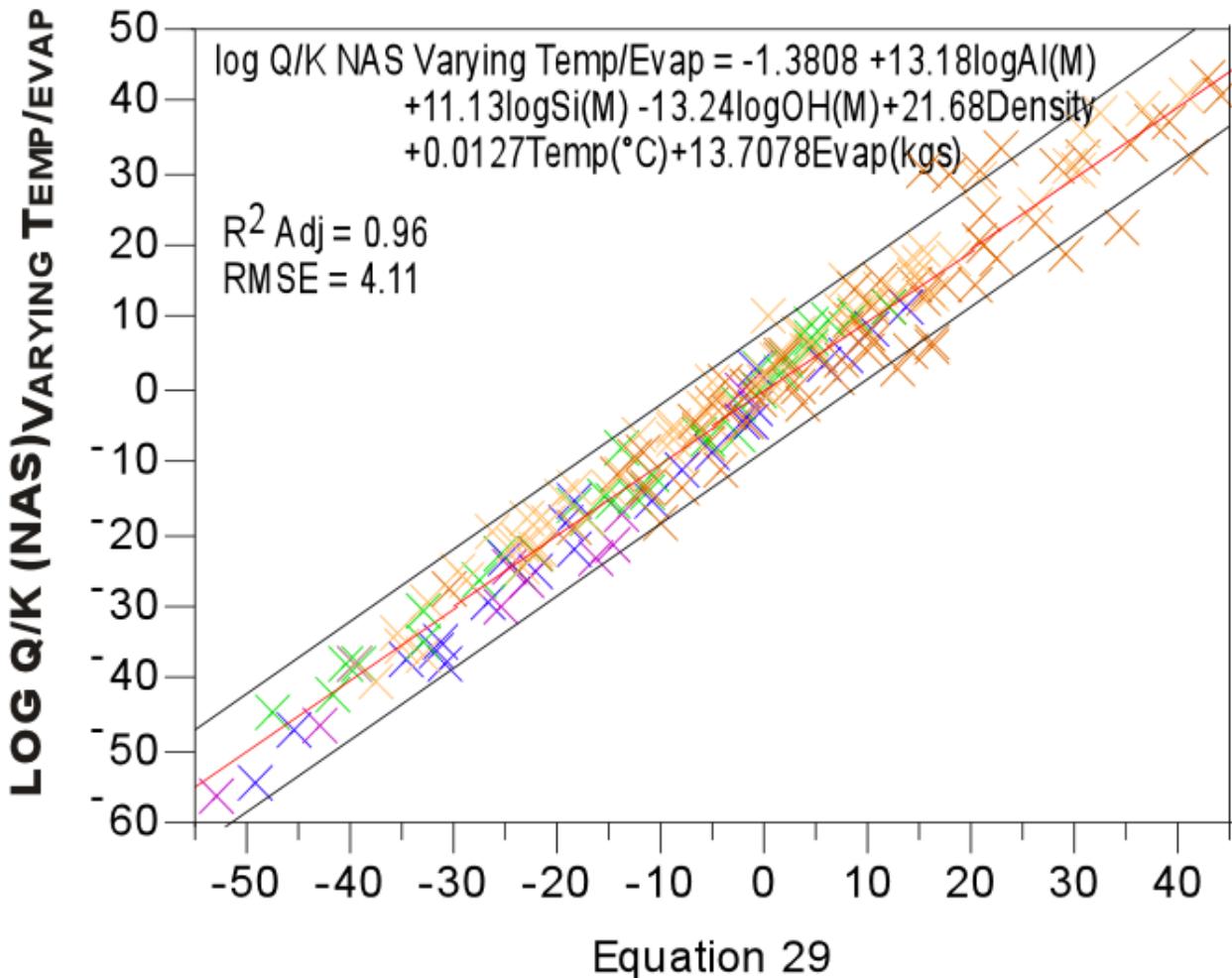


Figure 17. Bivariate Fit of $\log(Q/K)_{\text{NAS}}$ versus $\log Q(\text{NAS})_{25^\circ\text{C}}$ for the optimized Orthogonal Latin Hypercube model spanning 40°C-180°C and 0-80% evaporation. Note colors are associated with varying OH^- concentrations, warmer colors are lower OH^- concentration than cooler colors.

7.2 The OLH Expanded Evaporator Model

In order to include the effects of composition, temperature and evaporation (or solution density) into an expanded evaporator model, an OLS regression was performed on a randomly selected subset of the remaining 401 data points in the OLH design to relate $\log[\text{Al}(M)]$, $\log[\text{Si}(M)]$, $\log[\text{OH}(M)]$, evaporator solution density, evaporator operating temperature, and percent evaporation. A uniform random generator was set up in JMP statistical software and rows selected randomly from this column. This provided 200 OLH model data points and 201 OLH validation data points.

A stepwise regression was performed on the 201 randomly selected OLH model data points using the following tank concentrations at ambient temperature as variables, $\log \text{Al}(M)$, $\log \text{Si}(M)$, \log

$\text{OH}(M)$. In addition, evaporator temperature and fraction evaporation in kgs and solution density calculated from ambient tank measurements were used as variables. The OLS generated from the regression of these six variables against the $\log(Q/K)$ calculated by GWB yielded Equation 29 with an $R^2=0.96$ and RMSE=4.111:

$$-1.3808 + 13.18\log[Al(M)] + 11.13\log[Si(M)] - 13.24$$

Equation 29 $\log(Q/K)_{NAS} = \log[OH(M)] + 21.68Density + 0.0127Temp(^{\circ}C) + 13.7078Evap(kgs)$

Analysis of the importance (leverage) of each of the factors is shown in Figure 18. It can easily be seen from the leverage plots that the composition effects are more important than the remaining parameters and that the evaporator temperature is the least important of all the effects.

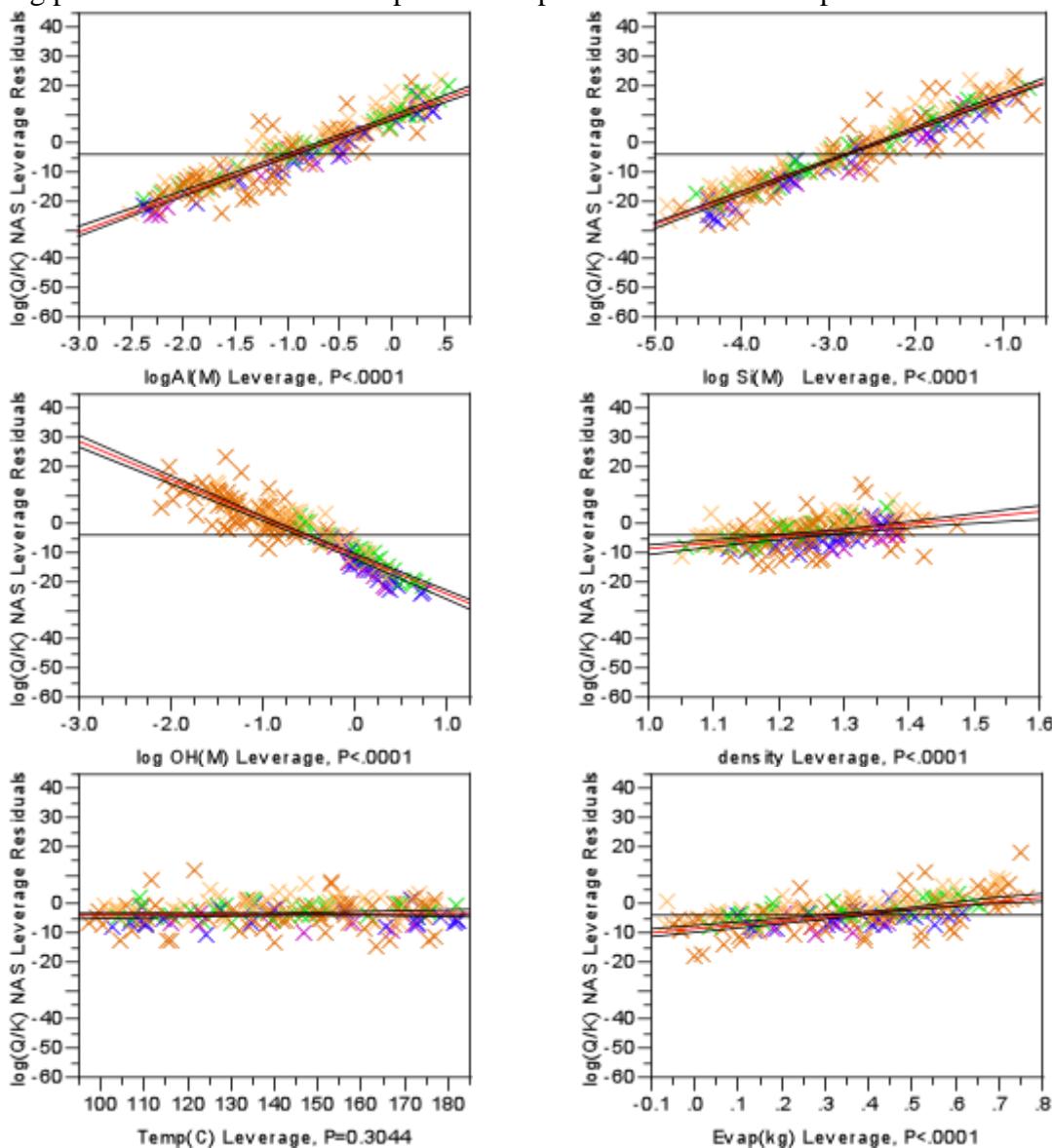


Figure 18 Significance (leverage) of the parameters in Equation 29.

Due to strong correlations between log Na(M) and density, an alternative equation could be derived using log Na(M). However, since this parameter is not routinely measured for evaporator solutions and this measurement is inherently inaccurate at the high molar concentrations of Na in the evaporator solutions, it is suggested that density not be substituted by log Na(M). In addition, there are evaporator temperature effects on solution density, so it is suggested that evaporator operating temperature be kept as a parameter which then allows the density measurement to represent the evaporator operating temperature solution density.

It can then be shown that a model with only five parameters, e.g. log Al(M), log Si(M), log OH(M), evaporator operating temperature, and final evaporator solution density, adequately represents the relation between these variables and the $\log(Q/K)_{NAS}$ calculated by GWB. A second OLS regression was performed with only five variables (% evaporation is removed) instead of the six variable used to derive which is shown in Equation 30 with an $R^2=0.94$ and RMSE=5.0421.

$$\text{Equation 30} \quad \log(Q/K)_{NAS} = \frac{9.8691 + 13.04 \log[Al(M)] + 11.09 \log[Si(M)] - 13.51}{\log[OH(M)] + 15.84 \text{Density} + 0.0163 \text{Temp}(\text{°C})}$$

It should be noted that both Equation 29 and Equation 30 have coefficients for the log Al(M), log Si(M), and log OH(M) that are close to the parameters 12:12:-12 developed in Equation 13 from the thermodynamic equation governing the precipitation of the NAS_{gel} .

Either Equation 29 or Equation 30 can be used for SRS evaporator process control. In Equation 29 overheads will have to be monitored to determine the percent evaporation. Use of Equation 30 does not entail monitoring of the percent evaporation since the coefficients of log Al(M), log Si(M), log OH(M), density, and operating temperature compensate for the missing parameter because they are all related to percent evaporation. Since Equation 30 is easier to implement than Equation 29, it is recommended that Equation 30 would be easier to implement as the process control model for the SRS 3H and 2F evaporators than Equation 29. However, Figure 19 demonstrates that the residuals span a wider range of $\log(Q/K)_{NAS}$ values, e.g. from +14.90 to – 20.45 than the nominal process control model given by Equation 13 and shown in Figure 12 where $\log(Q/K)_{NAS}$ values spanned only ± 4 . The wider distribution of the residuals for the expanded process control model is due to the expanded range of coverage of all the variables.

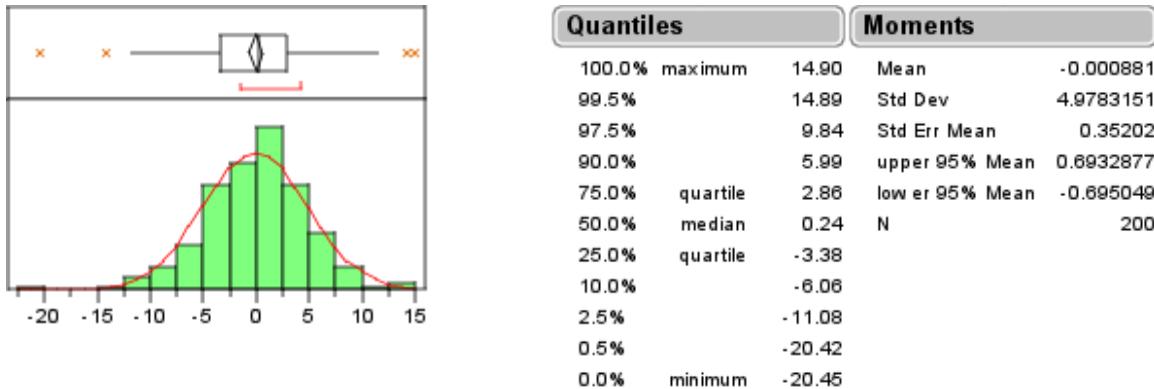


Figure 19. Assessment of the expanded process control model (Equation 30) to the GWB predicted values.

7.3 Validation of the OLH Expanded Evaporator Model

A plot of Equation 30, the calculated $\log(Q/K)_{NAS}$ from tank parameters to the $\log(Q/K)_{NAS}$ calculated by GWB for the 201 OLH model data gave a regression with a zero intercept and a slope of 1.0 (see Equation 31] with an $R^2=0.94$ for the 201 model data points.

$$\text{Equation 31} \quad \log(Q/K)_{NAS} = 0.0009 + 0.9999(\text{Equation}[31])$$

When Equation 30 was applied to the remaining 200 OLH validation solutions an OLS regression of the calculated $\log(Q/K)_{NAS}$ from tank parameters to the $\log(Q/K)_{NAS}$ calculated by GWB an intercept close to zero and a slope of ~1 was determined as shown in Equation 32.

$$\text{Equation 32} \quad \log(Q/K)_{NAS} = 0.1488 + 1.0235(\text{Equation}[31])$$

Equation 32, with an $R^2=0.93$, validates the expanded evaporator model given by Equation 30. A plot of the residuals for the validation data (similar to the plot shown in Figure 19 for model data) indicates a distribution around $\log(Q/K)_{NAS}$ of zero between +18.28 and -21.45.

7.4 Correlation of the OLH Expanded Evaporator Model to Historic Evaporator Operation

The expanded evaporator process control model (Equation 30) can then be related to recent SRS evaporator operation, in particular the data as measured by SRTC from Table I, Table II, and Table III. The $\log(Q/K)_{NAS}$ values calculated from Equation 30 are shown in Table IX for selected data from Table I, Table II, and Table III. The data for all the solutions in Table I, Table II, and Table III is shown in Figure 20.

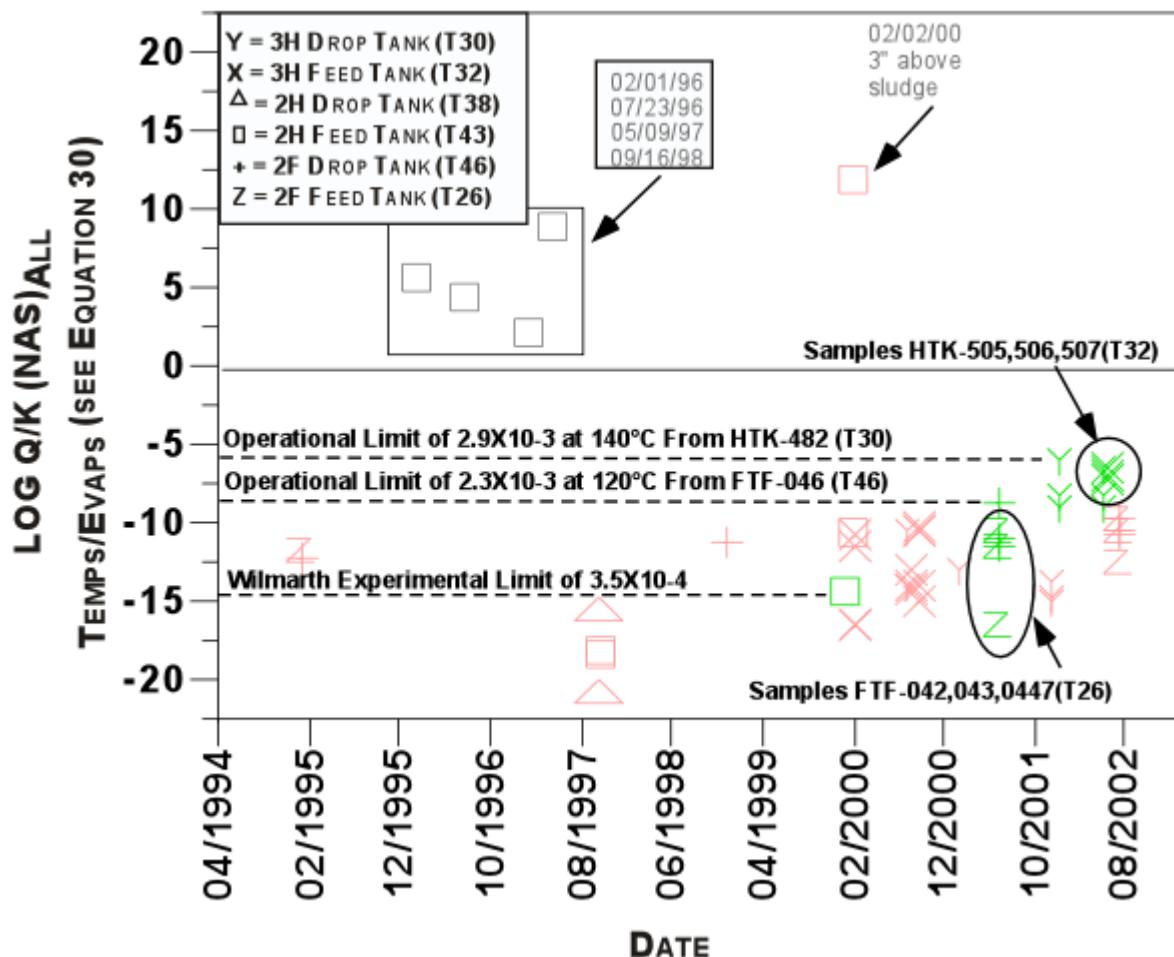


Figure 20. Operational History of SRS Evaporators assessed using Equation 30.

Table IX. Calculations of Log(Q/K)_{NAS} for Selected Samples of Model Data From Equation 30

Tank/Experiment	Sample	Height of Sample in Tank (Inches)	Calculated log (Q/K) _{NAS} from Equation 30	Average
Tank 43 (Feed-2H)	Wilmarth WSRC-TR-2000-00208	Dip	-14.31	-14.31
Tank 43 (Feed-2H)	Wilmarth WSRC-TR-2000-00208	64 (3" above sludge)	+11.92	+11.92
Tank 46 (Drop 2F)	FTF-045	252	-11.48	
Tank 46 (Drop 2F)	FTF-046	199	-8.50	
Tank 46 (Drop 2F)	FTF-047	145	-10.78	-10.25
Tank 26 (Feed 2F)	FTF-042	261	-16.29	
Tank 26 (Feed 2F)	FTF-043	166	-10.32	
Tank 26 (Feed 2F)	FTF-044	65	-11.40	-12.67
Tank 32 (Feed-3H)	HTK-505	196.5	-6.57	
Tank 32 (Feed-3H)	HTK-506	89	-7.12	
Tank 32 (Feed-3H)	HTK-507	77	-7.29	-6.99
Tank 30 (Drop-3H)	HTK-480	VDS	-8.24	
Tank 30 (Drop-3H)	HTK-481	VDS	-8.95	
Tank 30 (Drop-3H)	HTK-482	VDS	-5.78	-7.66
Tank 30 (Drop-3H)	HTK-508	221.9	-6.35	
Tank 30 (Drop-3H)	HTK-509	156	-8.05	
Tank 30 (Drop-3H)	HTK-511	4	-8.77	-7.72

Figure 20 demonstrates how the log(Q/K)_{NAS} data for all evaporators at all temperatures and unknown evaporation (calculated using Equation 30), can be related to SRS evaporator operational history between 1995 and 2002. All of the variable depth samples listed in Table IX are highlighted in Figure 20. The expanded process model based on the Mensah et al⁸ data (Equation 30) can be compared to the solubility product criteria, [Al]*[Si] in M² ~ 10⁻⁴, recently used by Wilmarth^{36,37} to determine the acceptability of feed tank solutions for processing in the SRS 3H-Evaporator. The Wilmarth solubility product is shown in Figure 20 compared to recent operational data for Tank 46F and Tank 30H.

Recent Tank 46F samples have been measured by SRTC and this sample can be used to set an operational limit at log(Q/K)_{NAS} of -8.50 since it is based on qualified Si data (sample FTF-046 from the 2F drop tank; see Table IX and Figure 20). More recently, samples from Tank 30H (sample HTK-482 from the 3H drop tank) analyzed at SRTC and associated with a recent tank

inspection, indicates that this sample can be used to set an operational limit at $\log(Q/K)_{NAS} = -5.78$ (see Table IX and Figure 20).

Although these samples are from evaporator drop tanks in the 3H and 2F evaporator systems, the FTF-046 liquor was recycled to the feed tank and experienced an additional evaporation of 31%⁵⁴. Likewise, the HTK-480, HTK-481, and HTK-482 samples from the SRS 3H evaporator drop tank (Tank 30) were taken on the same day at different depths. The 3H samples were also recycled to the feed tank and experienced a 9.7 % additional evaporation.⁵⁴ Figure 20 confirms that the HTK-482 series of samples and the FTF-046 series of samples are comfortably below saturation, e.g. $\log(Q/K)_{NAS} < 0$. Similarly, the feed tank samples from T26 and T32 (circled in Figure 20) have calculated $\log(Q/K)_{NAS} < 0$, e.g. averages of -6.99 and -12.67, respectively (see Table IX) Therefore, an operation limit of $\log(Q/K)_{NAS} < 0$ should prohibit aluminosilicate scale formation in SRS evaporators.

Note that the only samples in Figure 20 that have $\log(Q/K)_{NAS} > 0$ are samples in the gray box that represent the Si enrichment that the SRS 2H Evaporator feed pump was seeing when it was in the Zone of Turbidity between 1996 and 1998, e.g. when the SRS 2H Evaporator was exhibiting copious amounts of aluminosilicate scale. The remaining point at $\log(Q/K)_{NAS} > 0$ is a sample taken 3" above the sludge at a height of 64" in the 2H feed tank after the evaporator had been shut down and after feed pump had been moved to a height of 100" so that material had not been processed through the 2H Evaporator. These data show that precipitation of NAS_{gel} historically only occurred during process upset conditions, e.g. when the feed pump for the 2H evaporator was in the ZOT and the evaporator was receiving frequent silica rich frit SME carryovers from DWPF.³

7.5 Justification for Evaporator Operation at Saturation

Alternatively, the SRS evaporators could be run at $\log(Q/K)_{NAS} = 0$ (just saturation). This may be possible since

- silicate solutions can be >200% supersaturated at a given elevated temperature and not precipitate until the solutions are cooled.⁵⁵
- precipitation of NAS_{gel} historically only occurred during process upset conditions, e.g. when the feed pump for the 2H evaporator was in the ZOT and the evaporator was receiving frequent silica rich frit SME carryovers from DWPF

The $\log(Q/K)_{NAS} = 0$ limit on Figure 20 corresponds to a region of 7 years of successful evaporator operation without scaling ($\log(Q/K)_{NAS} < 0$) and evaporator operation with scaling ($\log(Q/K)_{NAS} > 0$). This demonstrates that control at $\log(Q/K)_{NAS} = 0$ may be possible if samples for analysis are taken at the height of the feed pump and analyzed by an accurate method for Si unless a process upset, that could cause increased Si, is experienced such as the following:

- evaporator feeds exposed to silica rich frit (SME) carryovers (samples in box shown on Figure 20)

- evaporator feeds pumped when the feed pump was too close to the sludge or in the Zone of Turbidity (ZOT) as defined in Parts I and II of this study^{3,4}
- evaporator feeds containing high silica and/or zeolite seeds such as the HEME/HEPA digests from DWPF⁵⁶
- sludge wash water that may contain enriched silica from degradation of IE-95 resin which liberates 11 moles of SiO₂ for every mole of degraded resin.⁵⁷

This implies that evaporator control at $\log(Q/K)_{NAS} = 0$ may be acceptable, rather than control at $\log(Q/K)_{NAS} < 0$, except during process upsets that could bring high concentrations of silica into the evaporator feed or drop tanks.

8.0 CONCLUSIONS

Nominal and expanded evaporator process control models are presented in this study based on calculated NAS_{gel} supersaturations performed using Geochemist's Workbench. Both models are based on solubility data of the NAS_{gel} phase determined by researchers at the University of Southern Australia (Mensah et.al.⁸). The kinetic data of Mattigod³⁰ is shown to validate the use of the NAS_{gel} precursor phase as the basis for the process control modeling. Use of the Mensah⁸ data demonstrated that the previous evaporator process control models had underestimated the importance of the OH⁻ term in modeling.

The nominal process control model covers the last 7 years of SRS evaporator operation over the compositional ranges given in Table VII for a nominal 40% evaporation at an operating temperature interval of 120-140°C. The sensitivity of this model to temperature is minimal while the sensitivity to percent evaporation is ten times larger. The revised nominal process control model was derived which takes the form of

$$\log(Q/K)_{NAS\ 120-140^{\circ}C/\ 40\% \ evap} = \frac{37.4848 + 1.0949(12\log[Al(M)] + 12\log[Si(M)] - 12\log[OH(M)])}{}$$

Where $\log(Q/K)_{NAS\ 120-140^{\circ}C/\ 40\% \ evap}$ on the LHS of the equation is the supersaturation that will be experienced in the evaporator pot between 120-140°C after a 40% evaporation of a solution represented at room temperature by the parameters on the RHS of the equation.

The RHS of the nominal process control model is referred to as $\log Q(NAS)_{25^{\circ}C}$. The nominal process control model is based on SRS evaporator feed tank data analyzed only at SRTC and is validated using an Orthogonal Latin Hypercube (OLH) statistical design of simulated evaporator solutions. Errors in this model are $\log(Q/K)_{NAS}$ of ± 2 at 90% confidence (Figure 12).

Equations similar to the nominal process control model can be derived for various combinations of operating temperature and percent evaporation; each should have similar errors in $\log(Q/K)_{NAS}$ as the nominal process control model. When these equations are solved at $\log(Q/K) = 0$, which represents saturation with respect to NAS_{gel}, a family of $\log Q(NAS)_{25^{\circ}C}$ values are derived and

the relationship between the tank chemistry ($\log Q(\text{NAS})_{25^\circ\text{C}}$), operating temperature and percent evaporation takes the form

$$\log Q(\text{NAS})_{25^\circ\text{C}} = -32.1114 - 0.1119(\% \text{Evaporation}) + 0.0165(\text{Operating Temp } ^\circ\text{C})$$

$$\text{where } \log Q(\text{NAS})_{25^\circ\text{C}} = (12\log[Al(M)] + 12\log[Si(M)] - 12\log[OH(M)])$$

The coefficients in this equation demonstrate that evaporation and operating temperature have opposite effects. Increased evaporation causes decreased solubility of components while increased temperature causes increased solubility of components. In addition, the coefficients demonstrate that evaporation is a factor of 10 more significant than operating temperature. Due to the insignificance of the temperature term, and the fact that higher temperature causes increased solubility of components, the temperature term can be eliminated from the above equation, which then becomes:

$$\log Q(\text{NAS})_{25^\circ\text{C}} = -29.9434 - 0.1092 (\% \text{Evaporation})$$

The above relation between $\log Q(\text{NAS})_{25^\circ\text{C}}$ and percent evaporation can be used to control scaling in the SRS evaporators at a variety of temperatures if the percent evaporation can be monitored. However, this process control approach is only valid over the compositional range of solutions modeled, e.g. the historic composition range experienced between 1995 and 2002 (Table VII).

The expanded evaporator process control model covers the wider tank farm compositional region given in Table VIII over evaporator operating conditions of:

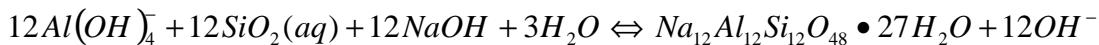
- 0-80 wt % evaporation
- 100°C to 180°C
- wider composition ranges defined in Table VIII

The expanded process control model was developed using an OLH experimental design covering the composition region defined over a 28 year operational period of the tank farm (1973-2001). Half of the data points, randomly chosen, were used to develop the expanded process control model and the remaining half were used for validation. The expanded process control model takes the form

$$\log(Q/K)_{\text{NAS}} = \frac{9.8691 + 13.04\log[Al(M)] + 11.09\log[Si(M)] - 13.51}{\log[OH(M)] + 15.84\text{Density} + 0.0163\text{Temp}(\text{ }^\circ\text{C})}$$

The usage of the expanded process control model does not entail monitoring of the percent evaporation since the coefficients of $\log Al(M)$, $\log Si(M)$, $\log OH(M)$, density, and operating temperature compensate for the missing parameter because they are all related to percent evaporation. However, the errors in this model are $\log(Q/K)_{\text{NAS}}$ of ± 6 at 90% confidence (Figure 19).

It should be noted that the nominal process control model uses coefficients for the log Al(M), log Si(M), and log OH(M) that are the parameters 12:12:-12 developed from the thermodynamic equation governing the phase boundary between NAS_{gel} and AlOOH which in turn is governed by the stoichiometry of the NAS_{gel} :



The and the expanded process control model uses coefficients that are similar to those governed by the stoichiometry of the NAS_{gel} .

When the expanded process control model is related to the past 7 years of SRS evaporator operating history it demonstrates that normal operation has been at $\log(Q/K)_{\text{NAS}} < < 0$ undersaturated region, e.g. values in the -15 to -10 range for the 2H evaporator when it was not scaling, for the 2F and 3H evaporators and in the -7 to -5 range for recent 3H evaporator operation (Table IX).

Therefore, a $\log(Q/K)_{\text{NAS}} < 0$ process control limit can be set for implementation of either the nominal or the expanded process control model based on operational history or a process control limit of $\log(Q/K)_{\text{NAS}} = 0$ can be implemented except during process upset conditions. The limit of $\log(Q/K)_{\text{NAS}} = 0$ separates the 7 years (1995-2002) of SRS Evaporator operation modeled into two populations, referred to as “normal operation” and “process upset operation.” This allows the simplified nominal process control model relating NAS_{gel} supersaturation to chemistry and percent evaporation, e.g. $\log Q(\text{NAS})_{25^\circ\text{C}} = -29.9434 - 0.1092 (\% \text{Evaporation})$, to be implemented.

Operation “just at saturation” is an attractive approach because of the following:

- silicate solutions can be >200% supersaturated at a given elevated temperature and not precipitate until the solutions are cooled
- precipitation of NAS_{gel} historically only occurred during process upset conditions, e.g. when the feed pump for the 2H evaporator was in the Zone of Turbidity (ZOT) and the evaporator was receiving frequent silica rich frit SME carryovers from DWPF

This demonstrates that it is only necessary to control at $\log(Q/K)_{\text{NAS}} < 0$ if there are known process upsets that could cause increased Si such as the following:

- evaporator feeds exposed to silica rich frit (SME) carryovers (samples in box shown on Figure 20)
- evaporator feeds pumped when the feed pump was too close to the sludge or in the Zone of Turbidity (ZOT) as defined in Parts I and II of this study

- evaporator feeds containing high silica and/or zeolite seeds such as the HEME/HEPA digests from DWPF
- sludge wash water that may contain enriched silica from degradation of IE-95 resin which liberates 11 moles of SiO₂ for every mole of degraded resin

Control at $\log(Q/K)_{NAS} = 0$ allows credit to be taken for keeping the feed pumps 40" above the sludge or 20" above the ZOT, so that receipt of silica rich material from the ZOT cannot occur.

9.0 ACKNOWLEDGEMENTS

Kent Gilbreath from the SRS H-Area Tank farm is thanked for providing the data about sludge levels, feed pump levels, and operating temperatures of the SRS 3H from the Tank Farm morning reports. Ken Jones of the F-Area laboratory is acknowledged for discussions about the F-Area Si analytic methodology and dilution factors.

Thomas B. Caldwell is also especially thanked for the database that he provided with >1800 datapoints spanning 29 years of operating history in the tank farm that related tank composition to density. This data is shown in Appendix A and was of great assistance in converting the molar to molal compositions by developing a solution density correlation.

Many thanks are due to David Hobbs and Bill Wilmarth of SRTC for their frequent and always helpful counsel. Kevin G. Brown, formerly of SRTC, is also thanked for his encouragement and help in setting up computer interfaces between the GWB, Excel, and JMP softwares to eliminate human error when transferring database calculations between the different software packages.

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APPENDIX A

DENSITY CORRELATION

Summary

Tank compositions and analytical results are typically reported on a solution basis (e.g., mg/L solution). For input into the Geochemist's Workbench (GWB), molality (moles per kilogram of solvent) is used. To convert from a solution based concentration to a solvent based concentration, the solution density must either be measured or estimated. Using historical solution density data from Tank Farm analyses, a correlation to relate density to sodium content was developed. The correlation is:

For $\text{Na (M)} \leq 16.5$,

$$\text{density} = 1.013 + 5.701 \cdot 10^{-2} \cdot \text{Na(M)} - 1.725 \cdot 10^{-3} \cdot \text{Na(M)}^2$$

Else

$$\text{density} = 1.483$$

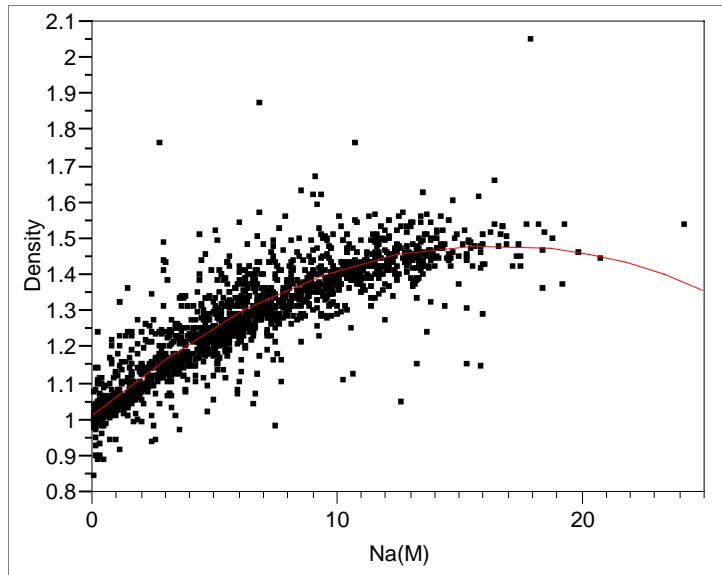
This correlation is based on data measured at ambient temperature (nominally 25°C). This correlation is used to convert from molarity to molality for all compositions input into GWB for evaporator modelling.

Correlation Derivation

A relationship to calculate tank salt solution density from solution composition was developed using past waste tank analyses. T. B. Caldwell of High Level Waste Division Program Management compiled a table of historic tank analyses with measured densities (see Table A-1). In Table A-1, the sodium concentration is calculated from a charge balance rather than a direct measurement. All other values in the table were measured. This table was imported into the statistical software JMP[®]¹. Samples with sodium concentrations less than 0.05M were deleted. These few points had unrealistically high measured densities. Other than deleting these points, there was no other screening of the data. As can be seen from Figure A-1, there are some obvious points with few potentially bad data have little impact on the correlation.

The Fit Y by X function of JMP was then used to fit a curve of density as a function of sodium concentration. A second order polynomial fit was chosen. This choice gave a good balance between simplicity and representation of the data. The results of the curve fit are given in Figure A-1.

¹ JMP[®] Version 4.0.5, SAS Institute Inc., SAS Campus Drive, Cary, North Carolina 27513

**Polynomial Fit Degree=2**

$$\text{Density} = 1.0713231 + 0.0369386 \text{Na}(M) - 0.0017254 (\text{Na}(M)-5.81717)^2$$

Summary of Fit

RSquare	0.807394
RSquare Adj	0.807181
Root Mean Square Error	0.071658
Mean of Response	1.252899
Observations (or Sum Wgts)	1815

Figure A-4. Polynomial fit of Tank Solution Density to Sodium Molarity

The correlation given in Figure A-1, when expanded, yields:

$$\text{density} = 1.013 + 5.701 \cdot 10^{-2} \cdot \text{Na}(M) - 1.725 \cdot 10^{-3} \cdot \text{Na}(M)^2$$

Taking the derivative of the above equation, setting to zero, and solving for Na(M), the maximum predicted density (1.483) occurs at a sodium concentration of 16.5M. Because a positively sloped regression of densities at sodium concentrations greater than 16.5M was not found, the predicted density is set to 1.483 for these high sodium concentrations. This modified density correlation is shown graphically in Figure A-2.

By setting the density of salt solutions with Na(M)>16.5 to 1.483, higher concentration solution densities will undoubtedly be underestimated. In normal evaporator operations, salt solutions are concentrated to a density of approximately 1.6, implying that evaporator feeds would have densities less than 1.6. Therefore, by setting the maximum density in the correlation to 1.483, the worst case underestimation of density would still be less than 10%.

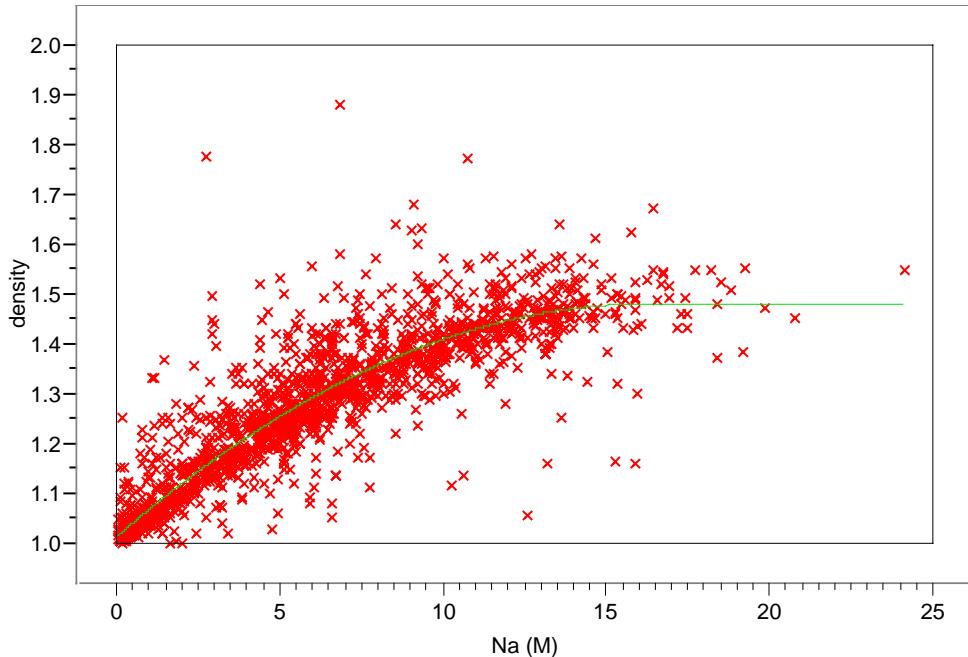


Figure A-5. Comparison Between Measured (**X**) and Predicted (—) Denisty

Figure A-3 shows the absolute value of the percent difference between the predicted and measured densities. It should be noted that the difference between the predicted and measured densities was less than 10% in over 90% of the samples.

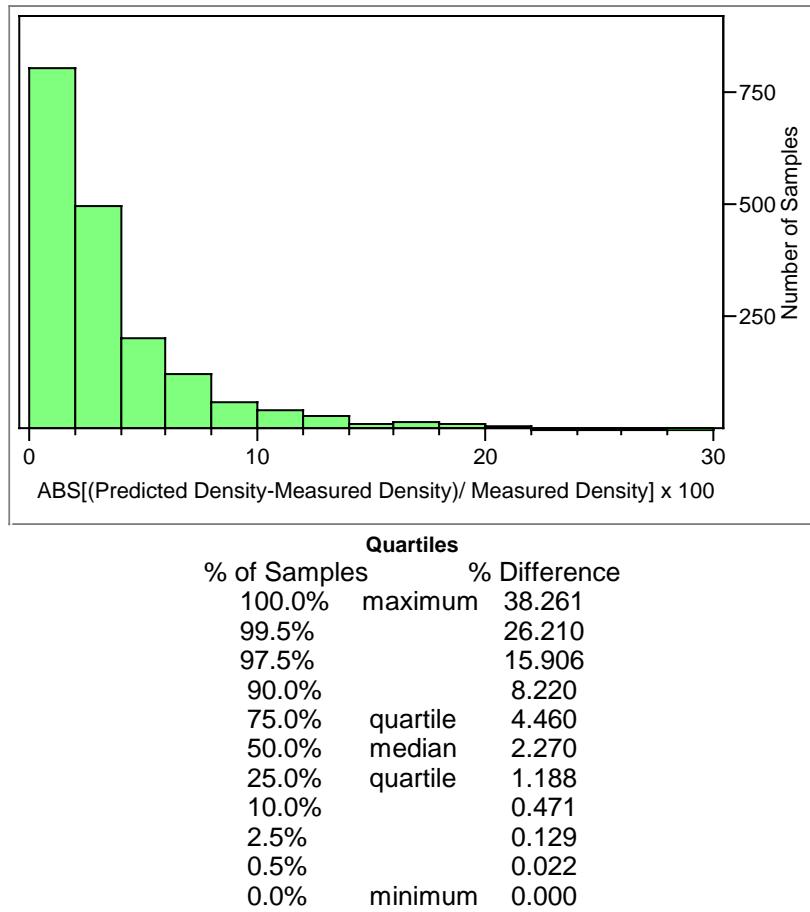


Figure A-6. Histogram Showing the Percent Difference Between Predicted and Measured Densities

Table A-2. Measured Tank Solution Densities and Chemical Compositions

Tank	Date	Density	Na(M)	AlOH4 (M)	C2O4 (M)	CrO4 (M)	Cl (M)	CO3 (M)	Fl (M)	Formate (M)	NO2 (M)	NO3 (M)	OH (M)	PO4 (M)	SO4 (M)	Titanate (M)
1	10/07/97	1.53000	15.153	0.7200			0.0250	0.1400			2.7500	2.0000	9.3000	0.0260		
1	08/07/96	1.53000	14.302	0.7800	0.0078		0.0260	0.0100	0.0150		2.7000	2.1100	8.5600	0.0240	0.0057	
1	09/09/95	1.49610	15.330	0.7100	0.0068		0.0280	0.1400	0.0052		2.2300	1.8400	10.1500	0.0230	0.0054	
1	07/07/94	1.52510	16.209	0.8500	0.0068		0.0210	0.3400	0.0000		3.1600	2.2500	9.1400	0.0250	0.0130	
1	07/22/93	1.62270	15.746	0.1100	0.0090		0.0140	0.0000	0.0000		3.2700	2.3400	9.8600	0.0420	0.0083	
1	07/31/92	1.51660	13.680								2.6800	2.2100	8.7900			
1	07/31/91	1.51650	13.520								2.4500	2.0400	9.0300			
1	05/15/89	1.50700	11.840								2.4200	2.3200	7.1000			
1	04/30/87	1.26450	9.133								1.7340	2.0090	5.3900			
1	09/05/85	1.37200	5.850								2.0300	1.8800	1.9400			
1	02/21/73	1.41000	11.658	0.8000		0.0080	0.0600	0.1000	0.0020		2.4000	1.6000	6.3000	0.0800	0.0200	
2	12/10/96	1.52400	14.056	1.0600	0.0068		0.0220	0.1500	0.0130		3.0400	2.2500	7.1800	0.0580	0.0053	
2	11/21/95	1.49580	13.418	0.6100	0.0068		0.0240	0.1500	0.0130		3.0800	2.2600	6.9700	0.0480	0.0052	
2	11/15/94	1.45760	12.823	1.3100	0.0068		0.0120	0.1100	0.0260		2.3700	1.7000	7.0200	0.0480	0.0071	
2	11/24/93	1.46257	14.572	1.7700	0.0068		0.0170	0.1600	0.0340		1.9700	1.5000	7.0200	0.0410	0.0058	
2	10/22/92	1.55640	13.100								3.4100	2.7400	6.9500			
2	10/08/91	1.54060	12.950								3.8900	2.8900	6.1700			
2	05/15/89	1.45990	9.390								3.1100	3.0100	3.2700			
2	04/30/87	1.26920	7.601								1.9780	3.1830	2.4400			
2	02/20/73	1.41000	10.930		0.0040	0.0600	0.1000	0.0020			2.9000	2.4000	4.5000	0.0400	0.0200	
4	11/26/00	1.27590	6.662	0.1800	0.0057		0.0028	0.4300	0.0053		1.3580	1.8050	1.8300	0.0053	0.2996	
4	11/28/99	1.31440	6.205	0.2300	0.0065		0.0027	0.4600	0.0130		1.3600	1.6800	1.1200	0.0110	0.4200	
4	12/04/98	1.32000	7.221	0.2600	0.0068		0.0028	0.2900	0.0130		1.6100	2.0300	1.7500	0.0028	0.4800	
4	12/03/97	1.33000	9.845	0.2200	0.0069		0.0072	0.6400	0.0130		1.9800	2.6600	2.5300	0.0160	0.5500	
4	11/05/96	1.31700	7.432	0.2400	0.0073		0.0030	0.6400	0.0057		1.3600	1.9200	1.8400	0.0120	0.3700	
4	09/09/95	1.31920	7.336	0.3000	0.0069		0.0053	0.6500	0.0053		1.3400	1.9000	1.6100	0.0160	0.4100	
4	07/09/94	1.29320	6.673	0.1800	0.0170		0.0075	0.3100	0.0000		1.3300	1.7700	1.9800	0.0160	0.3600	
4	07/22/93	1.30210	10.150	0.1300	0.0230		0.0140	2.2800	0.0000		1.1900	1.6900	1.6400	0.0210	0.4200	
4	07/31/92	1.31080	4.510								1.1000	1.7300	1.6800			
4	07/31/91	1.31080	5.240								1.1000	1.7300	2.4100			
4	07/31/91	1.28080	3.180								0.4700	0.8700	1.8400			
4	05/15/89	1.27270	3.380								0.8600	1.0600	1.4600			
4	10/07/87	1.13260	2.005								0.0150	0.2500	1.7400			
4	04/16/85	1.23600	3.120								0.8184	1.3830	0.9190			
4	12/01/83	1.25000	5.070								0.8500	1.6700	2.3500			
4	10/22/81	1.10000	4.700								0.9000	1.8000	2.0000			
4	03/10/80	1.13000	3.700								0.6000	1.3000	1.8000			
5	06/04/01	1.02620	4.720	0.1700	0.0074		0.0087	0.3000	0.0057		0.4672	1.8572	1.4500	0.0193	0.0477	
5	03/21/01	1.41930	7.692	0.1300	0.0392		0.0125	1.3000	0.0101		0.6831	2.8168	1.0600	0.0345	0.1186	
5	03/01/73	1.40000	11.036	0.7000		0.0070	0.0600	0.1000	0.0020		3.1000	2.4000	4.4000	0.0400	0.0200	
6	07/03/01	1.09060	1.994	0.0100	0.0057		0.0028	0.0100	0.0053		0.4903	0.1244	1.3000	0.0053	0.0097	
6	04/24/01	1.09660	2.200	0.0200	0.0057		0.0033	0.2000	0.0053		0.4874	0.1215	1.1200	0.0053	0.0106	
6	11/24/00	1.14400	3.275	0.0500	0.0057		0.0044	0.4100	0.0053		0.6240	0.1940	1.5300	0.0053	0.0128	
6	08/25/00	1.16500	3.267	0.0200	0.0057		0.0028	0.4200	0.0053		0.6120	0.1820	1.5600	0.0053	0.0117	
6	05/31/00	1.15300	2.962	0.0900	0.0069		0.0028	0.3900	0.0053		0.6080	0.1580	1.2700	0.0063	0.0110	
6	03/15/00	1.15360	3.228	0.0400	0.0069		0.0028	0.3600	0.0053		0.6085	0.2398	1.5600	0.0064	0.0126	
6	01/06/00	1.14920	2.612	0.0300	0.0069		0.0028	0.2400	0.0053		0.5400	0.1400	1.3700	0.0064	0.0091	
6	10/21/99	1.13170	3.054	0.0200	0.0068		0.0028	0.2800	0.0053		0.6400	0.1300	1.6500	0.0063	0.0100	
6	07/07/99	1.11000	1.918	0.0100	0.0069		0.0028	0.3400	0.0053		0.5700	0.1000	0.5100	0.0064	0.0068	
6	11/20/98	1.19000	3.410	0.0800	0.0007		0.0003	0.4700	0.0053		1.0700	0.4800	0.7700	0.0006	0.0310	
6	12/15/97	1.05900	1.223	0.0200	0.0007		0.0003	0.2000	0.0026		0.3700	0.0320	0.3900	0.0006	0.0027	
6	06/25/97	1.05200	1.172	0.0100	0.0007		0.0003	0.2200	0.0027		0.3300	0.0260	0.3500	0.0026	0.0023	
6	02/28/73	1.12200	5.395	0.4000		0.0060	0.0400	0.1000	0.0030		1.1000	1.6000	1.7000	0.0200	0.1400	
7	07/06/01	1.35520	9.636	0.6800	0.0058		0.0135	1.1500	0.0155		1.3586	1.5688	3.5300	0.0131	0.0624	
7	12/04/98	1.33000	7.651	0.5600	0.0034		0.0097	0.4300	0.0130		1.1200	1.4000	3.5400	0.0110	0.0560	
7	12/02/97	1.31000	7.281	0.5400	0.0068		0.0100	0.3800	0.0130		0.9200	1.3700	3.5200	0.0110	0.0540	
7	11/05/96	1.29400	7.947	0.5900	0.0074		0.0100	0.5600	0.0280		0.9900	1.4400	3.6200	0.0120	0.0530	
7	10/18/95	1.33640	8.649	0.5400	0.0068		0.0220	0.8500	0.0260		1.0400	1.5000	3.6600	0.0120	0.0590	
7	07/09/94	1.28850	7.801	0.6000	0.0073		0.0026	0.6900	0.0140		0.9200	1.3200	3.4200	0.0130	0.0490	
7	07/22/93	1.28440	8.326	0.5500	0.0091		0.0056	0.5000	0.0100		0.9100	1.5000	3.3700	0.0170	0.4600	
7	07/31/92	1.27540	5.400								0.7500	1.1700	3.4800			
7	07/31/91	1.19140	3.860								0.4300	1.0100	2.4200			
7	05/26/89	1.13740	2.070								0.2900	0.3900	1.3900			
7	04/14/87	1.105180	6.580								0.3000	0.5700	5.7100			
7	11/25/86	1.15360	4.150								0.7200	1.3600	2.0700			
7	04/04/86	1.135020	3.640								0.5000	0.9000	2.2400			
7	11/26/85	1.28450	2.518								0.7200	1.2640	0.5340			
7	02/10/84	1.25000	6.560								0.7500	1.8400	3.9700			
7	08/23/83	1.37000	7.030								0.9600	2.3700	3.7000			
7	05/17/82	1.51000	8.400								1.1000	2.7000	4.6000			
7	05/05/82	1.21000	3.770								0.1000	2.7000	0.9700			
7	04/22/82	1.28000	4.000								0.3000	3.2000	7.5000			
7	04/07/81	1.26000	4.500								0.1000	3.1000	1.3000			
7	03/13/80	1.16000	5.100								0.7000	1.5000	2.9000			</

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Tank	Date	Density	Na(M)	AlOH4 (M)	C2O4 (M)	CrO4 (M)	Cl (M)	CO3 (M)	F1 (M)	Formate (M)	NO2 (M)	NO3 (M)	OH (M)	PO4 (M)	SO4 (M)	Titanate (M)
10	04/07/87	1.17630	1.520								0.1000	1.2200	0.2000			
10	04/25/86	1.06020	0.740								0.1000	0.4500	0.1900			
10	12/20/85	1.35550	2.377								0.1000	1.9460	0.3310			
10	11/26/85	1.41000	7.440								0.4300	5.9400	1.0700			
10	07/09/85	1.37000	6.590								0.3900	4.6600	1.5400			
10	02/28/85	1.43000	7.993								0.4100	7.4500	0.1330			
10	09/14/84	1.41000	5.220								1.1800	3.8400	0.2000			
10	09/14/84	1.41000	5.230								1.1800	3.8500	0.2000			
10	05/21/83	1.41000	6.910								0.2400	6.0100	0.6600			
10	03/26/83	1.41000	6.560								0.2500	5.6300	0.6800			
10	03/26/83	1.33000	4.910								0.3600	3.9700	0.5800			
10	03/01/83	1.43000	5.550								0.2000	5.0000	0.3500			
10	12/14/82	1.39000	5.100								0.2000	4.6000	0.3000			
10	10/07/82	1.42000	6.100								0.3000	5.4000	0.4000			
10	09/30/82	1.20000	4.800								1.0000	1.4000	2.4000			
10	09/23/81	1.26000	4.800								1.0000	1.4000	2.4000			
10	09/22/81	1.18000	2.700								0.1000	2.1000	0.5000			
10	01/13/81	1.09000	1.500								0.1000	1.2000	0.2000			
10	12/19/80	1.13000	1.580								0.0800	1.0000	0.5000			
10	06/10/80	1.02000	0.500								0.1000	0.3000	0.1000			
10	05/19/80	1.02000	1.400								0.3000	1.0000	0.1000			
10	04/28/80	1.02000	2.400								0.1000	2.2000	0.1000			
10	04/28/80	1.02000	1.400								0.3000	1.0000	0.1000			
10	04/04/80	1.18000	5.200								0.3000	3.9000	1.0000			
10	03/24/80	1.32000	6.250								0.3000	5.0600	0.8900			
10	01/18/80	1.20000	2.800								0.1000	2.5300	0.1700			
10	08/29/79	1.38000	7.960	0.1000				0.2800			0.2500	5.8000	0.4300	0.4100		
10	08/27/74	1.39000	9.647	1.0000		0.0020	0.0200	0.1000	0.0030		1.8000	4.5000	1.9000	0.0200	0.0800	
11	05/22/00	1.42000	8.705	0.3000	0.0068	0.0160	0.3500	0.0130			2.7500	3.4800	1.1200	0.0063	0.1500	
11	05/29/99	1.38000	8.780	0.2000	0.0068	0.0110	0.5600	0.0130			2.6800	3.2300	1.1400	0.0063	0.1800	
11	06/13/98	1.38000	8.439	0.2800	0.0068	0.0100	0.5000	0.0130			2.4300	3.1400	1.0600	0.0063	0.2400	
11	05/09/97	1.38400	7.952	0.3800	0.0068	0.0110	0.3600	0.0053			2.1900	3.3200	0.8200	0.0063	0.2400	
11	05/08/96	1.36300	7.158	0.1600	0.0068	0.0170	0.0700	0.0053			1.9500	3.2200	1.1800	0.0063	0.2300	
11	03/27/95	1.33660	9.171	0.2600	0.0069	0.1200	1.2000	0.0053			1.8000	3.1600	0.9600	0.0064	0.2200	
11	03/24/94	1.28700	8.536	0.6200	0.0170	0.0010	0.9700	0.0000			1.5800	3.1100	0.8000	0.0160	0.2100	
11	03/03/93	1.32240	7.717	0.3000	0.0230	0.0140	0.6200	0.0000			1.5200	3.1900	1.0200	0.0000	0.2050	
11	02/17/92	1.29080	6.480								1.5700	3.7600	1.1500			
11	02/25/91	1.28560	9.540								2.4300	5.9100	1.2000			
11	03/08/90	1.20850	4.970								1.0200	2.9000	1.0500			
11	03/20/89	1.08790	2.070								0.4100	1.3000	0.3600			
11	03/07/88	1.28000	4.184								0.7200	2.5700	0.8940			
11	06/19/86	1.23260	3.989								0.6200	2.6700	0.6990			
11	09/05/84	1.19000	7.530								1.6400	3.2300	2.6600			
11	10/10/82	1.36000	5.600								0.3000	3.5000	1.8000			
11	01/21/82	1.38000	6.100								0.2000	4.2000	1.7000			
11	07/15/81	1.28000	5.500								0.4000	3.7000	1.4000			
11	06/24/80	1.23000	4.800								0.3000	3.3000	1.2000			
11	04/01/80	1.12000	4.500								0.2000	3.1000	1.2000			
11	06/07/01	1.46350	9.604	0.2300	0.0060	0.0160	0.4200	0.0056			3.3330	3.5774	1.3300	0.0056	0.1246	
12	11/29/84	1.36800	1.411								0.3860	0.4150	0.6100			
12	09/10/81	1.44000	6.700								2.3000	3.1000	1.3000			
12	04/01/80	1.20000	5.600								1.2000	2.9000	1.5000			
13	08/24/01	1.46310	4.623	0.1000	0.0127	0.0151	0.0100	0.0117			2.0338	2.3639		0.0141	0.0116	
13	08/25/01	1.38160	19.193	1.0100	0.0001	0.0155	4.9100	0.0122			1.9249	1.9827	4.3300	0.0123	0.0303	
13	09/09/00	1.44700	11.231	0.7600	0.0133	0.0206	0.0100	0.0123			1.7650	2.5280	6.0500	0.0123	0.0125	
13	03/26/00	1.43580	10.199	0.6400	0.0160	0.0100	0.0100	0.0120			1.5400	1.9800	5.9100	0.0150	0.0130	
13	10/07/99	1.41000	10.477	0.5200	0.0160	0.0096	0.0200	0.0120			1.8400	2.1100	5.8600	0.0150	0.0120	
13	04/15/99	1.40000	10.608	0.4800	0.0160	0.0130	0.0100	0.0120			1.7900	2.2200	5.9800	0.0150	0.0160	
13	10/18/98	1.36000	10.953	0.7200	0.0160	0.0100	0.0100	0.0120			1.6900	2.4500	5.9600	0.0150	0.0150	
13	09/24/97	1.40000	13.299	0.6800	3.0000	0.0097	0.2000	0.0130			1.2800	1.2200	6.6300	0.0160	0.0092	
13	09/19/96	1.43000	10.341	0.4500	0.0069	0.0097	0.0100	0.0130			1.5500	2.1900	6.0200	0.0110	0.0240	
13	10/01/95	1.45000	10.706	0.6700	0.0089	0.0096	0.4500	0.0052			1.4100	2.2300	5.3900	0.0087	0.0280	
13	09/29/94	1.41100	11.498	0.6100	0.0160	0.0120	0.4000	0.0240			1.4900	2.5300	5.9100	0.0140	0.0320	
13	09/05/93	1.38220	11.916	0.6800	0.0067	0.0059	0.3000	0.0000			1.6900	2.3900	6.4500	0.0110	0.0300	
13	04/30/93	1.41380	12.823	0.6700	0.0094	0.0058	0.4100	0.0140			1.6400	2.9100	6.6200	0.0220	0.0340	
13	11/30/92	1.45048	14.500	0.5400	0.0100	0.0200	0.2200	0.0100			2.0000	2.2300	9.1700	0.0200	0.0100	
13	05/29/91	1.51240	12.070	0.7500	1.2600	2480ppm		3470ppm			1.4000	1.5200	7.1400	7940ppm		
13	02/25/91	1.43100	11.650								1.8100	2.1300	7.7100			
13	03/09/90	1.43490	10.780								1.6900	1.9900	7.1000			
13	03/20/89	1.43040	7.560								1.3500	1.5900	4.6200			
13	03/21/88	1.39880	8.723								1.3670	1.5560	5.8000			
13	09/28/87	1.23590	9.220								1.0600	0.8600	7.3000			
13	12/12/86	1.30000	8.560								1.8600	2.1100	4.5900			
13	04/21/86	1.28940	6.655								2.0800	1.7100	2.8650			
13	05/01/85	1.42000	2.930								0.8700	0.9400	1.1200			
13	05/02/84	1.44480	2.930								0.8700	0.9400	1.1200			
13	08/05/83	1.15800	15.870								3.9800	2.8100	9.0800			
13	07/15/82	1.16000	13.200								2.5000	2.7000	8.0000			
13	08/30/81	1.50000	10.200								2.7000	1.9000	5.6000			
13	06/29/81	1.48000	9.740								2.3400	3.1900	4.2100			
13	06/29/81	1.50000	8.900													

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Tank	Date	Density	Na(M)	AlOH4 (M)	C2O4 (M)	CrO4 (M)	Cl (M)	CO3 (M)	Fl (M)	Formate (M)	NO2 (M)	NO3 (M)	OH (M)	PO4 (M)	SO4 (M)	Titanate (M)
17	05/01/95	1.04080	0.780	0.0100	0.0007	0.0003	0.1100	0.0019	0.2400	0.0044	0.3000	0.0006	0.0006	0.0005		
17	02/28/95	1.04550	1.114	0.0200	0.0007	0.0000	0.2300	0.0046	0.3100	0.0048	0.3100	0.0006	0.0006	0.0010		
17	11/15/94	1.04000	0.843	0.0300	0.0007	0.0007	0.1700	0.0040	0.2400	0.0048	0.2200	0.0006	0.0006	0.0004		
17	08/19/94	1.04070	0.911	0.0210	0.0007	0.0007	0.1800	0.0027	0.2400	0.0053	0.2800	0.0000	0.0005			
17	05/03/94	1.03609	0.772	0.0100	0.0007	0.0006	0.1100	0.0021	0.2300	0.0051	0.3000	0.0006	0.0006	0.0006		
17	02/14/94	1.03967	0.889	0.0220	0.0039	0.0019	0.1600	0.0038	0.2200	0.0041	0.3100	0.0006	0.0005			
17	11/24/93	1.03928	0.822	0.0290	0.0007	0.0006	0.1200	0.0052	0.2200	0.0041	0.3200	0.0006	0.0005			
17	08/12/93	1.03868	0.881	0.0250	0.0009	0.0014	0.1200	0.0050	0.2400	0.0250	0.3400	0.0008	0.0008			
17	05/11/93	1.03920	0.817	0.0210	0.0009	0.0014	0.1200	0.0053	0.2100	0.0038	0.3300	0.0008	0.0008			
17	03/08/93	1.03860	0.945	0.0200	0.0000	0.0000	0.1700	0.0100	0.2100	0.0050	0.3400	0.0000	0.0100			
17	11/13/92	1.03770	0.490						0.1900	0.0200	0.2800					
17	08/28/92	1.03850	0.540						0.2000	0.0100	0.3300					
17	05/19/92	1.03850	0.610						0.2400	0.0200	0.3500					
17	02/24/92	1.03660	0.590						0.1900	0.0200	0.3800					
17	12/1/91	1.04090	0.480						0.1800	0.0100	0.2900					
17	09/15/91	1.03950	0.430						0.1200	0.0100	0.3000					
17	04/12/91	1.03970	0.527						0.2000	200ppm	0.3271					
17	01/23/91	1.03960	0.560						0.2100	0.0100	0.3400					
17	01/09/91	1.03080	0.290						50ppm	44ppm	0.2900					
17	10/04/90	1.02850	0.230						46ppm	42ppm	0.2300					
17	03/28/90	1.02310	0.232						0.0100	0.0020	0.2200					
17	02/23/89	1.02400	0.340						0.1000	0.1000	0.1400					
17	02/13/89	1.02400	0.340						0.1000	0.1000	0.1400					
17	04/30/87	0.89400	0.451						0.1140	0.2070	0.1300					
17	11/24/86	0.92660	1.085						0.4200	0.1000	0.5650					
17	10/14/85	1.00500	0.132	0.0000				0.0000	0.0110	0.0800	0.0210		0.0100			
17	06/25/85	1.04000	0.280	0.0100				0.0300	0.0100	0.0900	0.0100		0.0500			
17	06/19/85	1.05000	0.490	0.0200				0.0300	0.0100	0.1300	0.1100		0.0800			
17	04/12/85	1.09000	1.760	0.0500				0.0400	0.0200	0.5700	0.5600		0.2400			
17	04/03/85	1.11000	1.944	0.0600				0.0300	0.0240	0.8100	0.3500		0.3200			
17	03/12/85	1.29000	6.210	0.4400				0.1000	0.1000	3.9900	1.1800		0.1500			
17	03/01/85	1.31000	7.250	0.5200				0.1000	0.1300	4.7700	1.2900		0.1700			
17	01/24/85	1.34000	7.850	0.7400				0.1100	0.1400	4.7000	1.7500		0.1500			
17	01/14/85	1.35000	7.800	0.7100				0.1200	0.1300	4.6900	1.7500		0.1400			
17	12/31/84	1.34000	7.470	0.6300				0.1300	0.1800	4.7000	1.7000					
17	06/27/84	1.35000	7.040	0.6500				0.0800	0.3500	3.8000	1.7200		0.1800			
17	06/22/84	1.34000	5.370	0.7900				0.0900	0.0000	2.2500	1.6700		0.2400			
17	06/01/84	1.34000	7.060	0.7100				0.0800	0.2200	3.9100	1.7000		0.1800			
17	03/09/84	1.31000	7.930						0.1400	0.49800	2.4500			0.1800		
17	03/01/84	1.28000	5.810	0.5400				0.0000	0.2000	3.4500	1.6200					
17	02/10/84	1.28000	6.850	0.5600				0.1000	0.2400	3.7300	1.8000		0.1600			
17	02/10/84	1.30000	6.920	0.5600				0.1200	0.2000	3.6900	1.8300		0.2000			
17	01/26/84	1.32000	5.920	0.5200				0.0400	0.0200	3.0200	1.9200		0.1800			
17	01/06/84	1.25000	5.520	0.3500				0.0900	0.1100	2.6900	1.8900		0.1500			
17	12/15/83	1.28000	6.170	0.3700				0.1200	0.2800	3.3300	1.5300		0.2100			
17	12/14/83	1.29000	5.950	0.3600				0.1000	0.1800	3.3000	1.4900		0.2100			
17	12/02/83	1.32000	7.110	0.5000				0.2000	0.4000	3.6300	1.9600		0.1100			
17	11/27/83	1.32000	6.840	0.5600				0.1400	0.2300	3.3000	2.1700		0.1500			
17	11/22/83	1.34000	7.810	0.4800				0.2100	0.2500	4.1500	2.2100		0.1500			
17	11/17/83	1.34000	7.750	0.5400				0.1700	0.3000	4.2100	2.1200		0.1200			
17	11/08/83	1.26000	5.800	0.4800				0.0800	0.1800	3.0200	1.6200					
17	07/26/83	1.23000	3.640						0.1200	1.5200	2.0000					
17	09/14/82	1.27000	4.600						0.2000	2.0000	2.2000					
17	07/11/78	1.20000	4.400						0.2000	2.1000	2.1000					
17	10/20/75	1.16400	3.792	0.1000	0.0005	0.0050	0.0080	0.0400	0.1000	1.9000	1.4000	0.0300	0.0700			
18	08/28/01	1.18600	3.304	0.0800	0.0150	0.0091	0.0300	0.0988	0.10156	0.8020	0.9700	0.0008	0.1256			
18	05/30/01	1.18850	4.124	0.1800	0.0235	0.0080	0.4100	0.0951	0.8738	0.7945	1.0900	0.0009	0.1181			
18	05/04/01	1.18240	3.703	0.0700	0.0131	0.0083	0.2900	0.0966	0.8639	0.7907	1.0400	0.0005	0.1195			
18	04/02/01	1.18650	3.258	0.0100	0.0210	0.0085	0.1100	0.0938	1.5950	1.0594	0.0100	0.0026	0.1162			
18	02/28/01	1.16920	3.706	0.0900	0.0145	0.0087	0.2900	0.0867	0.8640	0.7890	1.0400	0.0005	0.1146			
18	01/04/01	1.17480	3.709	0.0800	0.0133	0.0092	0.2800	0.0640	0.8440	0.8050	1.1500	0.0005	0.0909			
18	10/19/00	1.15300	3.413	0.0700	0.0086	0.0079	0.3400	0.0313	0.7280	0.6900	1.0900	0.0005	0.0530			
18	09/21/00	1.06500	0.666	0.0006	0.0035	0.0004	0.0500	0.0013	0.0603	0.0081	0.1000	0.0006	0.0014			
18	09/21/00	1.05400	0.692	0.0006	0.0036	0.0004	0.0600	0.0013	0.0270	0.3760	0.0032	0.0109				
18	08/04/00	1.03900	0.285	0.0100	0.0007	0.0004	0.0500	0.0013	0.0603	0.0081	0.1000	0.0006	0.0014			
18	05/10/00	1.01900	0.399	0.0100	0.0007	0.0008	0.0700	0.0029	0.1100	0.0180	0.1100	0.0006	0.0025			
18	02/11/00	1.01070	0.283	0.0100	0.0007	0.0008	0.0600	0.0013	0.0573	0.0077	0.0800	0.0006	0.0015			
18	12/08/99	1.01490	0.408	0.0100	0.0007	0.0008	0.0600	0.0024	0.0920	0.0160	0.1600	0.0006	0.0020			
18	09/22/99	1.02300	0.519	0.0100	0.0007	0.0012	0.0700	0.0038	0.1500	0.0250	0.1800	0.0006	0.0034			
18	07/07/99	1.03800	0.795	0.0200	0.0013	0.0021	0.1200	0.0064	0.2400	0.0490	0.2200	0.0006	0.0071			
18	11/17/98	1.01000	0.258	0.0100	0.0007	0.0004	0.0500	0.0012	0.0530	0.0082	0.0800	0.0006	0.0014			
18	02/19/98	1.02000	0.173	0.0100	0.0003	0.0004	0.0300	0.0010	0.0410	0.0067	0.0500	0.0003	0.0013			
18	09/09/97	1.00100	0.071	0.0100	0.0003	0.0003	0.0100	0.0006	0.0220	0.0045	0.0100	0.0003	0.0012			
18	12/01/96	1.25400	3.161	0.0500	0.0120	0.0160	0.2900	0.0490	0.0070	0.19170	0.4700					
18	05/01/87	0														

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Tank	Date	Density	Na(M)	AlOH4 (M)	C2O4 (M)	CrO4 (M)	Cl (M)	CO3 (M)	Fl (M)	Formate (M)	NO2 (M)	NO3 (M)	OH (M)	PO4 (M)	SO4 (M)	Titanate (M)
18	07/25/80	1.33000	5.500								0.1000	3.8000	1.6000			
18	07/10/80	1.27000	6.600								0.4000	2.5000	3.7000			
18	06/24/80	1.36000	9.300								0.5000	4.5000	4.3000			
18	10/14/75	1.36400	10.061	0.7000	0.0056	0.0130	0.0090	0.0090		1.6000	2.6000	4.8000	0.0500	0.0800		
19	07/24/01	1.18360	3.420	0.0700	0.0145	0.0083	0.0800	0.1029		0.9174	0.8229	1.0700	0.0026	0.1229		
19	06/27/01	1.18450	3.771	0.1100	0.0154	0.0085	0.2800	0.0926		0.8717	0.7784	1.0800	0.0026	0.1232		
19	02/28/01	1.16920	3.706	0.0900	0.0145	0.0087	0.2900	0.0887		0.8640	0.7890	1.0400	0.0005	0.1146		
19	02/01/01	1.17900	3.676	0.1000	0.0153	0.0090	0.2700	0.0790		0.8370	0.7970	1.0800	0.0026	0.1056		
19	12/05/00	1.17100	3.402	0.0700			0.3000			0.7276	0.6904	1.1600	0.0008	0.0756		
19	10/31/00	1.21990	4.785	0.1200	0.0130	0.0114	0.3400	0.0696		1.0400	1.0700	1.5700	0.0030	0.1010		
19	10/02/00	1.28600	7.093	0.1500	0.0052	0.0166	0.6100	0.0441		1.3840	1.5800	2.5100	0.0026	0.0874		
19	09/15/00	1.28200	6.069	0.0100	0.0057	0.0160	0.3000	0.0430		1.3880	1.5690	2.2500	0.0030	0.0890		
19	08/23/00	1.28800	7.360	0.0900	0.0059	0.0150	0.6000	0.0570		1.4700	1.6400	2.6800	0.0032	0.0960		
19	03/21/00	1.25520	5.236	0.0800	0.0063	0.0157	0.5500	0.0639		1.3950	1.5370	0.8400	0.0032	0.0990		
19	04/22/99	1.25300	5.042	0.0600	0.0061	0.0140	0.2600	0.0580		1.6800	1.6600	0.8400	0.0032	0.0980		
19	09/24/98	1.25400	5.623	0.0800	0.0068	0.0170	0.4900	0.0500		1.8600	1.5600	0.8600	0.0032	0.1000		
19	01/13/98	1.25600	4.434	0.0400	0.0068	0.0160	0.2700	0.0320		1.5200	1.6400	0.4300	0.0032	0.1000		
19	07/08/97	1.25300	5.924	0.0800	0.0070	0.0160	0.6000	0.0510		1.6500	1.8300	0.8600	0.0032	0.1100		
19	01/21/97	1.25200	5.706	0.0800	0.0075	0.0170	0.5300	0.0520		1.6300	1.7400	0.9100	0.0032	0.1000		
19	08/01/96	1.25200	5.568	0.0700	0.0073	0.0180	0.5000	0.0530		1.5500	1.7600	0.9000	0.0032	0.1000		
19	11/21/95	1.25160	5.252	0.0500	0.0065	0.0180	0.4600	0.0480		1.4700	1.6500	0.8800	0.0032	0.1000		
19	08/26/95	1.21840	5.558	0.1000	0.0075	0.0180	0.5600	0.0530		1.4900	1.7000	0.8600	0.0032	0.1000		
19	05/01/95	1.25690	5.654	0.0600	0.0073	0.0200	0.5100	0.0510		1.4500	1.8200	1.0200	0.0032	0.0980		
19	11/15/94	1.24920	5.572	0.1000	0.0093	0.0190	0.5300	0.0640		1.5600	1.7100	0.8400	0.0032	0.1000		
19	08/19/94	1.24960	6.151	0.0900	0.0099	0.0210	0.5400	0.0620		1.7300	1.9700	0.9900	0.0000	0.0990		
19	05/03/94	1.24893	4.777	0.0720	0.0076	0.0340		0.0580		1.5800	1.7300	1.0900	0.0032	0.0980		
19	02/14/94	1.24722	5.733	0.0650	0.0082	0.0240	0.5100	0.0660		1.5800	1.7600	1.0100	0.0000	0.1000		
19	11/24/93	1.24490	5.802	0.1600	0.0074	0.0280	0.5100	0.0540		1.5800	1.6200	1.1300	0.0032	0.0963		
19	07/23/93	1.24400	5.667	0.0820	0.0071	0.0140	0.5200	0.0630		1.5600	1.6500	1.0500	0.0042	0.0940		
19	04/12/93	1.24792	5.185	0.0660	0.0083	0.0170	0.4700	0.0560		1.4600	1.4400	1.0200	0.0000	0.0890		
19	01/18/93	1.23860	4.862	0.0078	0.0087	0.1876	0.0680	0.0620		1.5100	1.6600	1.0979	0.0000	0.0960		
19	10/23/92	1.24090	4.190							1.5500	1.5800	1.0600				
19	07/30/92	1.23950	4.410							1.5700	1.7700	1.0700				
19	04/06/92	1.23890	4.610							1.8000	1.7500	1.0600				
19	01/16/92	1.24140	3.980							1.4300	1.4500	1.1000				
19	10/30/91	1.23720	4.130							1.5700	1.5300	1.0300				
19	08/03/91	1.22200	4.670							1.7300	1.6000	1.3400				
19	07/31/91	1.23390	4.300							1.5200	1.6900	1.0900				
19	04/12/91	1.23590	4.519							1.6000	1.7200	1.1985				
19	02/28/91	1.22530	5.467	0.0200	0.0110	0.0230	0.1200	0.0730		1.7900	1.9300	1.1500	0.0032	0.1100		
19	01/09/91	1.23520	1.140							836m	1655m	1.1400				
19	10/04/90	1.23400	5.990							2.5600	2.4200	1.0100				
19	04/23/90	1.18980	2.960							0.7600	1.9800	0.2200				
19	04/23/90	1.177400	2.750							0.6600	1.8900	0.2000				
19	04/17/90	1.17460	2.660							0.4600	1.9800	0.2200				
19	04/17/90	1.18810	2.730							0.7000	1.8000	0.2300				
19	03/28/90	1.16270	2.283							0.0430	1.8900	0.3500				
19	02/23/89	1.15820	2.010							0.1000	1.6400	0.2700				
19	02/13/89	1.15800	2.010							0.1000	1.6400	0.2700				
19	11/26/88	1.01950	3.400							1.7000	1.4000	0.3000				
19	03/05/85	1.11000	2.230							0.0600	1.5500	0.6200				
19	01/27/84	1.13000	2.820			0.0900				0.1000	1.5800	0.7600	0.1000			
19	06/08/83	1.13000	2.700							0.0300	1.7100	0.9600				
19	01/06/83	1.12200	2.400							0.1000	1.4000	0.9000				
19	10/15/82	1.15000	1.500							0.1000	1.0000	0.4000				
19	10/15/82	1.15000	1.800							0.1000	1.0000	0.7000				
19	09/14/82	1.08000	1.922			0.0700				0.0220	1.1200	0.5000	0.0700			
19	09/14/82	1.08000	1.900							0.1000	1.0000	0.8000				
19	09/07/82	1.08000	2.540			0.0700				0.2300	1.5600	0.5100	0.0500			
19	08/04/82	1.00000	1.650							0.1000	1.2000	0.3500				
19	08/04/82	1.11000	1.700							0.1000	1.3000	0.3000				
19	01/08/82	1.04000	0.700							0.1000	0.3000	0.3000				
19	11/30/81	1.12000	1.400			0.1000				0.1000	0.4000	0.3000	0.2000			
19	07/03/81	1.22000	3.600			0.1000				0.1000	0.4000	0.3000	0.2000			
19	03/31/81	1.32000	5.400			0.1000				0.1000	3.4000	1.1000	0.3000			
19	03/24/81	1.29000	7.500			0.1000				0.1000	4.6000	1.8000	0.4000			
19	03/02/81	1.27000	5.300			0.1000				0.1000	3.1000	1.3000	0.3000			
19	12/12/80	1.25000	5.100							0.1000	3.2000	1.8000				
19	09/17/80	1.35000	6.400							0.1000	2.8000	1.0000				
19	09/03/80	1.34000	6.800							0.2000	4.7000	1.9000				
19	08/19/80	1.29000	5.800							0.2000	3.7000	1.8000				
19	08/14/80	1.28000	1.800							0.6200						
19	07/21/80	1.38000	6.400							0.1000	4.7000	1.6000				
19	07/18/80	1.39000	6.600							0.1000	4.9000	1.6000				
19	07/14/80	1.37000	5.800							0.1000	4.3000	1.4000				
19	02/20/80	1.42000	10.000							0.7000	1.9000	7.4000				
19	02/15/80	1.40000	5.380							0.1000	4.5000	0.7800				
19	02/04/80	1.43000	10.400							1.3000	2.2000	6.9000				
19	10/14/75	1.43000	10.961	0.6600	0.0003	0.0150	0.0200	0.0050		0.7400	2.4000	6.9000	0.0200	0.0700		
20	04/09/96	1.24510	2.531	0.0100	0.0170	0.0320	0.7500	0.0690		0.5200	0.0740	0.0200	0.0030	0.1400		
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Tank	Date	Density	Na(M)	AlOH4 (M)	C2O4 (M)	CrO4 (M)	Cl (M)	CO3 (M)	Fl (M)	Formate (M)	NO2 (M)	NO3 (M)	OH (M)	PO4 (M)	SO4 (M)	Titanate (M)		
20	07/26/87	1.01970	0.360							0.0900	0.1400	5.0200	0.9900	0.1000	0.1600			
20	05/01/87	1.21000	0.749							0.0800	0.1020	0.4570	0.1900					
20	08/08/86	1.22950	5.580	0.1300						0.0700	0.1000	2.9500	0.2100			0.1600		
20	08/02/86	1.22000	3.260							0.0740	0.0740	3.2000	0.5600			0.1800		
20	07/31/86	1.21890	4.454	0.1200						0.0740	0.1330	3.3000	0.2400					
20	07/14/86	1.35700	7.200	0.2500						0.0900	0.1400	5.0200	0.9900	0.1000	0.1600			
20	06/03/86	1.37000	7.776	0.2200						0.1000	0.1700	5.9600	0.9830	0.1400				
20	05/22/86	1.32700	9.753	0.2570						0.1280	0.1700	7.4300	1.1600			0.2400		
20	04/26/86	1.37000	8.057							0.1100	0.1380	6.4100	0.8890			0.2000		
20	03/14/86	1.35400	8.410							0.1400	0.1400	6.3000	1.3500			0.1700		
20	02/20/86	1.37000	7.253							0.1400	0.1070	5.4300	0.8160			0.3100		
20	11/15/85	1.17000	7.380							0.1200	0.1400	4.9000	1.6800			0.2100		
20	11/01/85	1.39380	3.026							0.0740	0.0740	1.8000	0.8700			0.0670		
20	10/10/85	1.38150	6.454							0.2340	0.2340	5.7600	0.4600					
20	08/12/85	1.39400	5.997							0.2020	0.2020	5.1450	0.6500					
20	07/03/84	1.36000	6.660							0.1500	0.1500	5.3900	1.1200					
20	01/27/84	1.38000	6.614							0.0720	0.2000	4.3500	1.4600			0.2300		
20	01/26/84	1.36000	7.150							0.1800	0.2000	4.9800	1.2100			0.2000		
20	11/11/83	1.37000	6.600								0.2800	0.2800	5.3000	1.0200				
20	10/14/83	1.37000	5.850								0.1300	0.1300	4.2800	1.4400				
20	10/14/83	1.37000	6.350								0.1100	0.1100	4.8000	1.4400				
20	02/17/83	1.49000	6.950								0.2000	0.2000	5.4100	1.3400				
20	01/06/83	1.39000	7.500								0.2000	0.2000	5.9000	1.4000				
20	09/14/82	1.42000	8.160								0.1500	0.1500	6.7900	1.2200				
20	09/14/82	1.40000	6.550								0.1500	0.1500	5.1000	1.3000				
20	09/07/82	1.26000	7.459								0.1990	0.1990	6.0400	1.2200				
20	08/04/82	1.50000	5.100								0.1000	0.1000	4.0000	1.0000				
20	08/04/82	1.27000	7.300								0.1000	0.1000	5.8000	1.4000				
20	11/08/81	1.35000	4.800								0.1000	0.1000	3.5000	1.2000				
20	09/19/81	1.27000	8.080								0.0800	0.0800	6.3000	1.7000				
20	02/15/81	1.06000	4.900							0.1000	0.1000	2.9000	1.1000			0.3000		
20	12/02/80	1.33000	1.100							0.1000	0.1000	0.5000	0.1000			0.1000		
20	11/07/80	1.24000	5.100							0.1000	0.1000	3.5000	0.7000			0.3000		
20	10/09/80	1.09000	3.800							0.1000	0.1000	1.8000	1.1000			0.3000		
20	09/05/80	1.13000	1.000								0.1000	0.1000	0.3000	0.6000				
20	08/20/80	1.16000	3.400								0.1000	0.1000	0.5000	2.8000				
20	07/20/80	1.47000	7.300								0.4000	0.4000	3.1000	3.8000				
20	06/24/80	1.49000	6.300								0.2000	0.2000	3.5000	2.6000				
20	02/20/80	1.63000	9.300								0.8000	0.8000	2.3000	6.2000				
20	02/14/80	1.38000	13.120									1.3200	1.3200	2.7000	9.1000			
20	02/12/80	1.42000	11.060									1.3000	1.3000	2.2000	7.5600			
20	02/01/80	1.40000	11.710									0.1000	0.1000	4.0900	6.5900			
20	10/19/78	1.44600	4.450								0.2300	0.2300	0.7200	3.5000				
21	09/13/01	1.04060	0.874	0.0100	0.0006		0.0003	0.0300	0.0007		0.2148	0.0653	0.5200	0.0005	0.0005			
21	04/26/01	1.03600	0.789	0.0100	0.0002		0.0005	0.0100	0.0005		0.1925	0.0625	0.5000	0.0005	0.0005			
21	02/04/01	1.03630	0.811	0.0100	0.0006		0.0006	0.0100	0.0007		0.1910	0.0650	0.5200	0.0006	0.0005			
21	11/29/00	1.03300	0.747	0.0100	0.0003		0.0003	0.0100	0.0005		0.1831	0.0610	0.4700	0.0003	0.0003			
21	08/23/00	1.03500	0.797	0.0100	0.0007		0.0003	0.0400	0.0013		0.1880	0.0640	0.4500	0.0006	0.0004			
21	06/04/00	1.03500	0.831	0.0100	0.0007		0.0028	0.0400	0.0013		0.1900	0.0630	0.4800	0.0006	0.0004			
21	03/16/00	1.03720	0.805	0.0100	0.0007		0.0003	0.0500	0.0013		0.1360	0.0540	0.5000	0.0006	0.0004			
21	12/21/99	1.04360	0.806	0.0100	0.0007		0.0005	0.0600	0.0013		0.1800	0.0580	0.4300	0.0013	0.0008			
21	10/07/99	1.06100	1.048	0.0100	0.0007		0.0005	0.1500	0.0013		0.2400	0.0600	0.4300	0.0013	0.0008			
21	07/09/99	1.05600	1.135	0.0100	0.0007		0.0009	0.1800	0.0013		0.2400	0.0740	0.3700	0.0250	0.0014			
21	04/18/99	1.10270	1.986	0.0100	0.0007		0.0022	0.6000	0.0013		0.4500	0.1400	0.1600	0.0049	0.0036			
21	01/19/99	1.10100	2.173	0.0100	0.0017		0.0022	0.6600	0.0013		0.4600	0.1400	0.2100	0.0070	0.0036			
21	10/18/98	1.09800	2.024	0.0100	0.0017		0.0022	0.5800	0.0013		0.4300	0.1400	0.2500	0.0071	0.0036			
21	07/19/98	1.09600	2.079	0.0100	0.0017		0.0022	0.5700	0.0013		0.4600	0.1400	0.3000	0.0057	0.0035			
21	01/21/98	1.09500	1.968	0.0100	0.0007		0.0022	0.5200	0.0013		0.3800	0.1300	0.3800	0.0058	0.0031			
21	10/21/97	1.09300	2.057	0.0100	0.0007		0.0020	0.5000	0.0013		0.4000	0.1300	0.4900	0.0057	0.0030			
21	07/20/97	1.09200	1.961	0.0100	0.0007		0.0021	0.4400	0.0026		0.3700	0.1300	0.5400	0.0063	0.0032			
21	04/21/97	1.07300	1.375	0.0100	0.0068		0.0021	0.3900	0.0013		0.3800	0.1400	0.3000	0.0062	0.0031			
21	01/21/97	1.07100	1.457	0.0100	0.0007		0.0021	0.4100	0.0005		0.3700	0.1300	0.1000	0.0059	0.0030			
21	10/24/96	1.07200	1.07000	0.0807	0.0100	0.0007	0.0021	0.0800	0.0005		0.3600	0.1400	0.1100	0.0060	0.0029			
21	07/21/96	1.06800	1.116	0.0100	0.0007		0.0020	0.1200	0.0000		0.3800	0.1100	0.3500	0.0060	0.0025			
21	04/24/96	1.06400	0.779	0.0100	0.0007		0.0020	0.1000	0.0013		0.2400	0.1200	0.1800	0.0063	0.0030			
21	02/01/96	1.07832	0.939	0.0100	0.0007		0.0020	0.1100	0.0005		0.3900	0.1200	0.1700	0.0066	0.0031			
21	10/08/95	1.07220	1.368	0.0100	0.0007		0.0017	0.2500	0.0005		0.4100	0.1200	0.3000	0.0063	0.0030			
21	07/16/95	1.06900	1.009	0.0100	0.0007		0.0029	0.1200	0.0005		0.3900	0.1400	0.2000	0.0065	0.0028			
21	05/03/95	1.07260	1.180	0.0100	0.0017		0.0020	0.1200	0.0013		0.4100	0.1300	0.3600	0.0066	0.0028			
21	01/22/95	1.06680	1.116	0.0100	0.0007		0.0020	0.1200	0.0000		0.3800	0.1100	0.3500	0.0060	0.0025			
21	10/21/94	1.06824	1.043	0.0070	0.0017		0.0025	0.0200	0.0026		0.4200	0.1300	0.4500	0.0065	0.0026			
21	07/27/94	1.08400	2.025	0.0030	0.0007		0.0053	0.3300	0.0044		0.5100	0.1600	0.6500	0.0086	0.0029			
21	04/27/94	1.08551	1.608	0.0000	0.0017		0.0043	0.1100	0.0026		0.5100	0.1600						

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Tank	Date	Density	Na(M)	AlOH4 (M)	C2O4 (M)	CrO4 (M)	Cl (M)	CO3 (M)	Fl (M)	Formate (M)	NO2 (M)	NO3 (M)	OH (M)	PO4 (M)	SO4 (M)	Titanate (M)
21	07/09/85	1.04000	0.210							0.0050	0.1000	0.1000	0.0100			
21	01/08/85	1.03000	0.176							0.0100	0.0920	0.0740				
21	11/14/84	1.07000	3.016								2.9000	0.1160				
21	09/14/84	1.07000	3.199								3.0130	0.1860				
21	09/14/83	1.04000	3.200								3.0100	0.1900				
21	08/05/83	1.11000	1.465							0.0050	0.7200	0.7400				
21	05/06/82	1.16000	3.000							0.1000	2.0000	0.9000				
21	04/22/81	1.19000	3.400							0.1000	2.3000	1.0000				
21	02/14/81	1.32000	3.900							0.1000	2.6000	1.2000				
21	11/19/80	1.21000	2.900							0.1000	1.7000	1.1000				
21	08/07/80	1.13000	3.700							0.1000	2.4000	1.2000				
21	04/28/80	1.21000	3.100							0.1000	2.0000	1.0000				
21	03/26/80	1.16000	1.600							0.1000	0.8000	0.7000				
22	04/26/01	1.03640	0.811	0.0100	0.0005		0.0006	0.0400	0.0005	0.1865	0.0706	0.4600	0.0005	0.0005		
22	02/04/01	1.03500	0.792	0.0100	0.0006		0.0006	0.0500	0.0005	0.1620	0.0460	0.4800	0.0005	0.0005		
22	11/29/00	1.03100	0.742	0.0100	0.0003		0.0006	0.0400	0.0004	0.1260	0.0430	0.4800	0.0003	0.0003		
22	08/24/00	1.03100	0.645	0.0100	0.0007		0.0003	0.0600	0.0005	0.0680	0.0230	0.4200	0.0006	0.0004		
22	06/04/00	1.03200	0.728	0.0100	0.0007		0.0003	0.0400	0.0005	0.1300	0.0440	0.4600	0.0006	0.0004		
22	03/10/00	1.03180	0.701	0.0100	0.0007		0.0003	0.0400	0.0005	0.1230	0.0440	0.4400	0.0006	0.0004		
22	12/20/99	1.02880	0.634	0.0100	0.0007		0.0003	0.0400	0.0005	0.1100	0.0400	0.3900	0.0006	0.0004		
22	10/07/99	1.03100	0.710	0.0100	0.0007		0.0003	0.0500	0.0013	0.1200	0.0350	0.4400	0.0006	0.0004		
22	07/18/99	1.02950	0.718	0.0100	0.0007		0.0003	0.0700	0.0005	0.1200	0.0340	0.4100	0.0006	0.0004		
22	04/18/99	1.03200	0.757	0.0100	0.0007		0.0004	0.0400	0.0005	0.1300	0.0730	0.4600	0.0006	0.0004		
22	01/19/99	1.03300	0.801	0.0100	0.0007		0.0004	0.0500	0.0013	0.1400	0.0460	0.5000	0.0006	0.0004		
22	10/19/98	1.03300	0.770	0.0100	0.0007		0.0004	0.0700	0.0005	0.1200	0.0460	0.4500	0.0006	0.0004		
22	07/19/98	1.03300	0.830	0.0100	0.0007		0.0004	0.0900	0.0005	0.1400	0.0460	0.4500	0.0006	0.0004		
22	01/22/98	1.05300	0.755	0.0100	0.0007		0.0055	0.0400	0.0013	0.1200	0.0450	0.4900	0.0006	0.0004		
22	10/21/97	1.04000	0.987	0.0100	0.0007		0.0012	0.0700	0.0013	0.1500	0.0310	0.6500	0.0006	0.0004		
22	07/21/97	1.05200	1.147	0.0100	0.0007		0.0020	0.1100	0.0013	0.1900	0.0200	0.7000	0.0006	0.0006		
22	04/21/97	1.05900	1.380	0.0100	0.0007		0.0023	0.1300	0.0013	0.2200	0.0230	0.8600	0.0007	0.0006		
22	01/21/97	1.05900	1.372	0.0100	0.0007		0.0026	0.1100	0.0013	0.2200	0.0240	0.8900	0.0006	0.0006		
22	10/24/96	1.05700	1.280	0.0100	0.0007		0.0024	0.1400	0.0005	0.2200	0.0230	0.7400	0.0006	0.0006		
22	07/21/96	1.05600	1.279	0.0100	0.0007		0.0021	0.1100	0.0013	0.2200	0.0220	0.8000	0.0006	0.0006		
22	04/24/96	1.05830	1.281	0.0100	0.0007		0.0023	0.0300	0.0013	0.2300	0.0240	0.9500	0.0007	0.0006		
22	02/25/96	1.05880	1.352	0.0100	0.0007		0.0025	0.0900	0.0013	0.2200	0.0240	0.9100	0.0007	0.0007		
22	02/08/96	1.05200	1.126		0.0000		0.0049			0.2050	0.0023	0.9100	0.0005	0.0006		
22	02/01/96	1.03530	1.280	0.0100	0.0000		0.0020	0.1000	0.0013	0.2300	0.0240	0.8100	0.0006	0.0006		
22	12/21/95	1.04630	1.139	0.0100	0.0007		0.0024	0.0300	0.0013	0.1500	0.0220	0.8900	0.0006	0.0006		
22	11/15/95	1.06280	1.515	0.0100	0.0007		0.0020	0.1100	0.0013	0.0990	0.2700	0.9000	0.0007	0.0048		
22	10/09/95	1.06040	1.416	0.0100	0.0007		0.0025	0.1100	0.0005	0.1800	0.0290	0.9700	0.0007	0.0007		
22	09/08/95	1.06120	1.482	0.0100	0.0007		0.0029	0.1400	0.0005	0.1900	0.0131	0.9800	0.0009	0.0008		
22	08/24/95	1.05539	1.094	0.0100	0.0007		0.0055	0.1200	0.0005	0.2400	0.0300	0.5600	0.0016	0.0013		
22	07/18/95	1.05460	0.948	0.0100	0.0008		0.0064	0.1200	0.0026	0.2500	0.0280	0.4000	0.0022	0.0016		
22	05/03/95	1.04330	0.575	0.0100	0.0009		0.0068	0.1200	0.0005	0.2200	0.0260	0.6000	0.0024	0.0018		
22	03/27/95	1.04388	0.485	0.0100	0.0011		0.0068	0.0600	0.0005	0.2200	0.0250	0.9000	0.0025	0.0018		
22	01/11/95	1.03920	0.401	0.0100	0.0010		0.0066	0.0600	0.0000	0.2100	0.0240	0.0200	0.0022	0.0016		
22	10/20/94	1.03778	0.350	0.0600	0.0011		0.0068	0.0200	0.0013	0.2300	0.0260	0.0100	0.0025	0.0017		
22	07/10/94	1.03850	0.408	0.0020	0.0014		0.0065	0.0610	0.0000	0.2200	0.0260	0.0190	0.0026	0.0018		
22	04/27/94	1.03870	0.517	0.0130	0.0017		0.0085	0.1100	0.0000	0.2200	0.0260	0.0170	0.0025	0.0016		
22	01/05/94	1.03914	0.588	0.0120	0.0009		0.0070	0.1200	0.0000	0.2300	0.0280	0.0590	0.0027	0.0016		
22	09/05/93	1.04010	0.554	0.0110	0.0009		0.0063	0.1000	0.0000	0.2100	0.0230	0.0910	0.0026	0.0018		
22	04/07/93	1.03680	0.819	0.0029	0.0012		0.0067	0.2300	0.0000	0.2000	0.0270	0.1100	0.0026	0.0016		
22	12/14/92	1.03690	0.970	0.0100	0.0100		0.0100	0.2000	0.0100	0.2200	0.0600	0.2000	0.0100	0.0100		
22	09/16/92	1.03680	0.400							0.1500	0.0300	0.2200				
22	06/25/92	1.03490	0.410							0.1800	0.0300	0.2000				
22	03/18/92	1.03720	0.560							0.2300	0.0400	0.2900				
22	12/26/91	1.01840	0.560							0.2200	0.0900	0.2500				
22	09/15/91	1.03330	0.520							0.2100	0.0600	0.2500				
22	06/25/91	1.03640	0.652							0.2330	0.0390	0.3800				
22	04/19/91	1.03750	0.804							0.2600	0.0700	0.4740				
22	01/31/91	1.04000	0.800							0.2600	0.0300	0.5100				
22	10/17/90	1.00660	0.115							0.0400	0.0300	0.0450				
22	03/09/90	1.09010	0.116							0.0280	0.0280	0.0600				
22	11/30/89	0.98350	0.081							0.0260	0.0250	0.0300				
22	08/21/89	0.99150	0.090							0.0200	0.0300	0.0400				
22	03/20/89	1.14930	0.100							0.0500	0.0300	0.0200				
22	12/21/88	1.00740	0.230							0.0700	0.1500	0.0100				
22	09/15/88	1.14860	0.190							0.0400	0.1400	0.0100				
22	08/22/88	1.00600	0.180							0.0400	0.1300	0.0100				
22	03/21/88	1.01680	0.420							0.0880	0.2200	0.1120				
22	09/28/87	0.90520	0.270							0.1400	0.0100	0.1200				
22	08/16/87	0.85000	0.060							0.0100	0.0400	0.0100				
22	09/22/86	1.27000	5.672	0.0540				0.1400		0.0980	3.4400	1.2200		0.2900		
22	07/16/86	1.33000	5.628	0.0580				0.0720		0.1000	3.7800	0.9460		0.3000		
22	07/08/86	1.33000	0.0													

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Tank	Date	Density	Na(M)	AlOH4 (M)	C2O4 (M)	CrO4 (M)	Cl (M)	CO3 (M)	Fl (M)	Formate (M)	NO2 (M)	NO3 (M)	OH (M)	PO4 (M)	SO4 (M)	Titanate (M)
23	07/19/98	1.01500	0.393	0.0100	0.0007	0.0003	0.0400	0.0005			0.1500	0.0280	0.1200	0.0006	0.0009	
23	01/21/98	1.01500	0.331	0.0100	0.0007	0.0003	0.0200	0.0005			0.1100	0.0250	0.1400	0.0006	0.0011	
23	10/21/97	1.01300	0.360	0.0100	0.0007	0.0003	0.0400	0.0005			0.1100	0.0250	0.1300	0.0006	0.0010	
23	07/21/97	1.01000	0.274	0.0100	0.0007	0.0003	0.0400	0.0005			0.0980	0.0210	0.0600	0.0006	0.0010	
23	04/15/97	1.01100	0.292	0.0100	0.0007	0.0003	0.0400	0.0005			0.1000	0.0160	0.0800	0.0006	0.0012	
23	01/21/97	1.01200	0.305	0.0100	0.0007	0.0004	0.0400	0.0005			0.1000	0.0190	0.0900	0.0006	0.0014	
23	10/26/96	1.01140	0.296	0.0100	0.0007	0.0004	0.0400	0.0005			0.1000	0.0200	0.0800	0.0006	0.0013	
23	07/21/96	1.01150	0.294	0.0100	0.0007	0.0004	0.0300	0.0005			0.0970	0.0210	0.1000	0.0006	0.0015	
23	04/24/96	1.01230	0.282	0.0100	0.0007	0.0004	0.0200	0.0005			0.1000	0.0250	0.1000	0.0006	0.0017	
23	02/01/96	1.01270	0.466	0.0100	0.0007	0.0017	0.0300	0.0005			0.1400	0.0310	0.2100	0.0013	0.0042	
23	07/18/95	1.02360	0.565	0.0100	0.0007	0.0007	0.0300	0.0005			0.1600	0.0230	0.3000	0.0006	0.0042	
23	05/03/95	1.01040	0.374	0.0100	0.0007	0.0005	0.1100	0.0005			0.0830	0.0350	0.0100	0.0007	0.0061	
23	03/27/95	1.00660	0.178	0.0100	0.0003	0.0004	0.0100	0.0003			0.0820	0.0320	0.0200	0.0003	0.0062	
23	01/22/95	1.00420	0.136	0.0100	0.0000	0.0004	0.0200	0.0000			0.0650	0.0081	0.0100	0.0006	0.0004	
23	10/20/94	1.00852	0.232	0.0007	0.0003	0.0010	0.0200	0.0000			0.0870	0.0190	0.0800	0.0008	0.0005	
23	07/10/94	1.01170	0.334	0.0030	0.0003	0.0023	0.0250	0.0000			0.1100	0.0250	0.1400	0.0006	0.0008	
23	05/02/94	1.00440	0.163	0.0060	0.0007	0.0017	0.0290	0.0000			0.0680	0.0230	0.0226	0.0006	0.0007	
23	01/12/94	1.00307	0.188	0.0082	0.0000	0.0032	0.0440	0.0000			0.0470	0.0200	0.0190	0.0006	0.0005	
23	10/05/93	1.00100	0.093	0.0014	0.0000	0.0006	0.0100	0.0000			0.0490	0.0190	0.0004	0.0005	0.0005	
23	07/13/93	1.00090	0.266	0.0370	0.0000	0.0004	0.0090	0.0000			0.0390	0.0180	0.1500	0.0008	0.0004	
23	03/29/93	1.01770	0.382	0.0019	0.0000	0.0016	0.0306	0.0000			0.1200	0.0330	0.1594	0.0010	0.0010	
23	12/14/92	1.01630	0.510	0.0100	0.0100	0.0100	0.0500	0.0100			0.1400	0.0300	0.1500	0.0100	0.0100	
23	09/16/92	1.02020	0.410								0.1400	0.0400	0.2300			
23	06/25/92	1.01170	0.250								0.1400	0.0300	0.0800			
23	03/16/92	1.01580	0.300								0.1100	0.0200	0.1700			
23	12/26/91	1.03960	0.730								0.2600	0.0800	0.3900			
23	09/15/91	1.01650	0.300								0.1100	0.0200	0.1700			
23	06/23/91	1.01360	0.222								0.0720	0.0200	0.1300			
23	05/29/91	1.01530	0.537	0.0123							0.1940	0.0440	0.2863			
23	04/19/91	1.01540	0.330								0.0800	0.0300	0.2200			
23	02/01/91	1.04090	0.717								0.2600	0.0370	0.4200			
23	09/18/90	1.00730	0.057								0.0030	0.0170	0.0370			
23	03/08/90	0.99140	0.332								0.0070	0.0250	0.3000			
23	11/30/89	1.00610	0.238								0.0080	0.0200	0.2100			
23	09/27/89	1.03770	0.040								0.0100	0.0200	0.0100			
23	05/22/89	1.01110	0.047								0.0100	0.0270	0.0100			
23	03/08/89	0.99870	0.070								0.0200	0.0400	0.0100			
23	12/21/88	1.02460	0.110								0.0100	0.0800	0.0200			
23	08/22/88	0.99900	0.040								0.0100	0.0200	0.0100			
23	03/22/88	1.00300	0.102								0.0100	0.0320	0.0600			
23	12/08/87	1.02780	0.352								0.0440	0.0080	0.3000			
23	12/01/87	0.98960	0.060								0.0100	0.0400	0.0100			
23	06/04/87	0.90100	0.192								0.0840	0.0080	0.1000			
23	03/23/87	0.95500	0.120								0.0100	0.0100	0.1000			
23	07/14/86	1.02170	0.300								0.1000	0.1000	0.1000			
23	04/21/86	0.99670	0.230								0.1000	0.0300	0.1000			
23	11/14/84	0.98500	0.107								0.0010	0.0500	0.0560			
23	11/14/84	1.01200	0.078								0.0250	0.0290	0.0240			
23	08/16/83	1.02000	0.110								0.0200	0.0400	0.0500			
23	06/09/83	1.00500	0.128								0.0020	0.0460	0.0800			
23	10/11/82	1.04000	0.150								0.0300	0.0700	0.0500			
23	09/09/81	0.94000	0.270								0.1000	0.1000	0.0700			
23	02/19/81	1.02000	0.300								0.1000	0.1000	0.1000			
23	10/24/75	1.00500	0.298	0.0100	0.0000	0.0070	0.0050	0.0010			0.0000	0.2000	0.0600	0.0000	0.0050	
24	09/17/01	1.03450	0.312	0.0010	0.0003	0.0005	0.02441	0.00637			0.0005	0.0005	0.0005	0.0005	0.0005	
24	07/14/01	1.03550	0.883	0.0100	0.0005	0.0004	0.0100	0.0005	0.2570	0.0633	0.5300	0.0005	0.0005	0.0005	0.0005	
24	04/25/01	1.03430	0.396	0.0100	0.0005	0.0005	0.0100	0.0005	0.2504	0.0622	0.0500	0.0005	0.0003	0.0003	0.0003	
24	02/04/01	1.03520	0.872	0.0100	0.0006	0.0001	0.0100	0.0005	0.2370	0.0610	0.5400	0.0005	0.0005	0.0005	0.0005	
24	11/30/00	1.03300	1.035	0.0100	0.0003	0.0001	0.1000	0.0004	0.2280	0.0550	0.5400	0.0003	0.0003	0.0003	0.0003	
24	08/24/00	1.03400	1.027	0.0100	0.0006	0.0043	0.1000	0.0005	0.2177	0.0514	0.5400	0.0005	0.0005	0.0005	0.0005	
24	06/04/00	1.05200	1.147	0.0100	0.0007	0.0043	0.1200	0.0005	0.4990	0.0390	0.3500	0.0006	0.0010	0.0010	0.0010	
24	03/26/00	1.06550	1.345	0.0100	0.0007	0.0082	0.2200	0.0005	0.7300	0.0300	0.1200	0.0007	0.0017	0.0017	0.0017	
24	01/03/00	1.07100	1.198	0.0100	0.0007	0.0085	0.0800	0.0005	0.7700	0.0320	0.2100	0.0008	0.0018	0.0018	0.0018	
24	12/21/99	1.06750	1.233	0.0100	0.0007	0.0084	0.1300	0.0013	0.7000	0.0370	0.2100	0.0007	0.0018	0.0018	0.0018	
24	10/07/99	1.05300	1.114	0.0100	0.0007	0.0010	0.1500	0.0013	0.4200	0.0360	0.3300	0.0007	0.0021	0.0021	0.0021	
24	04/22/98	1.05200	1.040	0.0100	0.0007	0.0090	0.1500	0.0013	0.3500	0.0330	0.3300	0.0007	0.0020	0.0020	0.0020	
24	01/22/98	1.05500	0.997	0.0100	0.0007	0.0088	0.1600	0.0013	0.3400	0.0310	0.2200	0.0008	0.0018	0.0018	0.0018	
24	10/21/97	1.05200	1.189	0.0100	0.0007	0.0089	0.2000	0.0013	0.3500	0.0320	0.3800	0.0007	0.0018	0.0018	0.0018	
24	07/21/97	1.04400	1.182	0.0100	0.0007	0.0110	0.2100	0.0013	0.3500	0.0330	0.3500	0.0008	0.0020	0.0020	0.0020	
24	04/15/97	1.05200	1.161	0.0100	0.0007	0.0095	0.2100	0.0013	0.3300	0.0330	0.3500	0.0009	0.0020	0.0020	0.0020	
24	01/21/97	1.05200	1.061	0.0100	0.0007	0.0094	0.1400	0.0013	0.3300	0.0330	0.3900	0.0008	0.0020	0.0020	0.0020	
24	10/24/96	1.05230	1.013	0.0100	0.0007	0.0098	0.1100	0.0013	0.3400	0.0350	0.3900	0.0009	0.0020	0.0020	0.0	

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Tank	Date	Density	Na(M)	AlOH4 (M)	C2O4 (M)	CrO4 (M)	Cl (M)	CO3 (M)	F1 (M)	Formate (M)	NO2 (M)	NO3 (M)	OH (M)	PO4 (M)	SO4 (M)	Titanate (M)
24	09/03/83	1.06000	1.090								0.2200	0.3400	0.5300			
24	08/22/83	1.50000	11.690							2.4700	3.4200	5.8000				
24	08/22/83	1.32000	5.040							0.2200	3.6400	1.1800				
24	08/15/83	1.38000	5.480							0.1200	3.8600	1.5000				
24	08/12/83	1.38000	5.890							0.2000	3.8600	1.8300				
24	07/26/83	1.34000	6.160							0.2600	4.3500	1.5500				
24	07/18/83	1.34000	5.980							0.3000	4.2000	1.4800				
24	06/18/82	1.34000	5.800							0.5000	4.3000	1.0000				
24	04/16/82	1.43000	6.400							0.4000	4.9000	1.1000				
24	03/09/82	1.36000	4.300							0.3000	3.1000	0.9000				
24	01/29/82	1.41000	6.660							0.4600	5.0000	1.2000				
24	11/25/81	1.37000	18.370			0.5200	0.5200			0.4200	4.9000	1.2100	5.1400			
24	10/20/81	1.41000	10.050	0.5900		0.5200	0.6200			0.5200	5.3000	1.4600		0.2100		
24	10/20/81	1.44000	6.800							0.4000	5.0000	1.4000				
24	10/20/81	1.42000	6.600							0.4000	4.8000	1.4000				
24	10/06/81	1.37000	6.600							0.4000	4.7000	1.5000				
24	08/25/81	1.29000	7.400			0.0400	0.9400			0.4000	3.4000	1.1000		0.2900		
24	08/25/81	1.24000	4.500							0.3000	3.2000	1.0000				
24	02/14/81	1.33000	6.300							0.7000	2.7000	2.9000				
24	10/24/75	1.11300	2.647	0.0590		0.0005	0.0040	0.0240	0.0010	0.2500	0.6700	1.5000	0.0200	0.0270		
24	02/06/73	1.39000	9.845	0.9000		0.0010	0.0400	0.1000	0.0030	1.7000	2.6000	4.3000	0.0200	0.0200		
25	02/12/98	1.44000	12.724	0.5000	0.0068	0.0200	0.1300	0.0130		1.3000	1.3400	9.2200	0.0180	0.0050		
25	04/10/97	1.45000	13.068		0.1160	0.0575	0.2040	0.1070	0.2260	1.2900	1.4600	8.8700	0.1070	0.1060		
25	02/13/97	1.45000	13.832	0.7640	0.1160	0.0575	0.2040	0.1070	0.2260	1.2900	1.4600	8.8700	0.1070	0.1060		
25	01/13/97	1.45400	12.855	0.3400	0.0068	0.0220	0.1400	0.0052		1.3100	1.3200	9.5000	0.0200	0.0056		
25	12/01/95	1.45460	14.463	0.5000	0.0067	0.0310	0.0100	0.0130		1.4300	1.9000	10.4900	0.0200	0.0061		
25	11/30/95	1.39700	10.440							1.2600	1.3700	7.8100				
25	08/31/95	1.44340	13.505	0.4700	0.0068	0.0200	0.1500	0.0130		1.3200	1.8500	9.4600	0.0180	0.0054		
25	08/18/94	1.45390	13.267	0.4700	0.0069	0.0140	0.1400			1.2800	1.8800	9.2500	0.0220	0.0100		
25	08/05/93	1.45900	17.455	0.6100	0.0090	0.0140	0.9700	0.0260		1.5500	2.3900	10.8400	0.0200	0.0082		
25	07/30/92	1.45060	14.128		0.0050	0.2200				1.2600	1.9300	10.6600	0.0140	0.0053		
25	07/30/92	1.45060	13.850							1.2600	1.9300	10.6600				
25	07/30/92	1.48200	14.068	0.5500	0.0050	0.2200				1.3000	1.3400	10.6000	0.0140	0.0053		
25	07/26/91	1.45500	12.970							1.3200	1.9100	9.7400				
25	05/15/89	1.44410	10.200							1.3600	1.6900	7.1500				
25	11/04/88	1.46000	8.870							1.3600	2.3500	5.1600				
25	04/21/88	1.45008	20.732							7.9800	1.5600	11.1920				
25	10/07/87	1.32160	7.150							0.0240	0.0260	7.1000				
25	04/04/86	1.46000	11.650							1.4900	1.7600	8.4000				
25	08/19/85	1.64000	8.550							1.4500	2.7200	4.3800				
25	03/19/85	1.41000	6.370							1.0400	2.4900	2.8500				
25	02/09/84	1.41000	11.220							1.2500	0.3050	6.9200				
25	03/18/83	1.42000	10.470							0.8500	3.6200	6.0000				
25	06/30/82	1.47000	11.700							1.3000	2.8000	7.6000				
25	11/10/81	1.46000	8.400							0.8000	3.2000	4.4000				
25	11/06/81	1.44000	11.400							1.2000	3.1000	7.1000				
25	10/16/81	1.43000	6.400							0.2000	5.6000	6.0000				
25	04/08/81	1.42000	9.000							0.9000	2.9000	5.2000				
25	09/22/80	1.52000	10.400							1.3000	1.9000	7.2000				
26	08/15/01	1.46000	13.663	0.9500	0.0057	0.0249	0.0100	0.0062		2.0308	1.5644	9.0000	0.0131	0.0108		
26	05/27/01	1.46990	12.439	0.3100	0.0066	0.0235	0.0100	0.0062		1.8762	2.0004	8.1200	0.0120	0.0190		
26	02/27/01	1.35130	8.530	0.3100	0.0063	0.0148	0.0300	0.0054		1.0904	1.6795	5.2800	0.0078	0.0301		
26	12/06/00	1.32700	8.834	0.4200	0.0058	0.0200		0.0100		1.1660	2.3170	4.8200	0.0071	0.0269		
26	09/08/00	1.46000	14.044	0.6300	0.0056	0.0240	0.0100	0.0052		2.0890	1.7599	9.4500	0.0134	0.0099		
26	06/30/00	1.47000	12.729	0.8600	0.0012	0.0203	0.0800	0.0010		2.1790	1.8270	7.6300	0.0102	0.0098		
26	04/11/00	1.31000	10.387	0.7000	0.0070	0.0150	0.0600	0.0140		1.5800	1.6200	6.2800	0.0091	0.0120		
26	12/09/99	1.37870	9.774	0.4600	0.0068	0.0140	0.0100	0.0130		1.4000	1.3900	6.4200	0.0087	0.0120		
26	10/06/99	1.48431	12.536	0.7600	0.0068	0.0180	0.0100	0.0130		1.9800	1.8200	7.8600	0.0100	0.0140		
26	07/22/99	1.43000	11.235	0.5500	0.0068	0.0140	0.0100	0.0130		1.8000	2.5700	6.2100	0.0077	0.0140		
26	05/18/99	1.43000	9.818	0.5200	0.0067	0.0180	0.0300	0.0130		2.1100	1.9200	5.1200	0.0087	0.0120		
26	12/02/98	1.32000	9.629	0.4590	0.0061	0.0057	0.3370	0.0061		1.0800	1.8400	5.4800	0.0061	0.0301		
26	09/16/98	1.41000	13.474	3.0000	0.0068	0.0150	0.2800	0.0130		1.6300	2.2900	5.8900	0.0090	0.0210		
26	04/20/98	1.43000	11.531	0.4100	0.0068	0.0180	0.0800	0.0130		1.2500	2.3600	7.2700	0.0063	0.0120		
26	02/18/98	1.36000	9.636	0.3800	0.0068	0.0140	0.1400	0.0130		1.0000	2.1400	5.7400	0.0079	0.0190		
26	12/03/97	1.42000	10.912	0.4200	0.0068	0.0170	0.0200	0.0130		1.2300	2.4500	6.6700	0.0098	0.0180		
26	07/30/97	1.40000	11.333	0.4800	0.0068	0.0170	0.0100	0.0130		1.2200	2.7900	6.7200	0.0100	0.0180		
26	04/17/97	1.42900	11.083	0.4200	0.0068	0.0150	0.2400	0.0130		1.1000	3.0800	5.9000	0.0094	0.0200		
26	01/13/97	1.36900	9.530	0.3200	0.0068	0.0140	0.1600	0.0130		0.9100	2.6400	5.2100	0.0082	0.0360		
26	11/05/96	1.35700	7.745	0.2200	0.0072	0.0120	0.2100	0.0140		0.5700	2.0900	4.3200	0.0067	0.0360		
26	08/01/96	1.40900	10.033	0.1900	0.0068	0.0170	0.0600	0.0130		0.9400	3.0000	5.6600	0.0080	0.0310		
26	05/17/96	1.41300	10.361	0.0100	0.0071	0.0190	0.0100	0.0140		0.9200	3.4800	5.8100	0.0077	0.0290		
26	11/21/95	1.36750	8.701	0.2800	0.0068	0.0180	0.0600	0.0130		0.8100	2.9800	4.3400	0.0063	0.0570		
26	08/18/95	1.33900	9.193	0.2900	0.0068	0.0140	0.5900	0.0053		0.7400	2.7700	4.0200	0.0064	0.0740		
26	05/11/95	1.38410	8.123	0.1300	0.0075	0.0130	0.1300	0.0052		0.6800	2.8200	4.0300	0.0063	0.0790		
26	02/28/95	1.42480	8.149	0.2400	0.0090	0.0140	0.0500	0.0180		0.7200	2.770					

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Tank	Date	Density	Na(M)	AlOH4 (M)	C2O4 (M)	CrO4 (M)	Cl (M)	CO3 (M)	Fl (M)	Formate (M)	NO2 (M)	NO3 (M)	OH (M)	PO4 (M)	SO4 (M)	Titanate (M)	
26	09/16/82	1.32000	4.150								0.1500	2.2000	1.8000				
26	06/21/82	1.20000	4.500							0.4000	2.4000	1.7000					
26	06/03/82	1.27000	6.000							0.6000	2.6000	2.8000					
26	05/24/82	1.26000	3.430							0.1000	2.5000	0.8300					
26	05/24/82	1.26000	3.340							0.1600	2.3000	0.8800					
26	02/22/82	1.49000	10.500							1.5000	1.8000	7.2000					
26	02/22/82	1.48000	10.600							1.4000	2.0000	7.2000					
26	12/03/81	1.52000	9.300							1.3000	1.2000	6.8000					
26	06/12/81	1.42000	9.500							1.2000	2.3000	6.0000					
26	03/24/81	1.42000	7.600							0.8000	2.9000	3.9000					
26	09/22/80	1.32000	11.400							1.5000	3.1000	6.8000					
26	03/06/80	1.16000	5.100							0.5000	1.5000	3.1000					
26	02/01/80	1.14000	3.020							0.1000	1.2200	1.7000					
26	01/25/80	1.08000	1.700							0.1000	0.8000	0.8000					
27	06/24/99	1.48000	14.012	0.0100	0.0067		0.0210	0.1400	0.0130	1.4200	1.7100	10.4800	0.0180	0.0086			
27	07/09/97	1.48000	14.319	1.0800	0.0068	0.0220	0.1200	0.0130		1.3400	2.0000	9.5400	0.0210	0.0069			
27	07/09/96	1.45060	12.626	0.3400	0.0068	0.0200	0.0900	0.0130		1.1900	1.6700	9.1400	0.0170	0.0077			
27	08/21/95	1.43840	13.286	0.4100	0.0069	0.0190	0.4900	0.0130		1.2100	1.7100	8.8700	0.0150	0.0110			
27	08/18/94	1.46035	13.291	0.3800	0.0170	0.0140	0.1200	0.0000		1.2900	1.8400	9.4100	0.0180	0.0230			
27	08/05/93	1.45624	15.251	0.5100	0.0090	0.0140	0.9900	0.0260		1.0200	1.4600	10.1600	0.0180	0.0092			
27	07/21/92	1.50820	13.782	0.4200	0.0050	0.0210				1.1800	1.9400	10.1600	0.0130	0.0085			
27	07/21/92	1.50820	13.280							1.1800	1.9400	10.1600					
27	07/21/92	1.45300	12.962	0.4200	0.0050	0.0210				1.2000	1.3600	9.9000	0.0130	0.0085			
27	08/02/91	1.42230	12.120							1.1500	2.0700	8.9000					
27	05/24/90	1.43280	11.370							1.3000	1.8000	8.2700					
27	05/15/89	1.40170	10.570							1.0600	1.7000	7.8100					
27	11/04/88	1.26390	6.200							0.7200	0.8700	4.6100					
27	04/21/88	1.66810	16.390							1.9000	1.7500	12.7400					
27	10/07/87	1.30180	7.149							0.0220	0.0270	7.1000					
27	04/03/87	1.32250	2.870								1.0100	1.2300	0.6300				
27	11/25/86	1.29840	6.810							1.4200	1.7400	3.6500					
27	10/20/84	1.35800	6.213							1.5550	3.6440	1.0140					
27	02/09/84	1.40000	9.780							0.8400	3.4000	5.5400					
27	08/23/83	1.43000	5.990							1.0300	2.3600	2.6000					
27	03/18/83	1.35000	7.170							0.4900	2.3300	4.3500					
27	03/25/82	1.58000	6.800							0.6000	2.9000	3.3000					
27	10/16/81	1.30000	5.700							0.5000	2.6000	2.6000					
27	08/19/80	1.37000	9.500							1.5000	2.6000	5.4000					
27	03/06/80	1.36000	7.400							0.5000	4.1000	2.8000					
27	02/01/80	1.32000	10.280							0.5500	6.5400	3.1900					
27	01/25/80	1.38000	9.540							0.4300	6.2700	2.8400					
27	01/24/80	1.38000	9.540							0.4300	6.2700	2.8400					
28	06/29/99	1.46000	11.578	0.5100	0.0068	0.0210	0.0400	0.0130		1.7200	2.1000	7.0400	0.0240	0.0076			
28	08/26/97	1.44000	12.092	0.5800	0.0068	0.0200	0.1100	0.0130		1.4400	1.9400	7.7900	0.0220	0.0080			
28	08/26/96	1.44420	12.888	0.0100	0.0068	0.0200	0.0100	0.0130		1.4400	2.0000	9.3000	0.0210	0.0077			
28	08/31/95	1.46490	13.674	0.6000	0.0069	0.1000	0.1700	0.0130		1.5400	2.0700	8.9200	0.0220	0.0088			
28	07/08/94	1.42380	13.038	0.6300	0.0069	0.0084	0.2400	0.0130		1.5000	1.8000	8.5200	0.0200	0.0099			
28	07/23/93	1.37550	11.033	0.8800	0.0090	0.0110	0.3000	0.0210		1.2200	1.5700	6.6400	0.0210	0.0094			
28	07/21/92	1.46320	13.031	0.6400		0.0260				1.3700	2.0000	8.9400	0.0140	0.0066			
28	07/21/92	1.46320	12.310							1.3200	1.3700	8.5000	0.0140	0.0066			
28	07/26/91	1.45090	11.750							1.3400	2.1200	8.2900					
28	05/24/90	1.45090	12.080							1.7300	2.0400	8.3100					
28	05/15/89	1.43990	10.930							1.5000	1.7500	7.6800					
28	11/04/88	1.42860	11.170							1.2700	2.0600	7.8400					
28	04/21/88	1.57486	13.609							1.4300	2.0500	10.1290					
28	10/07/87	1.31620	7.057							0.0220	0.0250	7.0100					
28	11/26/86	1.18450	4.940							1.6200	1.4600	1.8600					
28	04/04/86	1.38000	9.560							1.0500	2.9700	5.5400					
28	08/19/85	1.41000	6.960							0.9700	2.9000	3.0900					
28	03/19/85	1.44000	7.450							1.6400	1.7200	4.0900					
28	12/01/83	1.48000	12.350							1.5500	2.3800	8.4200					
28	03/18/83	1.47000	10.780							0.6000	3.0200	7.1600					
28	04/22/82	1.57000	13.400							1.6000	1.6000	10.2000					
28	10/16/81	1.53000	11.900							1.7000	1.3000	8.9000					
28	04/08/81	1.28000	11.900							1.6000	2.4000	7.9000					
28	11/10/80	1.54000	12.600							1.7000	2.5000	8.4000					
28	09/08/80	1.55000	13.400							2.2000	2.2000	9.0000					
28	03/13/80	1.36000	7.900							0.6000	2.3000	5.0000					
28	02/01/80	1.24000	5.940							0.2200	2.5800	3.1400					
29	06/19/01	1.18630	4.097	0.3200	0.0064	0.0053	0.0100	0.0059		0.8792	0.8491	1.9700	0.0073	0.0097			
29	05/02/01	1.37380	8.990	0.7700	0.0058	0.0109	0.0500	0.1053		1.9700	2.1000	3.8400	0.0203	0.0135			
29	02/15/01	1.10000	2.210	0.1000	0.0062	0.0034	0.1300	0.0057		0.3889	0.4228	1.0000	0.0037	0.0057			
29	12/02/00	1.36200	7.822	0.4800	0.0057	0.0126	0.1700	0.0053		1.6410	1.6800	3.5700	0.0163	0.0191			
29	09/10/00	1.30000	6.024	0.6200	0.0057	0.0094	0.1600	0.0053		1.3397	1.3931	2.2600	0.0151	0.0126			
29	03/18/99	1.41000	9.866	0.7700	0.0068	0.0082	0.1900	0.0133		1.9950	2.0770	4.5200	0.0217	0.0151			
29	09/24/99	1.43000	10.192	0.4800	0.0069	0.0040	0.1200	0.0130		2.1200	1.9000	5.3300	0.0220	0.0160			
29	03/29/99	1.40000	10.599	0.7800	0.0069	0.0087	0.3000	0.0130		2.2500	2.0600	4.8000	0.0160	0.0160			
29	12/02/98	1.42000	12.338	0.8130	0.0062	0.0054	0.3270	0.0058		1.9000	1.9300	6.9600	0.0116	0.0143			
29	01/22/98	1.36000	8.813	0.5800	0.0068	0.0074	0.0200	0.0130		1.8400	1.7400	4.5100	0.0200	0.0081			
29	12/18/96	1.47000	11.558	0.9400	0.0068	0.0100	0.0600	0.0130		2.3700	2.3700	5.6000	0.0280	0.0220			

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Tank	Date	Density	Na(M)	AlOH4 (M)	C2O4 (M)	CrO4 (M)	Cl (M)	CO3 (M)	Fl (M)	Formate (M)	NO2 (M)	NO3 (M)	OH (M)	PO4 (M)	SO4 (M)	Titanate (M)
30	02/15/01	1.29000	5.154	0.3200	0.0054	0.0063	0.1200	0.0071		0.8860	1.5900	0.2300	0.0050	0.0270		
30	12/01/00	1.47000	10.405	0.7400	0.0057	0.0149	0.0100	0.0053		2.0890	3.0310	4.4400	0.0091	0.0159		
30	12/01/00	1.44000	5.500							0.8000	1.7000	3.0000				
30	12/01/00	1.14000	6.100							0.9000	1.9000	3.3000				
30	12/01/00	1.08000	6.600							1.0000	2.0000	3.6000				
30	09/10/00	1.43540	10.680	0.7900	0.0056	0.0260	0.0100	0.0052		1.7002	2.9874	5.0300	0.0156	0.0344		
30	06/17/00	1.38000	8.197	0.4800	0.0071	0.0045	0.1500	0.0055		1.2611	3.0210	2.9800	0.0066	0.0541		
30	06/08/00	1.41000	9.251			0.0030				1.0600	3.0000	5.1000		0.0440		
30	05/16/00	1.06500	0.873	0.0100	0.0069	0.0028	0.0100	0.0053		0.0840	0.1960	0.5200	0.0064	0.0042		
30	11/24/99	1.37080	10.492	0.0100	0.0067	0.0070	0.1100	0.0130		1.2600	3.2100	5.6300	0.0076	0.0560		
30	06/02/99	1.42590	10.542	0.5900	0.0069	0.0062	0.1100	0.0130		1.4200	3.2600	4.9000	0.0081	0.0510		
30	12/14/98	1.42000	10.274	0.7200	0.0071	0.0071	0.1800	0.0130		1.3800	2.6500	5.0000	0.0081	0.0560		
30	09/17/97	1.40000	9.950	0.4800	0.0068	0.0065	0.2200	0.0130		1.1700	3.1400	4.5700	0.0072	0.0510		
30	09/19/96	1.32000	7.346	0.2200	0.0068	0.0053	0.0100	0.0130		0.9000	2.5600	3.5200	0.0063	0.0410		
30	09/08/95	1.33920	7.610	0.4300	0.0068	0.0049	0.2200	0.0053		0.8600	2.2300	3.5400	0.0063	0.0370		
30	09/21/94	0.99150	7.421	0.3700	0.0140	0.0160	0.1800	0.0220		0.9400	2.1200	3.4500	0.0130	0.0450		
30	09/05/93	1.39819	10.737	0.6600	0.0170	0.0140	0.5700	0.0000		1.2500	3.3500	4.1600	0.0160	0.0490		
30	04/30/93	1.42430	10.739	0.5800	0.0089	0.0056	0.4300	0.0000		1.2200	3.1100	4.8200	0.0083	0.0550		
30	11/29/92	1.28000	7.353	0.4800	0.0100	0.0045				0.6700	2.1900	3.9000	0.0020	0.0460		
30	11/29/92	1.35710	9.190	0.3600	0.0100	0.0200	0.4200	0.0100		1.1600	2.9800	3.6400	0.0100	0.0700		
30	03/18/92	1.36450	6.180							0.7500	2.4000	3.0300				
30	09/04/91	1.35270	7.440							0.9800	3.3000	3.1600				
30	02/25/91	1.36530	8.860							1.0900	4.3600	3.4100				
30	01/23/91	1.36240	8.370							1.0900	3.4700	3.8100				
30	08/26/90	1.35920	8.749							0.9900	3.3900	4.3500	0.0063			
30	03/09/90	1.34700	8.797							1.1120	3.9450	3.7400				
30	12/15/89	1.38450	8.560							1.1100	3.6000	3.8500				
30	09/27/89	1.39290	7.900							0.9500	3.4900	3.4600				
30	08/22/88	1.34930	8.080							1.0300	2.9700	4.0800				
30	09/06/86	1.16400	4.490							0.4700	3.1400	0.8800				
30	06/11/86	1.31340	5.590							0.8500	3.4300	3.1300				
30	08/05/83	1.54000	16.710							3.0100	2.0400	11.6600				
31	03/12/99	1.47000	11.198	0.8600	0.0068	0.0098	0.0500	0.0130		2.5000	2.3900	5.2200	0.0220	0.0160		
31	09/17/97	1.45000	11.486	0.8400	0.0068	0.0089	0.2900	0.0130		1.9800	2.9000	5.0600	0.0230	0.0140		
31	09/19/96	1.38300	9.716	0.7800	0.0070	0.0084	0.0100	0.0130		1.7500	2.4200	4.6200	0.0220	0.0160		
31	07/23/96	1.18800	3.861	0.1100	0.0070	0.0056	0.0100	0.0054		0.6800	0.7200	2.2600	0.0089	0.0130		
31	05/04/95	1.45300	11.520	0.9000	0.0068	0.0099	0.1500	0.0052		1.9600	3.1600	5.0700	0.0220	0.0210		
31	04/27/94	1.41460	5.960	0.0880	0.0180	0.0150	0.0570	0.0000		1.9300	3.2200	0.4600	0.0210	0.0260		
31	04/07/93	1.42930	10.890	0.7700	0.0100	0.0000	0.5300	0.0000		1.6400	3.1400	4.1300	0.0240	0.0340		
31	03/18/92	1.43320	7.530							1.2500	3.1000	3.1800				
31	09/04/91	1.46240	11.410							2.4400	2.5300	6.4400				
31	02/25/91	1.40880	8.130							1.2800	2.7200	4.1300				
31	09/18/90	1.50240	10.940							2.6700	1.9700	6.3000				
31	03/09/90	1.42950	12.040							2.7390	2.6410	6.6600				
31	01/03/90	1.43320	9.320							1.9900	2.7700	4.5600				
31	09/27/89	1.50880	12.080							2.7800	2.2900	7.0100				
31	12/11/88	1.48110	9.760							1.3500	1.5700	6.8400				
31	08/30/88	1.46490	11.210							2.4500	1.9800	6.7800				
31	06/11/86	1.51100	9.500							2.7500	3.1600	3.5900				
31	08/08/83	1.61000	14.660							3.1200	1.8700	9.6700				
31	09/13/82	1.50000	11.400							2.3000	1.6000	7.5000				
31	09/03/81	1.54000	12.800	0.9000						2.4000	1.8000	7.7000				
31	04/22/81	1.38000	13.100							3.1000	2.6000	7.4000				
31	02/25/81	1.50000	8.090							0.8000		7.2900				
31	11/10/80	1.44000	10.100							1.9000	3.4000	4.8000				
31	07/08/80	1.41000	8.800							1.4000	4.2000	3.2000				
31	06/10/80	1.60000	9.200							1.0000	5.6000	2.6000				
31	04/28/80	1.36000	5.600							0.3000	4.4000	0.9000				
31	04/11/80	1.27000	5.500							0.4000	4.0000	1.1000				
31	02/27/80	1.32000	8.800							1.8000	3.3000	3.7000				
31	02/27/80	1.51000	9.430							1.7000	3.7000	4.0300				
31	02/13/80	1.57000	10.020							1.6200	4.0000	4.4000				
31	02/07/80	1.47000	19.820							9.7000	2.3000	7.8200				
31	02/07/80	1.56000	12.100							3.3000	3.0000	5.8000				
31	01/31/80	1.40000	12.970							1.9700	6.7300	4.2700				
31	01/30/80	1.43000	11.970							1.6900	6.4200	3.8600				
32	08/16/01	1.40800	4.393	0.2100	0.0055	0.0027	0.0000	0.0051		0.7134	1.1687	2.2600	0.0051	0.0062		
32	05/15/01	1.44170	7.206	0.1300	0.0063	0.0067	0.0500	0.0061		1.0390	2.0150	3.8300	0.0068	0.0262		
32	02/15/01	1.44700	9.036	0.7600	0.0058	0.0110	0.0300	0.0054		1.8300	1.7600	4.5600	0.0073	0.0111		
32	12/05/00	1.43000	10.501	0.8500	0.0057	0.0126	0.0100	0.0053		1.8590	2.8240	4.8600	0.0088	0.0191		
32	06/29/00	1.52000	4.396	0.4700	0.0070	0.0032	0.0100	0.0054		0.8500	1.8730	1.0800	0.0070	0.0333		
32	04/06/00	1.32000	7.071	0.4900	0.0069	0.0030	0.0100	0.0053		1.1700	2.8500	2.4100	0.0053	0.0500		
32	11/28/99	1.34000	5.979	0.6800	0.0069	0.0028	0.0700	0.0053		1.0500	2.6300	1.3500	0.0053	0.0490		
32	08/05/99	1.38000	6.288	0.4200	0.0069	0.0028	0.1000	0.0130		1.0700	2.4000	2.0500	0.0064	0.0530		
32	03/02/99	1.32000	6.548	0.3800	0.0068	0.0033	0.0100	0.0053		1.5100	2.3900	2.1100	0.0063	0.0520		
32	06/13/98	1.29000	6.042	0.4200	0.0069	0.0028	0.1600	0.0053		1.1800	2.3900	1.5800	0.0064	0.0590		
32	06/28/97	1.27000	6.224	0.4400	0.0068	0.0028	0.2600	0.0053		1.0900						

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Tank	Date	Density	Na(M)	AlOH4 (M)	C2O4 (M)	CrO4 (M)	Cl (M)	CO3 (M)	Fl (M)	Formate (M)	NO2 (M)	NO3 (M)	OH (M)	PO4 (M)	SO4 (M)	Titanate (M)
33	11/05/96	1.12000	3.151	0.1800	0.0072	0.0030	0.1200	0.0056	0.0770	1.4500	1.0800	0.0067	0.0440			
33	04/09/96	1.15500	3.170	0.0600	0.0068	0.0028	0.0100	0.0130	0.0800	1.6300	1.2300	0.0064	0.0540			
33	09/09/95	1.15420	3.584	0.0600	0.0096	0.0044	0.1500	0.0053	0.1200	1.6800	1.3100	0.0063	0.0380			
33	02/27/95	1.12880	2.788	0.0700	0.0068	0.0014	0.0200	0.0026	0.0720	1.0800	1.4500	0.0016	0.0300			
33	08/18/94	1.23280	5.417	0.1600	0.0081	0.0200	0.2700	0.0100	0.4500	2.5200	1.4300	0.0063	0.1300			
33	02/01/94	1.24775	5.358	0.1700	0.0065	0.0056	0.1600	0.0066	0.4900	2.5300	1.5400	0.0032	0.1400			
33	08/12/93	1.24576	5.727	0.1800	0.0063	0.0028	0.2100	0.0180	0.4900	2.6400	1.6600	0.0100	0.1400			
33	02/24/93	1.26040	5.890	0.2900	0.0100	0.0100	0.3200	0.0100	0.5400	2.9600	1.0800	0.0100	0.1600			
33	08/28/92	1.25400	4.590						0.4400	2.6100	1.5400					
33	02/26/92	1.25340	4.140						0.4000	2.3600	1.3800					
33	06/26/91	1.23620	4.420						0.4200	2.5000	1.5000					
33	01/09/91	1.22960	4.460						0.4400	2.6200	1.4000					
33	08/01/90	1.24040	4.850						0.4400	2.8300	1.5800					
33	01/24/90	1.20860	4.690						0.4200	2.9400	1.3300					
33	02/13/89	1.22400	4.350						0.3800	2.8200	1.1500					
33	08/23/88	1.22860	4.960						0.28400	0.3000	1.8200					
33	01/08/87	1.12710	4.910						0.7100	2.6600	1.5400					
33	08/18/86	1.26300	3.550						0.3800	2.1600	1.0100					
33	04/26/85	1.28230	4.736						0.4478	3.2230	1.0650					
33	08/06/84	1.27000	6.330						1.6300	3.4600	1.2400					
33	02/10/84	1.32000	8.330						0.4600	4.6400	3.2300					
33	07/12/83	1.34000	13.270						0.6700	3.6500	8.9500					
33	12/27/82	1.48000	9.200						0.7000	4.8000	3.7000					
33	12/14/82	1.39000	8.800						0.8000	3.9000	4.1000					
33	11/16/81	1.51000	11.500						2.2000	1.7000	7.6000					
33	03/06/80	2.06000	17.900						3.5000	4.0000	10.4000					
34	07/14/99	1.40000	11.257	0.2900	0.0074	0.0160	0.5300	0.0130	1.1600	2.4700	6.1600	0.0069	0.0300			
34	08/27/97	1.38000	9.364	0.4600	0.0068	0.0150	0.2000	0.0130	0.8500	2.6600	4.8700	0.0076	0.0330			
34	04/10/97	1.38000	9.906		0.1140	0.0606	0.2000	0.1050	0.2220	0.8710	2.5100	5.1000	0.1050	0.1040		
34	02/13/97	1.38000	10.112	0.2000	0.1140	0.0606	0.2040	0.1050	0.2200	0.8710	2.5100	5.1000	0.1050	0.1040		
34	06/18/96	1.37900	10.172	0.1700	0.0068	0.0140	0.1600	0.0013	0.9000	2.4600	6.2000	0.0078	0.0380			
34	07/18/95	1.38600	9.219	0.2700	0.0068	0.0070	0.0100	0.0052	0.9900	2.3100	5.5200	0.0081	0.0330			
34	01/20/95	1.39880	10.349	0.2900	0.0068	0.0170	0.0100	0.0140	1.0600	2.2800	6.5500	0.0091	0.0420			
34	07/09/94	1.24670	5.826	0.1900	0.0068	0.0045	0.3600	0.0160	0.4000	2.1400	2.0500	0.0063	0.1400			
34	01/29/94	1.24810	7.156	0.4400	0.0038	0.0030	0.7300		0.3700	2.3800	2.1900	0.0032	0.1500			
34	07/23/93	1.22080	5.457	0.1400	0.0042	0.0033	0.2400	0.0160	0.3500	2.3600	2.0500	0.0084	0.0140			
34	01/18/93	1.24390	7.165	0.0400	0.0042	0.0073	0.8600	0.0230	0.3700	2.3600	2.3400	0.1500				
34	07/30/92	1.25430	4.900						0.3500	2.2900	2.2600					
34	01/15/92	1.27950	5.160						0.3600	2.4500	2.3500					
34	07/31/91	1.22050	4.600						0.3200	2.6200	1.6600					
34	01/09/91	1.21950	4.570						0.2600	2.3400	1.9700					
34	08/01/90	1.26050	5.340						0.2400	2.7400	2.3600					
34	01/24/90	1.23080	4.370						0.1800	2.4600	1.7300					
34	02/13/89	1.20400	2.050						0.1000	1.9300	0.0200					
34	11/04/88	1.20130	4.400						0.1000	2.3600	1.9400					
34	04/21/88	1.16260	15.270						0.1000	1.7800	13.3900					
34	10/07/87	1.16210	2.479						0.0087	0.0507	2.4200					
34	04/04/86	1.25040	2.690						0.1000	1.5200	1.0700					
34	11/26/85	1.18160	3.774						0.1790	2.5450	1.0500					
34	08/19/85	1.22600	2.190						0.2100	1.9800						
34	03/19/85	1.22000	3.780						0.2600	2.6700	0.8500					
34	01/04/83	1.88000	6.800						0.8000	3.3000	2.7000					
34	07/22/82	1.30000	4.600						0.1000	2.3000	2.2000					
34	01/08/82	1.22000	3.600						0.1000	1.8000	1.7000					
34	08/25/81	1.25000	4.400						0.2000	2.2000	2.0000					
34	08/25/81	1.28000	5.300						0.5000	2.3000	2.5000					
34	04/07/81	1.42000	8.100						1.0000	3.2000	3.9000					
34	09/10/80	1.25000	5.700						0.3000	2.5000	2.9000					
34	04/30/80	1.34000	6.700						0.8000	3.3000	2.6000					
34	01/25/80	1.24000	7.290						0.9400	4.0700	2.2800					
35	01/06/01	1.35390	7.194	0.3100	0.0057	0.0262	0.1500	0.0068	1.3719	2.1915	2.9000	0.0061	0.0319			
35	05/17/00	1.30700	6.757	0.4600	0.0069	0.0046	0.0100	0.0130	1.1000	2.1800	2.8800	0.0063	0.0370			
35	11/23/99	1.30000	6.668	0.4100	0.0069	0.0032	0.0100	0.0130	1.1200	2.0700	2.9300	0.0064	0.0380			
35	05/29/99	1.32000	6.730	0.5400	0.0069	0.0028	0.1500	0.0053	1.0800	2.8500	1.8300	0.0063	0.0480			
35	12/09/98	1.31000	6.789	0.6000	0.0160	0.0068	0.0100	0.0013	1.2400	3.4800	1.1800	0.0015	0.1200			
35	06/13/98	1.33000	6.692	0.5000	0.0068	0.0028	0.1800	0.0053	1.0700	2.9900	1.6400	0.0063	0.0490			
35	08/23/97	1.28000	5.943	0.5300	0.0010	0.0070	0.2400	0.0010	0.7300	2.6900	1.4200	0.0020	0.0390			
35	06/26/97	1.31000	6.862	0.5300	0.0068	0.0028	0.2700	0.0053	0.9400	3.0800	1.6400	0.0063	0.0490			
35	12/08/96	1.31700	6.592	0.5800	0.0069	0.0028	0.0200	0.0053	0.9600	3.1300	1.7500	0.0064	0.0490			
35	07/17/96	1.30700	6.574	0.5200	0.0100	0.0029	0.0100	0.0054	0.9200	3.0200	1.9600	0.0065	0.0480			
35	07/16/96	1.30000	7.261	0.6100	0.0120	0.0120	0.1300	0.0220	0.8800	3.4100	1.9300	0.0110	0.0460			
35	07/01/96	1.31000	6.575	0.5200	0.0068	0.0029	0.0100	0.0100	0.9200	3.0200	1.9600	0.0065	0.0480			
35	11/15/95	1.30940	6.822	0.5100	0.0068	0.0050	0.1600	0.0053	0.9600	3.0700	1.8200	0.0063	0.0530			
35	05/09/95	1.30790	6.710	0.4800	0.0067	0.0028	0.0700	0.0052	0.9100	3.1600	1.8200	0.0310	0.0460			
35	11/24/94	1.31030	6.639	0.5400	0.0069	0.0028	0.0600	0.0260	0.9000	2.9600	1.9700	0.0064	0.0470			
35	05/27/94	1.11540	10.222	0.7300	0.0068	0.0190	1.8400	0.0260	0.7800	2.8100	2.0900	0.0400				
35	11/21/93	1.29500	8.391	1.0500	0.0068	0.0140	0.9200	0.0130	0.8700	3.1000	1.3900	0.0063	0.0440			
35	05/27/93	1.28700	7.645	0.5500	0.0220	0.0140	0.3600	0.0260	0.8600	3.0600	2.2400	0.0210	0.0450			
35	11/29/92	1.330														

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Tank	Date	Density	Na(M)	AlOH4 (M)	C2O4 (M)	CrO4 (M)	Cl (M)	CO3 (M)	Fl (M)	Formate (M)	NO2 (M)	NO3 (M)	OH (M)	PO4 (M)	SO4 (M)	Titanate (M)
36	03/02/92	1.50291	13.490								1.8400	1.7600	9.8900			
36	03/09/90	1.48210	14.100								1.8200	1.5800	10.7000			
36	01/03/90	1.46200	13.240								2.0300	2.0300	9.1800			
36	09/29/89	1.48440	16.560								2.7200	2.3200	11.5200			
36	03/20/89	1.63720	13.510								2.5000	2.0100	9.0000			
36	03/21/88	1.29740	7.164								0.9440	0.7700	5.4500			
36	09/28/87	1.39000	9.960								1.6400	1.2500	7.0700			
36	03/23/87	1.38300	14.980								2.7400	2.2500	9.9900			
36	04/21/86	1.51370	6.750								2.2400	1.5700	2.9400			
36	08/05/83	1.52000	11.590								3.7200	0.8300	7.0400			
36	07/17/82	1.68000	9.100								0.2000	1.9000	7.0000			
36	07/17/82	1.55000	10.800								2.0000	1.8000	7.0000			
36	09/03/81	1.41000	6.300								0.2000	5.7000	0.4000			
36	02/14/81	1.30000	15.900								4.3000	3.3000	8.3000			
36	11/19/80	1.58000	12.700								2.9000	2.3000	7.5000			
36	02/25/80	1.30000	9.340								2.3100	1.4300	5.6000			
37	09/14/01	1.43020	11.463	0.4900	0.0133		0.0183	0.0100	0.0169		1.7726	2.3566	6.6900	0.0202	0.0122	
37	03/12/99	1.47000	11.971	0.4800	0.0170		0.0130	0.0600	0.0130		1.9600	2.2900	7.0000	0.0160	0.0150	
37	06/29/97	1.43000	11.510	0.4800	0.0074		0.0110	0.2800	0.0140		1.5200	2.6800	6.1500	0.0160	0.0200	
37	04/24/96	1.43000	10.502	0.3600	0.0068		0.0100	0.0100	0.0130		1.5000	2.7500	5.7400	0.0140	0.0300	
37	03/27/95	1.41090	12.319	0.5100	0.0068		0.0100	1.4000	0.0130		1.3900	2.5400	4.9200	0.0130	0.0450	
37	03/24/94	1.36100	10.986	0.9900	0.0068		0.0040	0.9800			1.2500	2.7800	3.7700	0.0310	0.0660	
37	03/29/93	1.34650	9.594	0.4700	0.0090		0.0056	0.5400			1.0800	2.9800	3.7700	0.0091	0.0860	
37	03/29/93	1.40000	6.192	0.2100	0.0018		0.0640	0.1400	0.0800		0.7400	1.9600	2.6900	0.0180	0.0560	
37	03/16/92	1.32410	5.660								0.7800	2.3600	2.5200			
37	09/04/91	1.29850	5.860								0.8000	2.7700	2.2900			
37	02/25/91	1.57410	11.520								1.0800	2.0800	8.3600			
37	01/23/91	1.46310	12.130								2.0200	1.6800	8.4300			
37	08/28/90	1.47570	8.990								2.1100	2.0000	4.8800			
37	03/09/90	1.47320	13.780								1.7500	1.4300	10.6000			
37	01/04/90	1.50810	13.930								2.0700	1.7900	10.0700			
37	09/29/89	1.43420	15.950								2.4500	1.9400	11.5600			
37	03/20/89	1.52360	12.800								2.4900	2.0800	8.2300			
37	03/21/88	1.52960	12.387								1.8650	1.2020	9.3200			
37	09/28/87	1.29230	9.360								6.4000	1.4800	1.4800			
37	03/23/87	1.42470	13.690								2.6400	1.9300	9.1200			
37	06/11/86	1.48420	9.662								2.8600	2.0800	4.7220			
37	08/16/83	1.56000	10.730								2.6200	2.0800	6.0300			
37	07/17/82	1.51000	11.600								2.3000	2.4000	6.9000			
37	09/09/81	1.34000	9.600								2.5000	2.3000	4.8000			
37	02/14/81	1.34000	11.500								2.8000	5.7000	3.0000			
37	12/05/80	1.35000	8.200								1.3000	3.2000	3.7000			
37	11/19/80	1.35000	8.200								1.3000	3.2000	3.7000			
37	06/10/80	1.45000	7.400								0.6000	5.1000	1.7000			
37	02/25/80	1.40000	11.250								3.2500	1.9000	6.1000			
38	07/08/01	1.06350	1.738	0.0100	0.0059		0.0029	0.0100	0.0055		0.3415	0.3587	0.9600	0.0055	0.0086	
38	05/16/01	1.17410	3.111	0.1600	0.0090		0.0033	0.1000	0.0050		0.4588	0.5063	1.7100	0.0050	0.0218	
38	02/26/00	1.04920	1.441	0.0500	0.0057		0.0028	0.0600	0.0053		0.2734	0.4571	0.5000	0.0053	0.0052	
38	12/15/00	1.16000	2.495	0.1100	0.0057		0.0031	0.0100	0.0053		0.4395	0.4409	1.4300	0.0053	0.0121	
38	11/30/00	1.09300	1.667	0.0500	0.0058		0.0054	0.0600	0.0054		0.3500	0.3040	0.8000	0.0054	0.0053	
38	08/27/00	1.09000	1.893	0.0100	0.0069		0.0040	0.0100	0.0053		0.3630	0.2997	1.1300	0.0064	0.0072	
38	06/10/00	1.12400	4.935	0.1600	0.0111		0.0044	0.2300	0.0053		0.7810	0.9572	2.3700	0.0072	0.0821	
38	03/21/00	1.13620	1.942	0.1000	0.0068		0.0028	0.0100	0.0053		0.3297	0.3553	1.0900	0.0063	0.0068	
38	12/18/99	1.30220	6.385	0.2800	0.0140		0.0048	0.3600	0.0050		1.1478	1.4762	2.5300	0.0060	0.0947	
38	11/29/99	1.23000	4.118	0.2800	0.0140		0.0033	0.3600	0.0050		0.6500	0.7500	1.5400	0.0060	0.0690	
38	08/25/99	1.42090	11.052	0.2600	0.0150		0.0080	0.2200	0.0130		2.0700	2.1500	5.9800	0.0140	0.0370	
38	03/07/99	1.52000	11.411	0.1200	0.0180		0.0096	0.2400	0.0130		2.1500	2.3200	6.1900	0.0200	0.0250	
38	11/30/98	1.24000	7.124	0.0100	0.0120		0.0057	0.0600	0.0130		1.1200	1.3000	4.4200	0.0270	0.0210	
38	08/30/98	1.39000	10.612	0.1500	0.0068		0.0100	0.2700	0.0130		1.9000	1.7000	6.1800	0.0140	0.0350	
38	05/26/98	1.29000	7.218	0.0300	0.1500		0.0076	0.1700	0.0130		1.2300	1.1700	4.1900	0.0130	0.0240	
38	02/25/98	1.41000	10.218	0.3600	0.0068		0.0120	0.1200	0.0130		1.7700	1.8500	5.8800	0.0200	0.0130	
38	11/01/97	1.30000	8.492	0.2200	0.0068		0.0090	0.2400	0.0130		1.3900	1.3000	5.0000	0.0170	0.0110	
38	08/09/97	1.30000	7.845	0.2700	0.0069		0.0090	0.2000	0.0130		1.2200	1.1800	4.6800	0.0160	0.0093	
38	05/09/97	1.45700	14.959	3.0000	0.0068		0.0140	0.2600	0.0130		2.1800	2.1400	6.9700	0.0270	0.0170	
38	02/25/97	1.42000	12.049	0.2600	0.0068		0.0130	0.3200	0.0130		1.8400	2.1000	7.0600	0.0240	0.0220	
38	10/03/96	1.40100	10.769	0.0100	0.0089		0.0140	0.0100	0.0130		1.8200	1.9000	6.8600	0.0250	0.0240	
38	10/03/96	1.43400	11.222	0.3400			0.0180	0.0100	0.0130		2.0500	1.9800	6.6900	0.0310	0.0088	
38	07/23/96	1.35900	8.976	0.1500	0.0070		0.0140	0.0100	0.0130		1.5000	1.5700	5.5800	0.0200	0.0310	
38	06/20/96	1.29600	7.563	0.1200	0.0074		0.0110	0.4000	0.0053		1.3300	1.2900	3.9100	0.0150	0.0220	
38	02/01/96	1.37500	9.832	0.3000	0.0068		0.0150	0.0100	0.0130		1.7800	1.6100	5.9700	0.0230	0.0240	
38	10/15/95	1.17540	3.768	0.1700	0.0068		0.0069	0.0100	0.0053		0.4900	0.6500	2.3800	0.0093	0.0057	
38	09/07/95	1.16012	3.936	0.1200	0.0068		0.0048	0.1300	0.0100		0.5100	0.6400	2.3500	0.0085	0.0045	
38	07/18/95	1.47490	12.340	0.4300	0.0069		0.0071	0.0100	0.0053		2.4800	2.0800	7.1700	0.0350	0.0180	
38	05/03/95	1.43100	11.528	0.5400	0.0067		0.0180	0.0900	0.0052		2.1900	1.8600	6.6000	0.0300	0.0190	
38	01/26/95	1.13550	10.617	0.3900	0.0066		0.0130	0.0800	0.0130		1.7000	1.5300	6.6900	0.0280	0.0150	

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Tank	Date	Density	Na(M)	AlOH4 (M)	C2O4 (M)	CrO4 (M)	Cl (M)	CO3 (M)	F1 (M)	Formate (M)	NO2 (M)	NO3 (M)	OH (M)	PO4 (M)	SO4 (M)	Titanate (M)
38	03/12/83	1.07000	1.460								0.3800	0.4400	0.6400			
38	02/18/83	1.42000	6.700								0.1500	5.2700	1.2800			
38	09/13/82	1.16000	1.960								0.0600	0.8000	1.1000			
38	06/18/82	1.38000	9.000								1.6000	3.0000	4.4000			
38	05/14/82	1.54000	10.100								2.4000	2.2000	5.5000			
38	05/06/82	1.18000	2.800								0.0500	2.7000	0.0500			
38	01/28/82	1.17000	3.200								0.1000	3.0000	0.1000			
39	07/08/01	1.23610	5.721	0.0100	0.0064		0.0066	0.2700	0.0059		0.6409	1.8006	2.6000	0.0059	0.0464	
39	02/02/01	1.32000	5.506	0.3100	0.0057		0.0089	0.0100	0.0053		0.7210	1.9650	2.3600	0.0053	0.0473	
39	07/30/00	1.30000	6.000	0.3300	0.0069		0.0077	0.0200	0.0053		0.8020	1.7960	2.9100	0.0064	0.0413	
39	02/17/00	1.28000	5.709	0.1500	0.0068		0.0064	0.0100	0.0053		0.7760	1.8570	2.7900	0.0063	0.0392	
39	08/25/99	1.28050	6.413	0.2600	0.0068		0.0065	0.1100	0.0130		0.8700	1.9200	3.0100	0.0063	0.0440	
39	03/07/99	1.28000	5.695	0.1400	0.0068		0.0062	0.0100	0.0130		0.7800	1.6200	3.0100	0.0063	0.0400	
39	09/07/98	1.28000	6.037	0.2600	0.0069		0.0061	0.1100	0.0130		0.8000	1.7300	2.9000	0.0064	0.0410	
39	03/11/98	1.25000	5.789	0.2200	0.0068		0.0065	0.1000	0.0130		0.6300	1.6500	2.9800	0.0063	0.0320	
39	09/17/97	1.22000	6.060	0.1700	0.0068		0.0070	0.2400	0.0053		0.5900	1.6300	3.1000	0.0063	0.0260	
39	04/10/97	1.24600	5.129	0.4510	0.0310		0.0154	0.1370	0.0287	0.0606	0.7040	1.8600	1.5100	0.0287	0.0539	
39	12/02/96	1.38800	6.562	0.4200	0.0068		0.0032	0.0600	0.0053		1.0100	2.9400	1.8700	0.0063	0.0840	
39	06/19/96	1.31000	6.764	0.5400	0.0068		0.0031	0.1400	0.0052		0.9600	2.9000	1.8800	0.0063	0.0850	
39	11/16/95	1.29800	6.807	0.4000	0.0068		0.0064	0.1600	0.0052		0.9300	2.7900	2.1600	0.0063	0.0850	
39	05/09/95	1.25290	7.463	0.4100	0.0067		0.0042	0.2000	0.0052		1.0800	3.4100	1.9800	0.0063	0.0740	
39	11/22/94	1.30290	6.490	0.5100	0.0068		0.0028	0.1100	0.0053		0.8700	2.5900	2.1100	0.0063	0.0780	
39	05/31/94	1.21840	5.928	0.4300	0.0007		0.0007	0.3400	0.0010		0.7200	2.4300	1.6500	0.0006	0.0070	
39	11/21/93	1.29400	8.219	0.8000	0.0047		0.0140	0.8700	0.0130		0.8400	2.5200	2.2600	0.0040	0.0076	
39	11/29/92	1.32210	7.270	0.3200	0.0100		0.0900	0.1200	0.1300		0.9200	3.0600	2.2900	0.0100	0.0900	
39	03/16/92	1.28550	4.690								0.6600	2.0900	1.9400			
39	01/14/92	1.30800	6.520								0.7900	3.2500	2.4800			
39	09/04/91	1.29800	5.860								0.8200	2.8600	2.1800			
39	03/02/91	1.29260	6.740								0.7600	3.2700	2.7100			
39	09/18/90	1.35360	7.000								0.8200	3.1100	3.0700			
39	04/09/90	1.27620	5.900								0.7600	2.9200	2.2200			
39	05/22/89	1.52870	5.010								0.7500	2.7000	1.5600			
39	12/11/88	1.30600	4.920								0.7600	3.3600	0.8000			
39	12/01/87	1.29840	4.480								0.5100	2.2100	1.7600			
39	03/23/87	1.19450	5.380								0.5200	2.8700	1.9900			
39	09/09/86	1.15710	4.220								0.4300	2.9500	0.8400			
39	07/14/86	1.31380	5.120								0.5900	4.4300	0.1000			
39	03/14/86	1.30200	4.294								0.5200	3.0600	0.7140			
39	08/12/85	1.32800	5.218								0.5340	3.7940	0.8900			
39	07/09/85	1.39000	4.340								0.5900	3.7500				
39	08/03/84	1.35000	6.090								1.6300	3.5400	0.9200			
39	02/21/84	1.33000	7.300								0.3600	4.9800	1.9600			
39	08/18/83	1.34000	11.370								0.4900	4.8700	6.0100			
39	02/15/83	1.30000	5.270			0.0200					0.1600	3.4000	1.6900			
39	07/20/82	1.32000	4.400								0.1000	2.8000	1.5000			
39	03/09/82	1.24000	6.100								0.4000	3.7000	2.0000			
40	09/18/01	1.04850	0.097	0.0100	0.0009		0.0003	0.0100	0.0006		0.0271	0.0127	0.0200	0.0005	0.0020	
40	07/22/01	1.02440	1.273	0.0200	0.0115		0.0032	0.0100	0.0091		0.5021	2.704	0.3400	0.0060	0.0394	
40	07/22/01	1.05300	1.261	0.0200	0.0162		0.0032	0.0100	0.0092		0.4880	0.2678	0.3400	0.0059	0.0393	
40	06/14/01	1.06550	1.846	0.0100	0.0263		0.0030	0.0200	0.0133		0.7739	0.3440	0.5100	0.0057	0.0543	
40	07/10/00	1.14000	2.156		0.0240		0.0100	0.0100	0.0150		0.2800	0.6300	1.0000	0.0210	0.0570	
40	07/10/00	1.11000	2.355		0.0270		0.0100	0.0100	0.0150		0.3100	0.7000	1.0800	0.0210	0.0650	
40	04/18/00	1.17000	3.527	0.1800	0.0110		0.0033	0.0100	0.0250		0.5340	1.0000	1.5300	0.0113	0.0950	
40	10/23/99	1.32000	7.866	0.2000	0.0067		0.0100	0.0200	0.0130		1.5600	1.5500	4.3800	0.0100	0.0380	
40	03/29/99	1.36000	9.181	0.2800	0.0068		0.0110	0.1800	0.0130		1.9400	1.6500	4.8100	0.0087	0.0420	
40	09/28/98	1.32000	8.538	0.1500	0.0067		0.0130	0.2900	0.0130		1.7500	1.3500	4.5700	0.0110	0.0360	
40	03/30/98	1.33000	8.611	0.1000	0.0069		0.0110	0.0400	0.0130		1.6400	1.6800	4.9700	0.0093	0.0410	
40	01/01/98	1.35000	7.890	0.2200	0.0061		0.0100	0.3200	0.0110		1.5200	1.5100	3.8400	0.0091	0.0530	
40	06/26/97	1.34000	8.767	0.3000	0.0068		0.0120	0.4200	0.0130		1.6600	1.6800	4.1100	0.0098	0.0580	
40	04/05/96	1.36700	9.522	0.2600	0.0076		0.0130	0.1000	0.0300		1.7300	1.7400	5.5400	0.0190	0.0620	
40	02/26/96	1.18000	2.601		0.0172		0.0428		0.0052		1.0700	0.9920	0.1820	0.0213	0.1140	
40	10/07/95	1.16010	3.511	0.0800	0.0200		0.0022	0.3100	0.0420		1.1700	1.0800	0.2300	0.0022	0.1300	
40	08/23/95	1.15122	2.987	0.0700	0.0210		0.0014	0.1200	0.0390		1.1400	1.1800	0.0700	0.0018	0.1100	
40	05/10/95	1.16770	3.492	0.0900	0.0240		0.0200	0.3000	0.0490		1.2600	1.0700	0.1200	0.0063	0.1200	
40	12/18/94	1.13024	2.671	0.1200	0.0250		0.0070	0.1200	0.0370		0.9900	0.8700	0.1400	0.0160	0.0970	
40	06/29/94	1.15570	3.397	0.1000	0.0250		0.0260	0.2600	0.0470		1.2300	0.9600	0.2500	0.0063	0.1100	
40	01/22/94	1.15810	3.497	0.1100	0.0190		0.0028	0.3000	0.0470		1.2000	1.0200	0.2500	0.0160	0.1000	
40	08/24/93	1.15839	3.487	0.1200	0.0190		0.0028	0.2800	0.0500		1.2300	1.0300	0.2300	0.0084	0.1100	
40	03/01/93	1.18600	3.630	0.0991	0.0190		0.0310	0.3530	0.0670		1.2800	1.0400	0.1592	0.0030	0.1100	
40	12/28/92	1.14000	8.531	0.2600	0.0034		0.0120	0.1800	0.0260		1.6800	1.6700	4.3800	0.0100	0.0550	
40	03/20/89	1.18650	1.850								0.4800	0.9100	0.4600			
40	02/16/89	1.11040	1.300								0.4000	0.8900	0.0100			
40	08/22/88	1.38280	10.080								1.3000	2.2800	6.5000			
40	05/19/87	1.01500	0.216								0.0310	0				

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Tank	Date	Density	Na(M)	AlOH4 (M)	C2O4 (M)	CrO4 (M)	Cl (M)	CO3 (M)	Fl (M)	Formate (M)	NO2 (M)	NO3 (M)	OH (M)	PO4 (M)	SO4 (M)	Titanate (M)
41	04/21/86	1.48620	7.350								1.5600	1.5900	4.2000			
41	08/13/84	1.23000	6.090								1.5800	3.0200	1.4900			
41	02/26/84	1.44000	10.350								1.1700	3.3200	5.8600			
41	08/09/83	1.45000	8.170								2.7300	2.1600	3.2800			
41	04/22/83	1.41000	10.710								0.3800	5.5300	4.8000			
41	04/22/83	1.49000	12.410								0.4300	6.9700	5.0100			
41	04/22/83	1.49000	11.690								0.4200	6.0600	5.2100			
41	03/09/82	1.22000	4.700								0.3000	3.1000	1.3000			
42	08/05/01	1.27450	7.564	0.1900	0.0057		0.0106	0.0100	0.0053		1.5151	1.7093	4.0100	0.0095	0.0346	
42	06/14/01	1.31900	8.096	0.2100	0.0018		0.0126	0.1700	0.0038		1.6500	1.4387	4.3300	0.0103	0.0389	
42	04/16/01	1.32280	7.887	0.2300	0.0016		0.0133	0.1100	0.0043		1.5768	1.4270	4.3000	0.0107	0.0407	
42	03/10/01	1.32200	7.123	0.2700	0.0034		0.0134	0.0400	0.0051		1.5347	1.3975	3.7100	0.0098	0.0398	
42	01/09/01	1.32000	3.625	0.0300	0.0016		0.0102	0.0100	0.0038		1.3820	1.3090	0.7900	0.0010	0.0378	
42	08/09/00	1.32000	7.965	0.2300	0.0034		0.0102	0.1200	0.0026		1.5390	1.4260	4.4100	0.0094	0.0378	
42	02/10/00	1.32750	7.807	0.2200	0.0034		0.0026	0.0600	0.0026		1.5301	1.4552	4.3700	0.0100	0.0367	
42	11/12/99	1.35000	8.317	0.2200	0.0068		0.0100	0.1800	0.0130		1.5200	1.5100	4.5600	0.0110	0.0420	
42	09/09/99	1.30000	7.139		0.0200		0.0060	0.1600	0.0010		1.2200	1.2300	4.2500	0.0100	0.0310	
42	06/08/99	1.00980	0.333	0.0100	0.0015		0.0003	0.0700	0.0017		0.1300	0.0240	0.0100	0.0006	0.0068	
42	05/07/99	1.04800	0.191	0.0100	0.0011		0.0028	0.0200	0.0012		0.0970	0.0180	0.0100	0.0006	0.0046	
42	08/05/98	1.02100	0.467	0.0100	0.0036		0.0005	0.0800	0.0020		0.2200	0.0420	0.0100	0.0006	0.0086	
42	05/27/98	1.01900	0.408	0.0100	0.0035		0.0005	0.0600	0.0019		0.2000	0.0430	0.0100	0.0006	0.0087	
42	01/13/98	1.02000	0.448	0.0030	0.0030		0.0010	0.0670	0.0020		0.2200	0.0500	0.0160	0.0002	0.0090	
42	10/27/97	1.02000	0.470	0.0040	0.0040		0.0010	0.0770	0.0040		0.2100	0.0500	0.0240	0.0002	0.0090	
42	09/23/97	1.02000	0.440	0.0040	0.0040		0.0010	0.0640	0.0030		0.2000	0.0500	0.0310	0.0002	0.0090	
42	08/16/97	1.07500	0.372	0.0100	0.0033		0.0006	0.0700	0.0009		0.1400	0.0440	0.0200	0.0006	0.0057	
42	06/22/97	1.01000	0.259	0.0100	0.0026		0.0005	0.0400	0.0008		0.1000	0.0350	0.0200	0.0006	0.0042	
42	01/01/97	1.03000	0.642	0.0100	0.0076		0.0012	0.0900	0.0020		0.2400	0.0920	0.0700	0.0063	0.0100	
42	07/29/96	1.03900	0.528	0.0100	0.0078		0.0003	0.0600	0.0020		0.2500	0.0970	0.0200	0.0006	0.0097	
42	04/30/96	1.02630	0.527	0.0100	0.0085		0.0004	0.0400	0.0020		0.2400	0.0950	0.0700	0.0006	0.0095	
42	01/05/96	1.02650	0.568	0.0100	0.0083		0.0010	0.0500	0.0037		0.2600	0.1100	0.0500	0.0016	0.0100	
42	11/03/95	1.02220	0.504	0.0100	0.0026		0.0003	0.0700	0.0020		0.2300	0.0600	0.0400	0.0006	0.0085	
42	07/06/95	1.03030	0.545	0.0100	0.0030		0.0007	0.0800	0.0041		0.2400	0.0680	0.0400	0.0006	0.0086	
42	03/07/95	1.02130	0.458	0.0100	0.0034		0.0007	0.0400	0.0026		0.2300	0.0610	0.0500	0.0016	0.0078	
42	12/18/94	1.01960	0.466	0.0100	0.0033		0.0007	0.0500	0.0019		0.2200	0.0600	0.0500	0.0016	0.0078	
42	09/20/94	1.01770	0.422	0.0060	0.0032		0.0007	0.0490	0.0022		0.2200	0.0600	0.0140	0.0008	0.0078	
42	06/15/94	1.03000	0.315								0.2160	0.0510	0.0480			
42	06/15/94	1.02000	0.310								0.2140	0.0500	0.0460			
42	06/10/94	1.01000	0.300								0.1970	0.0560	0.0470			
42	06/10/94	1.01000	0.315								0.2050	0.0600	0.0500			
42	06/04/94	1.02000	0.316								0.2040	0.0590	0.0530			
42	06/04/94	1.01000	0.308								0.2030	0.0590	0.0460			
42	05/18/94	1.08000	0.300								0.1960	0.0490	0.0550			
42	05/18/94	1.06000	0.295								0.1920	0.0480	0.0550			
42	05/15/94	1.04000	0.294								0.1920	0.0400	0.0620			
42	05/15/94	1.03000	0.287								0.1890	0.0430	0.0550			
42	05/16/94	1.09000	0.746								0.4880	0.1570	0.1010			
42	04/18/94	1.04000	0.746								0.4880	0.1570	0.1010			
42	02/19/94	1.04884	1.049	0.0074	0.0051		0.0026	0.1200	0.0063		0.5700	0.1700	0.0110	0.0016	0.0160	
42	11/15/93	1.04680	1.050	0.0200			0.0057	0.1200	0.0057		0.5700	0.1500	0.0230	0.0006	0.0170	
42	06/27/93	1.04733	1.107	0.0090	0.0050		0.0016	0.1300	0.0062		0.5800	0.1800	0.0310	0.0008	0.0160	
42	11/16/92	1.04580	0.810								0.5600	0.1800	0.0700			
42	10/09/92	1.06000	0.820								0.5500	0.2200	0.0500			
42	02/17/92	1.04520	0.890								0.6300	0.1800	0.0800			
42	08/30/91	1.04250	0.760								0.5600	0.1500	0.0500			
42	01/26/91	1.03930	0.780								0.6000	0.1600	0.0200			
42	08/19/90	1.04310	0.750								0.6000	0.1400	0.0100			
42	02/20/90	1.03400	0.610								0.4400	0.1400	0.0300			
42	09/15/89	1.03420	0.610								0.4100	0.1900	0.0100			
42	09/15/89	1.04900	0.620								0.3900	0.2200	0.0100			
42	08/11/89	1.02210	0.410								0.2500	0.1500	0.0100			
42	07/08/89	1.00060	0.010											0.0100		
42	04/24/89	1.01900	0.740								0.4900	0.1800	0.0100		0.0300	
42	10/16/88	0.99700	0.510								0.3100	0.1100	0.0900			
42	06/04/87	1.00400	1.804								0.5900	0.7340	0.4800			
42	04/08/87	1.06000	1.650								0.1400	0.9300	0.5800			
42	12/18/86	1.02240	1.730								0.2300	1.1400	0.3600			
42	07/14/86	1.03370	0.584								0.2900	0.1900	0.1040			
42	02/25/86	1.01000	0.039								0.0360	0.0030				
42	12/29/85	1.00800	0.026								0.0230	0.0029	0.0002			
42	07/17/85	1.01000	0.037								0.0230	0.0015	0.0125			
42	05/22/82	1.11000	2.320								0.6800	1.1400	0.5000			
42	05/05/82	1.10000	2.488	0.0980							0.4800	1.3300	0.5200	0.0300		
42	03/11/82	1.14000	2.230								0.4800	1.2400	0.5100			
43	09/08/01	1.19100	4.763	0.1400	0.0069		0.0034	0.0600	0.0064		0.7500	1.2377	2.4400	0.0064	0.0195	
43	09/08/01	1.22700	5.413	0.1400	0.0064		0.0037	0.0700	0.0060		0.8082	1.4017	2.8100	0.0060	0.0217	
43	09/08/01	1.22300	5.281	0.1000	0.0062		0.0036	0.1000	0.0058		0.8082	1.3187	2.7800	0.0058	0.0206	
43	09/08/01	1.22000	5.315	0.0500	0.0065		0.0035	0.0100	0.0060		0.8651	1.4404	2.8600	0.0062	0.0224</td	

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Tank	Date	Density	Na(M)	AlOH4 (M)	C2O4 (M)	CrO4 (M)	Cl (M)	CO3 (M)	Fl (M)	Formate (M)	NO2 (M)	NO3 (M)	OH (M)	PO4 (M)	SO4 (M)	Titanate (M)	
43	10/04/93	1.31750	9.186	0.4300	0.0068	0.0140	0.5300	0.0130		1.1600	1.6500	4.7300	0.0220	0.0280			
43	07/13/93	1.35090	9.780	0.3800	0.0090	0.0056	0.4600	0.0280		1.3600	1.5400	5.4100	0.0250	0.0260			
43	03/12/93	1.44540	12.718	0.4200	0.0220	0.0140	0.6500	0.0380		1.5000	1.8300	7.4200	0.0440	0.0210			
43	11/24/92	1.43000	14.594	0.4600	0.0050	0.0190				1.8800	1.7300	10.4000	0.0290	0.0064			
43	11/24/92	1.43220	13.560	0.3200			0.6200			1.6000	1.8000	8.6000					
43	06/25/92	1.37050	10.050	0.3600			0.0100			1.3100	1.3800	6.9800					
43	06/20/92	1.37770	13.100	0.0300			0.6200			1.2800	1.8500	8.7000					
43	05/16/92	1.36850	8.810	0.3500			0.0100			1.2300	1.2800	5.9300					
43	03/16/92	1.34080	8.270	0.3300			0.0600			1.0900	1.2100	5.5200					
43	12/26/91	1.32330	7.060	0.1900			0.1200			0.7700	1.2500	4.6100					
43	10/01/91	1.30840	8.010	0.3300			0.1800			0.9500	1.4800	4.8900					
43	08/28/91	1.11360	3.060				0.3400			0.3400	0.7400	1.3000					
43	06/17/91	1.24040	6.140	0.2000			0.5200			0.5400	0.9900	3.3700					
43	05/24/91	1.18200	6.782	0.3070			1.1800			0.4700	0.8700	2.7750					
43	03/08/91	1.08460	3.820							0.2000	0.3400	3.2800					
43	01/23/91	1.07370	0.900							0.1700	0.3000	0.4300					
43	02/28/90	1.16020	3.530							0.3000	0.6700	2.5600					
43	02/16/89	1.42800	9.800							1.4800	1.8200	6.5000					
43	12/11/88	1.29870	7.020							0.9600	1.3500	4.7100					
43	04/05/88	1.18850	5.089							0.4320	1.7500	2.9070					
43	03/07/88	1.15400	3.029							1.4500	1.5300	0.0490					
43	09/28/87	1.11040	4.180							0.4600	1.6400	2.0800					
43	02/24/87	1.22600	6.020							0.5600	2.0900	3.3700					
43	07/14/86	1.33560	5.560							0.7400	2.5100	2.3100					
43	03/14/86	1.36040	5.148							0.7700	2.3200	2.0580					
43	07/09/85	1.25000	2.427			0.0100				0.3900	0.9400	1.0970					
43	06/03/85	1.44100	7.230							1.3900	2.3100	3.5300					
43	01/08/85	1.25000	1.560									1.5600					
43	09/30/84	1.26300	6.106							1.0700	3.6000	1.4360					
43	08/13/84	1.26000	6.120								1.0700	3.6100	1.4400				
43	02/26/84	1.22000	5.250							0.3600	2.4000	2.4900					
43	02/15/83	1.07000	0.750			0.0100				0.0700	0.3500	0.3200					
43	02/15/83	1.07000	0.740							0.0700	0.3500	0.3200					
43	07/29/82	1.17000	3.718	0.3400			0.0340			0.2800	1.2600	1.7700					
43	07/29/82	1.17000	3.400							0.3000	1.3000	1.8000					
43	07/29/82	1.17000	3.310							0.2800	1.2600	1.7700					
43	07/20/82	1.19000	2.800							0.3000	1.5000	1.0000					
43	05/09/82	1.34000	4.600							0.4000	3.0000	1.2000					
43	05/06/82	1.34000	4.600							0.4000	3.0000	1.2000					
44	02/03/99	1.52000	14.844	0.2400	0.0067	0.0170	0.0100	0.0130		1.3100	1.5000	11.6900	0.0120	0.0054			
44	05/01/97	1.50600	14.072	0.0100	0.0067	0.0240	0.0100	0.0130		1.4700	1.3900	11.1000	0.0096	0.0045			
44	04/23/96	1.49000	15.124	0.2800	0.0067	0.0230	0.0600	0.0052		1.4800	1.3200	11.8500	0.0098	0.0047			
44	04/27/95	1.46200	15.235	0.4000	0.0170	0.0140	0.2000	0.0260		1.3300	1.5400	11.4400	0.0160	0.0100			
44	04/18/94	1.46400	13.593	0.2800	0.0090	0.0140	0.3400			1.2600	1.2300	10.0700	0.0087	0.0120			
44	04/12/93	1.41990	13.390							1.2000	1.1500	11.0400					
44	04/06/92	1.49920	11.540							1.1600	1.3300	9.0500					
44	10/30/91	1.43030	17.130							1.5700	3.2300	12.3300					
44	04/12/91	1.43770	16.040							2.0000	1.8700	12.1700					
44	10/04/90	1.48980	17.380							1.6600	1.6800	14.0400					
44	08/08/90	1.53750	7.600							0.8500	1.3700	5.3800					
44	03/21/90	1.31770	15.300							1.7100	2.2900	11.3000					
44	08/15/89	1.62740	9.000							0.9800	1.4000	6.6200					
44	05/15/89	1.36250	11.840							1.6300	1.4900	8.7200					
44	04/21/88	1.57020	14.200							1.7200	2.3400	10.1400					
44	04/03/87	1.11970	5.390							1.0700	2.1900	2.1300					
44	11/25/86	1.21990	7.411							1.2980	2.9730	3.1400					
44	02/09/84	1.44000	8.100							1.9900	1.8100	4.3000					
44	08/23/83	1.48000	12.550							1.2600	2.9100	8.3800					
44	03/18/83	1.55000	13.000							1.8000	2.9000	8.3000					
45	04/12/99	1.49000	16.929	0.2200	0.0087	0.0280	0.2900	0.0130		1.7000	1.2200	13.1100	0.0130	0.0050			
45	05/01/97	1.54200	16.739	0.1000	0.0067	0.0270	0.0100	0.0130		1.5500	1.5700	13.4000	0.0140	0.0050			
45	04/10/96	1.48900	15.881	0.3500	0.0068	0.0300	0.0100	0.0130		1.5400	1.2500	12.6200	0.0140	0.0046			
45	03/26/95	1.50780	18.798	0.3100	0.0067	0.0320	1.2700	0.0052		1.4900	1.2500	13.1100	0.0140	0.0058			
45	02/24/93	1.52190	18.480	0.5700	0.0100	0.0200	0.4100	0.0400		1.5900	1.3700	13.9800	0.0200	0.0100			
45	11/13/92	1.42540	15.800	0.5300			0.4700			1.3900	1.7200	11.2200					
45	08/14/92	1.54820	19.220	0.7200			0.9600			1.7000	1.6700	13.2100					
45	05/19/92	1.54650	16.430	0.5700			0.2700			1.3700	1.2600	12.6900					
45	05/19/92	1.52200	0.000														
45	02/26/92	1.47090	13.860							1.2900	1.2600	11.3100					
45	02/26/92	1.45600	0.000														
45	01/17/92	1.52130	15.890							1.5100	1.6700	12.7100					
45	11/13/91	1.50000	13.830							1.4400	1.7200	10.6700					
45	10/30/91	1.48690	12.840							1.3900	1.5700	9.8800					
45	09/15/91	1.48680	15.850							1.5300	1.4700	12.8500					
45	08/09/91	1.54470	17.680							1.9100	2.0200	13.7500					
45	07/01/91	1.29430	9.470	0.3400						0.8200	1.6200	6.6900					
45	05/24/91	1.40000	13.240							1.2200	1.8700	10.1500					
45	04/12/91	1.32120	14.390							1.3700	1.5000	11.5200					
45	10/12/90	1.42880	17.470							1.5100	2.1600	13.8000					
45	03/21/90	1.47800	14.240							1.5800	1.4900	11.1700					
45	11/17/89	1.44580	13.280							1.1100	1.0500	11.1200					
45	05/15/89	1.40990	12.390							1.5200	1.3300	9.5400					
45	11/04/88	1.16750	5.120							0.4200	1.2800	3.4200					
45	04/21/88	1.36430	7.260														

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Tank	Date	Density	Na(M)	AlOH4 (M)	C2O4 (M)	CrO4 (M)	Cl (M)	CO3 (M)	Fl (M)	Formate (M)	NO2 (M)	NO3 (M)	OH (M)	PO4 (M)	SO4 (M)	Titanate (M)	
46	01/13/97	1.41000	11.785	0.4200	0.0072	0.0160	0.1600	0.0130			1.0600	3.0600	6.8000	0.0096	0.0300		
46	08/01/96	1.43300	11.788	0.1800	0.0068	0.0220	0.0100	0.0130			1.1800	2.8400	7.4600	0.0100	0.0180		
46	04/25/96	1.44800	11.156	0.4300	0.0068	0.0220	0.0400	0.0130			1.0900	3.2400	6.2000	0.0099	0.0220		
46	11/21/95	1.39170	10.772	0.3900	0.0060	0.0220	0.0800	0.0130			0.9700	3.7500	5.3500	0.0063	0.0460		
46	08/18/95	1.41974	10.898	0.3900	0.0068	0.0180	0.2300	0.0130			0.9300	3.4300	5.4800	0.0100	0.0700		
46	05/11/95	1.41440	9.750	0.3200	0.0068	0.0038	0.2300	0.0160			0.5800	3.0400	4.9700	0.0630	0.0820		
46	03/06/95	1.37620	10.094	0.2400	0.0068	0.0190	0.1800	0.0260			0.8300	3.1800	5.2500	0.0074	0.0800		
46	11/23/94	1.37800	9.075	0.2900	0.0068	0.0530	0.1400	0.0053			0.7500	3.0600	4.3700	0.0066	0.1200		
46	08/20/94	1.43860	10.955	0.3000	0.0068	0.0140	0.2400	0.0260			0.9400	3.3100	5.7300		0.0740		
46	05/13/94	1.05354	12.546	0.3600	0.0068	0.0070	0.1100	0.0130			1.1200	1.8200	8.9300	0.0110	0.0180		
47	01/13/98	1.32000	7.834	0.4000	0.0068	0.0077	0.2800	0.0130			0.6200	2.3700	3.7600	0.0063	0.0390		
47	01/13/97	1.33700	7.749	0.3300	0.0067	0.0100	0.2000	0.0052			0.6400	2.2800	3.9600	0.0110	0.0420		
47	05/22/96	1.31100	8.994	0.0300	0.0068	0.0130	0.5000	0.0130			0.6600	2.6500	4.5300	0.0130	0.0260		
47	10/19/95	1.31770	7.782	0.3600	0.0068	0.0150	0.2600	0.0053			0.6200	2.1000	4.0400	0.0110	0.0410		
47	07/18/95	1.30990	6.657	0.3000	0.0068	0.0150	0.1000	0.0260			0.6800	2.1500	3.7700	0.0110	0.0380		
47	04/27/95	1.33800	9.512	0.3500	0.0068	0.0120	0.3300	0.0053			0.8500	2.4000	4.9900	0.0220	0.0860		
47	01/20/95	1.36020	9.838	0.3800	0.0060	0.0160	0.1400	0.0130			0.8000	2.4100	5.0800	0.0110	0.4100		
47	10/06/94	1.10890	7.732	0.4900	0.0063	0.0390	0.4500	0.0240			0.7200	2.0300	3.4200	0.0130	0.0320		
47	11/13/91	1.36420	8.510									0.8700	1.5100	6.1300			
47	05/24/91	1.51600	16.910									1.5300	1.5000	13.8800			
47	12/06/90	1.46250	13.000									1.7300	1.6200	9.6500			
47	05/24/90	1.45140	12.930									1.9800	1.8100	9.1400			
47	01/24/90	1.37420	12.090									1.3500	1.2000	9.5400			
47	05/15/89	1.48260	13.210									1.8300	1.4400	9.9400			
47	11/04/88	1.42810	12.380									1.4900	1.4700	9.4200			
47	04/21/88	1.48940	14.354									1.4300	2.2500	10.6740			
47	11/25/86	1.39370	8.950									1.8800	1.7000	5.3700			
47	04/04/86	1.47330	7.740									1.4100	1.6600	4.6700			
47	08/19/85	1.41700	6.210									1.0500	2.6000	2.5600			
47	03/19/85	1.29000	4.436									0.3600	2.6500	1.4260			
47	10/20/84	1.35000	6.764									1.5040	3.4310	1.8290			
47	07/12/83	1.51000	9.580									1.9700	2.5900	5.0200			
47	01/14/83	1.18000	3.290									0.0900	1.9000	1.3000			
47	07/22/82	1.19000	3.800									0.1000	1.5000	2.2000			
47	05/09/82	1.34000	4.800									0.2000	2.0000	2.6000			
47	01/08/82	1.25000	3.600									0.2000	1.5000	1.9000			
47	10/16/81	1.30000	4.800									0.3000	2.1000	2.4000			
47	07/02/81	1.24000	4.100									0.1000	2.8000	1.2000			
47	07/02/81	1.46000	5.600									2.7000	1.9000	1.0000			
47	07/02/81	1.42000	11.622					0.0410				2.5400	2.9000	6.1000			
48	05/10/01	1.14410	2.824	0.0800	0.0110	0.0153	0.3600	0.0007			0.5344	0.2518	1.1900	0.0049	0.0031		
48	12/08/00	1.13700	2.933	0.0800	0.0109	0.0053	0.4000	0.0053			0.5310	0.2740	1.2600	0.0065	0.0034		
48	07/25/00	1.13000	2.641	0.1100	0.0108	0.0057	0.3300	0.0053			0.5600	0.2820	0.9800	0.0063	0.0042		
48	02/18/97	1.12100	2.871	0.2250	0.0059	0.0006	0.2250	0.0011	0.0022	0.4500	0.3110	1.4000	0.0062	0.0031			
48	08/30/96	1.12600	2.678	0.1200			0.1840				0.4200	0.3500	1.4200				
48	08/30/96	1.12400	2.729	0.1070			0.1810				0.4500	0.3500	1.4600				
48	03/21/95	1.21690	5.044	0.1400	0.0110	0.0100	0.1800	0.0053			0.8300	0.7400	2.9000	0.0120	0.0056		
48	11/03/94	1.07790	1.452	0.0300	0.0200	0.0038	0.3300				0.3000	0.1700	0.2400	0.0064	0.0045		
48	06/18/94	1.05314	1.427	0.0600	0.0018	0.0110	0.3000	0.0015			0.3700	0.1400	0.2300	0.0016	0.0038		
48	02/02/94	1.05590	1.292	0.0500	0.0170	0.0027	0.2900				0.3600	0.1100	0.1600	0.0016	0.0037		
48	09/24/93	1.04450	1.063	0.0600	0.0170	0.0027	0.2600	0.0018			0.1700	0.1000	0.1800	0.0016	0.0034		
48	08/25/93	1.03887	0.917	0.0410	0.0170	0.0036	0.2400	0.0026			0.1100	0.1000	0.1500	0.0021	0.0032		
48	04/18/93	1.05980	1.148	0.0320	0.0140	0.0036	0.2800	0.0040			0.2100	0.0790	0.2300	0.0021	0.0047		
48	12/16/92	1.09110	1.990	0.0100	0.0100	0.0100	0.6200	0.0100			0.3300	0.1400	0.1900	0.0100	0.0100		
48	08/28/92	1.07300	0.490									0.2700	0.0900	0.1300			
48	03/13/92	1.06410	0.400									0.0900	0.0300	0.2800			
48	11/19/91	1.05960	0.460									0.0500	0.0300	0.3800			
48	08/24/91	1.09500	2.120									0.1200	0.0200	0.1900			
48	04/17/91	1.05440	0.570									0.0300	0.0800	0.4600			
48	01/26/91	1.05420	0.661									0.0870	0.0350	0.5390			
48	08/19/90	1.04310	0.750									0.6000	0.1400	0.0100			
48	05/26/90	1.22770	0.760									0.5200	0.1300	0.1100			
48	02/12/90	1.15850	0.741									0.4260	0.0750	0.2400			
48	11/30/89	1.14050	0.936									0.3200	0.1160	0.5000			
48	08/21/89	1.12110	0.891									0.3000	0.0810	0.5100			
48	12/11/88	1.10200	0.560									0.3900	0.1600	0.0100			
48	06/04/87	1.12090	0.349									0.2420	0.0070	0.1000			
48	09/09/86	0.99140	0.420									0.2800	0.1200	0.0200			
48	01/08/86	1.05500	1.298				0.2890					0.2400	0.0880	0.3740	0.0090		
48	05/14/85	1.05000	0.730									0.1800	0.0800	0.4700			
49	07/09/01	1.11030	1.220	0.0100	0.0044	0.0008	0.1100	0.0026			0.5904	0.3071	0.0300	0.0060	0.0182		
49	05/27/01	1.10430	1.209	0.0100	0.0048	0.0008	0.1000	0.0005			0.6017	0.3263	0.0300	0.0006	0.0167		
49	04/15/01	1.10700	2.066	0.0100	0.0048	0.0008	0.5400	0.0005			0.5880	0.3200	0.0200	0.0006	0.0198		
49	09/11/00	1.22100	4.630	0.0100	0.0105	0.0014	1.2700	0.0005			1.1900	0.7700	0.0200	0.0014	0.0419		
49	01/30/00	1.20940	5.417	0.0400	0.0034	0.0017	0.7300	0.0026			1.7300	1.7300	0.4400</				

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Tank	Date	Density	Na(M)	AlOH4 (M)	C2O4 (M)	CrO4 (M)	Cl (M)	CO3 (M)	Fl (M)	Formate (M)	NO2 (M)	NO3 (M)	OH (M)	PO4 (M)	SO4 (M)	Titanate (M)
50	06/25/99	1.23890	5.180	0.0300	0.0080	0.0400	0.0900	0.0053		0.0580	2.8400	1.9400	0.0063	0.0300		
50	09/02/97	1.25100	5.766	0.1210	0.0150	0.0270	0.1240	0.0010		0.2000	3.0200	2.0600	0.0100	0.0220		
50	09/01/97	1.27000	5.429	0.1100	0.0100	0.0180	0.1200	0.0010		0.2000	2.8700	1.9100	0.0100	0.0200		
50	08/01/97	1.25300	5.486	0.1100	0.0080	0.0190	0.1300	0.0010		0.2300	2.9500	1.8500	0.0040	0.0230		
50	07/01/97	1.26000	5.366	0.1300	0.0120	0.0140	0.1800	0.0010		0.1800	2.7500	1.8700	0.0030	0.0200		
50	06/11/97	1.25300	5.148	0.1500	0.0010	0.0170	0.1100	0.0010		0.2100	2.7000	1.8000	0.0030	0.0200		
50	05/01/97	1.28500	5.209	0.1700	0.0140	0.0190	0.1250	0.0010		0.2100	2.7300	1.7700	0.0030	0.0180		
50	04/24/97	1.27600	5.415	0.1360	0.0090	0.0170	0.1340	0.0100		0.2350	2.8100	1.8800	0.0040	0.0190		
50	02/01/97	1.24000	5.060	0.1300	0.0150	0.0130	0.1300	0.0100		0.2700	2.4300	1.8900	0.0040	0.0150		
50	02/01/97	1.26400	5.030	0.2000	0.0100	0.0130	0.1000	0.0010		0.3000	2.7400	1.5000	0.0100	0.0180		
50	01/19/97	1.26000	5.215	0.1200	0.0080	0.0140	0.1400	0.0010		0.2300	2.4000	2.1100	0.0040	0.0200		
50	12/01/96	1.23500	5.093	0.1190	0.0110	0.0190	0.1620	0.0010		0.2700	2.4800	1.8300	0.0010	0.0180		
50	11/30/96	1.24000	4.847	0.1190	0.0110	0.0160	0.1160	0.0001		0.2700	2.2700	1.8900	0.0010	0.0180		
50	10/30/96	1.26700	4.957	0.1320	0.0100	0.0170	0.1640	0.0100		0.2600	2.2700	1.8700	0.0100	0.0150		
50	10/24/96	1.26000	5.124	0.1400	0.0010	0.0200	0.1900	0.0100		0.3300	2.3500	1.8500	0.0010	0.0200		
50	10/06/96	1.24800	4.951	0.1400	0.0010	0.0170	0.1700	0.0100		0.2700	2.2400	1.8900	0.0010	0.0200		
50	09/24/96	1.24400	5.052	0.1600	0.0010	0.0180	0.1400	0.0100		0.3100	2.4200	1.8100	0.0010	0.0200		
50	08/13/96	1.25000	5.631	0.1230	0.0080	0.0200	0.1600	0.0300		0.3500	2.6900	2.0200	0.0100	0.0200		
50	07/29/96	1.24000	5.233	0.1500	0.0100	0.0360	0.1700	0.0110		0.3400	2.4900	1.8100	0.0020	0.0200		
50	06/02/96	1.24000	5.172	0.1280	0.0010	0.0200	0.1650	0.0100		0.3200	2.4200	1.9000	0.0010	0.0200		
50	05/16/96	1.24000	5.227	0.0880	0.0010	0.0050	0.2100	0.0200		0.3500	2.3300	1.9700	0.0010	0.0200		
50	05/06/96	1.24000	5.120	0.0990	0.0100	0.0200	0.1840	0.0100		0.3600	2.1900	2.0500	0.0010	0.0050		
50	05/04/96	1.24000	4.054	0.0950	0.0100	0.0200	0.1630	0.0400		0.3700	2.1500	1.0000	0.0010	0.0200		
50	04/04/96	1.24000	5.467	0.1100	0.0009	0.0190	0.1600	0.0100		0.3800	2.4900	2.0900	0.0010	0.0220		
50	03/19/96	1.26000	4.925	0.0700	0.0080	0.0180	0.1700	0.0300		0.3000	2.0400	2.0700	0.0030	0.0200		
50	02/20/96	1.26000	5.246	0.1180	0.0040	0.0200	0.1660	0.0400		0.3300	2.2200	2.1300	0.0040	0.0200		
50	02/01/96	1.24000	4.245	0.1250	0.0060	0.0100	0.2600	0.0010		0.3300	1.1100	2.1000	0.0010	0.0200		
50	01/16/96	1.24000	5.389	0.1300	0.0070	0.0180	0.1600	0.0090		0.4000	2.3700	2.0800	0.0050	0.0200		
50	01/03/96	1.23500	4.965	0.1200	0.0100	0.0200	0.2300	0.0100		0.3800	1.8200	2.0900	0.0050	0.0200		
50	12/20/95	1.22800	4.950	0.1300	0.0100	0.0180	0.2000	0.0100		0.3900	1.8200	2.1200	0.0040	0.0200		
50	12/01/95	1.22600	5.059	0.1400	0.0070	0.0190	0.1700	0.0300		0.4000	1.8900	2.1800	0.0050	0.0190		
50	11/08/95	1.22500	5.227	0.1160	0.0100	0.0100	0.1700	0.0100		0.2900	2.3500	2.0400	0.0050	0.0230		
50	10/05/95	1.26000	5.283	0.1110	0.0080	0.0180	0.1130	0.0200		0.0500	3.2000	1.5600	0.0100	0.0300		
50	09/02/95	1.25500	5.292	0.1020	0.0100	0.0200	0.1500	0.0200		0.0500	3.1300	1.5700	0.0100	0.0300		
50	08/02/95	1.28000	5.366	0.1100		0.0200	0.1130	0.0100		0.0600	3.3500	1.5300	0.0300			
50	07/10/95	1.26000	4.999	0.1100		0.0150	0.1100	0.0100		0.0500	2.9600	1.5700	0.0320			
50	06/01/95	1.26000	10.550	0.1000	0.0200	2.7600	0.0200	0.0200		0.0600	3.2900	1.3900	0.0100	0.0300		
50	05/18/95	1.26000	5.250	0.0900	0.0100	0.0200	0.1300	0.0400		0.0600	3.1000	1.5800	0.0100	0.0300		
50	04/23/95	1.25600	5.372	0.1030	0.0140	0.0260	0.1650	0.0100		0.0650	3.2300	1.4800	0.0100	0.0420		
50	11/04/91	1.23750	4.770					0.3200		0.2400	2.6500	1.3300				
50	04/17/91	1.23540	4.544					0.3600		0.2500	2.7200	1.3400		0.1600		
50	08/23/89	1.27940	4.480							0.0240	3.1000	1.4200				
50	12/01/88	1.31970	5.970							0.1900	3.0200	1.2700				
50	10/26/88	1.25420	5.110	0.2500				0.3200		0.2400	2.6500	1.3300				
50	10/11/88	1.25770	5.630	0.2800				0.3600		0.2500	2.7200	1.3400				
50	12/01/87	1.04000	0.145							0.0100	0.0400	0.0950				
50	06/04/87	0.97680	3.544							0.2230	2.1010	1.2200				
50	01/01/87	1.12900	4.190							0.4400	2.1700	1.5800				
50	06/11/86	1.28050	4.648							0.3900	3.3700	0.8880				
50	04/25/86	1.25260	2.820							0.2100	1.9400	0.6700				
50	02/24/86	1.24680	3.220							0.2500	2.4700	0.5600				
50	02/24/86	1.23000	3.460							0.2600	2.6000	0.6000				
50	02/24/86	1.23000	3.530							0.2800	2.6600	0.5900				
50	01/06/86	1.19620	3.710							0.3100	2.8600	0.5400				
50	11/26/85	1.22000	4.452							0.3880	3.5500	0.5140				
51	09/25/01	1.01600	0.296	0.0100	0.0041		0.0003	0.0500	0.0016		0.1393	0.0280	0.0000	0.0005	0.0058	
51	06/19/01	1.01680	0.345	0.0100	0.0042		0.0004	0.0600	0.0017		0.1567	0.0288	0.0100	0.0005	0.0060	
51	04/04/01	1.10560	0.215		0.0043		0.0004		0.0018		0.1630	0.0319		0.0003	0.0064	
51	12/08/00	1.11740	0.243	0.0100	0.0050		0.0011	0.0100	0.0021		0.1380	0.0310	0.0200	0.0005	0.0069	
51	05/09/00	1.05000	0.455	0.0100	0.0049		0.0004	0.0800	0.0020		0.1620	0.0393	0.0600	0.0006	0.0071	
51	01/04/00	1.12000	0.309	0.0100	0.0052		0.0003	0.0100	0.0023		0.1700	0.0440	0.0400	0.0006	0.0078	
51	05/18/99	1.09600	0.455	0.0100	0.0050		0.0016	0.0800	0.0026		0.1700	0.0400	0.0400	0.0032	0.0081	
51	03/16/99	1.01700	0.474	0.0100	0.0055		0.0004	0.0500	0.0024		0.2600	0.0560	0.0200	0.0006	0.0087	
51	10/09/98	1.03000	0.443	0.0050	0.0050		0.0020	0.0540	0.0020		0.2100	0.0610	0.0360	0.0007		
51	10/10/98	1.05000	0.691	0.0150	0.0120		0.0003	0.0490	0.0040		0.2900	0.1400	0.1100	0.0110		
51	10/11/98	1.03000	0.600	0.0160	0.0110		0.0010	0.0410	0.0040		0.2000	0.1500	0.1200	0.0080		
51	08/07/97	1.10600	0.690	0.0200	0.0130		0.0007	0.0800	0.0024		0.2400	0.1300	0.1000	0.0006	0.0110	
51	06/03/97	1.17900	0.673	0.0300	0.0150		0.0004	0.0600	0.0037		0.2500	0.1300	0.1000	0.0006	0.0110	
51	04/10/97	1.03000	0.596	0.0170	0.0120		0.0010	-	0.0020		0.3000	0.1400	0.1000	0.0120		
51	10/10/96	1.06000	0													

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APPENDIX B

MODIFICATIONS TO GEOCHEMIST'S WORKBENCH FOR NAS_{gel}

The Geochemist's Workbench (GWB) software package uses equilibrium constants to calculate mineral saturation. For the previous evaporator reports,^{3,4,5} the equilibrium constants used for sodium aluminosilicate gel (NAS_{gel}), the precursor for undesirable minerals in the SRS evaporators, were based on an extrapolation of solubility data in nominally 4 M sodium solutions at temperatures of 30 and 50°C.⁶ To better model the solubility of NAS_{gel} at SRS evaporator sodium concentrations (nominally 8.5 M), Jonas Adai-Mensah of the University of South Australia measured NAS_{gel} solubility at a variety of solution conditions and temperatures.⁸ These results were then used to calculate equilibrium constants for input into the GWB database. An outline of the methodology follows.

1. Add data for NAS_{gel} to the thermodynamic database. Data includes the molecular weight, molecular formula, decomposition reaction using GWB basis species, and the log of the decomposition reaction equilibrium constant (K) at 0, 25, 60, 100, 150, 200, 250, and 300°C. At this step all log K values are set to zero.
2. Run the React.exe module of GWB with the experimentally determined solution compositions and temperatures to calculate log K for each solution and temperature².
3. Fit a model of the calculated log K values as a function of solution composition and temperature.
4. Using the model, calculate log K for the composition 8.5 m Na^+ , 3 m $\text{NO}_2^- + \text{NO}_3^-$, and 0.2 m $\text{Al}(\text{OH})_4^-$ at the following temperatures: 0, 25, 60, 100, 150, 200, 250, and 300°C.
5. Enter the calculated log K values in the database

The molecular formula for NAS_{gel} , as determined by Mensah, is given in Equation B-1. This equation also shows the decomposition of NAS_{gel} in terms of GWB basis species³.



In the Mensah experiments, NAS_{gel} was dissolved in solutions of known compositions and known temperatures (see Table B-1). When the decomposition reaction was at equilibrium⁴, silicon and aluminum concentrations were measured. Based on the starting solution composition and the measured silicon and aluminum concentrations, the equilibrium solution compositions were calculated as follows:

² At saturation, $\log Q/K=0$ ($\log Q = \log K$). With $\log K$ set to zero, at saturation, the reaction quotient, Q, as calculated by React.exe is equal to K or $\log Q = \log K$.

³ The actual species that are involved in the reaction (e.g., $\text{Al}(\text{OH})_4^-$) are swapped for basis species when running components of GWB.

⁴ Solutions were periodically sampled and analyzed to determine when equilibrium was reached (see Ref 8 for details).

- (Na^+) was increased based on the measured silicon concentration, since, per Equation B-1, for each mole of silicon formed, one mole of Na^+ is formed.
- Silicon is assumed to be in the form $\text{H}_2\text{SiO}_4^{2-}$.
- Aluminum is assumed to be in the form Al(OH)_4^-
- Hydroxide is calculated from a charge balance:

$$(\text{OH}^-) = (\text{Na}^+) - (\text{NO}_3^-) - (\text{NO}_2^-) - (\text{Al(OH)}_4^-) - 2 \cdot (\text{H}_2\text{SiO}_4^{2-})$$

The calculated equilibrium solution compositions are given in Table B-2.

Table B-6. Initial Solution Composition and Equilibrium Aluminum and Silicon Compositions for NAS_{gel} Solubility Experiments

Solution ID	Initial Solution Composition					Equilibrium Solubility	
	(Na^+)	(OH^-)	(NO_3^-)	(NO_2^-)	(Al(III))	(Si)	(Al)
$T = 30^\circ\text{C}$							
NAS-1	3	3	0	0	0	0.0702	0.0791
NAS-2	6	6	0	0	0	0.1013	0.0989
NAS-3	6	4	1	1	0	0.0861	0.0791
NAS-4	6	4	1	1	0.15	0.0558	0.1941
NAS-5	6	4	1	1	0.45	0.0398	0.4703
NAS-6	12	8	2	2	0	0.1088	0.1091
NAS-7	12	8	2	2	0.15	0.0852	0.2201
NAS-8	12	8	2	2	0.45	0.0564	0.5104
$T = 65^\circ\text{C}$							
NAS-9	3	3	0	0	0	0.0881	0.1049
NAS-10	6	6	0	0	0	0.2074	0.2061
NAS-11	6	4	1	1	0	0.1163	0.125
NAS-12	6	4	1	1	0.15	0.0705	0.2052
NAS-13	6	4	1	1	0.45	0.0454	0.5083
NAS-14	12	8	2	2	0	0.2578	0.2842
NAS-15	12	8	2	2	0.15	0.1937	0.3508
NAS-16	12	8	2	2	0.45	0.1447	0.5796
$T = 130^\circ\text{C}$							
NAS-17	3	3	0	0	0	0.1119	0.1132
NAS-18	6	6	0	0	0	0.2934	0.2952
NAS-19	6	4	1	1	0	0.1565	0.1589
NAS-20	6	4	1	1	0.15	0.0892	0.2282
NAS-21	6	4	1	1	0.45	0.0576	0.5108

Table B-7. Molar NAS_{gel} Equilibrium Compositions

Solution ID	(Na^+)	(OH^-)	(NO_3^-)	(NO_2^-)	$(\text{H}_2\text{SiO}_4^{2-})$	$(\text{Al(OH})_4^-)$
$T = 30^\circ\text{C}$						
NAS-1	3.0702	2.8507	0	0	0.0702	0.0791
NAS-2	6.1013	5.7998	0	0	0.1013	0.0989
NAS-3	6.0861	3.8348	1	1	0.0861	0.0791
NAS-4	6.0558	3.7501	1	1	0.0558	0.1941
NAS-5	6.0398	3.4899	1	1	0.0398	0.4703
NAS-6	12.1088	7.7821	2	2	0.1088	0.1091
NAS-7	12.0852	7.6947	2	2	0.0852	0.2201
NAS-8	12.0564	7.4332	2	2	0.0564	0.5104
$T = 65^\circ\text{C}$						
NAS-9	3.0881	2.807	0	0	0.0881	0.1049
NAS-10	6.2074	5.5865	0	0	0.2074	0.2061
NAS-11	6.1163	3.7587	1	1	0.1163	0.125
NAS-12	6.0705	3.7243	1	1	0.0705	0.2052
NAS-13	6.0454	3.4463	1	1	0.0454	0.5083
NAS-14	12.2578	7.458	2	2	0.2578	0.2842
NAS-15	12.1937	7.4555	2	2	0.1937	0.3508
NAS-16	12.1447	7.2757	2	2	0.1447	0.5796
$T = 130^\circ\text{C}$						
NAS-17	3.1119	2.7749	0	0	0.1119	0.1132
NAS-18	6.2934	5.4114	0	0	0.2934	0.2952
NAS-19	6.1565	3.6846	1	1	0.1565	0.1589
NAS-20	6.0892	3.6826	1	1	0.0892	0.2282
NAS-21	6.0576	3.4316	1	1	0.0576	0.5108

For input into React.exe of GWB, the molarities must now be converted to molalities.

$$[X] = (X) \cdot \left(\frac{1}{\text{density} - \text{solute mass}} \right) \quad \text{B-2}$$

where

$[X]$ = molality of component X

(X) = molarity of component X

density = solution density in kg/L

solute mass = mass in kg of solute in 1 L of solution

The density is calculated from Equation B-3. The derivation of this correlation can be found in Appendix A of this document.

$$\text{density} = 1.013 + 5.701 \cdot 10^{-2} \cdot (Na^+) - 1.725 \cdot 10^{-3} \cdot (Na^+)^2 \quad \text{B-3}$$

$$solute\ mass = \frac{1}{1000} \sum (X_i) MW_i$$

B-4

Table B-3 shows the results of the conversion of equilibrium molar concentrations to equilibrium molal concentrations.

The compositions and temperatures given in Table B-3 were input into React.exe of GWB. The calculated log K values are given in Table B-4.

Table B-8. Calculated Solution Density, Solute Mass, and Composition in Molality for NAS_{gel} Equilibrium Solutions

Solution ID	Solution Density (kg/L)	Solute Mass (kg/L)	$[Na^+]$	$[OH^-]$	$[NO_2^- + NO_3^-]$	$[H_2SiO_4^{2-}]$	$[Al(OH)_4^-]$
$T = 30^\circ C$							
NAS-1	1.117	0.133	3.121	2.898	0.000	0.0714	0.0804
NAS-2	1.219	0.258	6.350	6.036	0.000	0.1054	0.1029
NAS-3	1.246	0.329	6.634	4.180	2.180	0.0939	0.0862
NAS-4	1.246	0.335	6.646	4.115	2.195	0.0612	0.2130
NAS-5	1.249	0.355	6.754	3.903	2.236	0.0445	0.5259
NAS-6	1.476	0.647	14.618	9.395	4.829	0.1313	0.1317
NAS-7	1.476	0.654	14.699	9.359	4.865	0.1036	0.2677
NAS-8	1.478	0.673	14.981	9.236	4.970	0.0701	0.6342
$T = 65^\circ C$							
NAS-9	1.118	0.137	3.146	2.860	0.000	0.0898	0.1069
NAS-10	1.227	0.277	6.534	5.880	0.000	0.2183	0.2169
NAS-11	1.249	0.335	6.697	4.115	2.190	0.1273	0.1369
NAS-12	1.247	0.337	6.671	4.093	2.198	0.0775	0.2255
NAS-13	1.250	0.358	6.780	3.865	2.243	0.0509	0.5701
NAS-14	1.487	0.676	15.105	9.190	4.929	0.3177	0.3502
NAS-15	1.484	0.675	15.059	9.208	4.940	0.2392	0.4332
NAS-16	1.485	0.688	15.238	9.129	5.019	0.1816	0.7272
$T = 130^\circ C$							
NAS-17	1.120	0.140	3.175	2.831	0.000	0.1142	0.1155
NAS-18	1.233	0.292	6.688	5.750	0.000	0.3118	0.3137
NAS-19	1.252	0.342	6.768	4.051	2.199	0.1720	0.1747
NAS-20	1.249	0.341	6.708	4.057	2.203	0.0983	0.2514
NAS-21	1.251	0.360	6.799	3.851	2.245	0.0646	0.5733

Table B-9. Calculated log K Values for NAS gel Solutions

Solution ID	log K
NAS-1	157.7136
NAS-2	158.0517
NAS-3	161.6694
NAS-4	164.4053
NAS-5	168.2868
NAS-6	164.4158
NAS-7	167.0295
NAS-8	169.9796
NAS-9	135.4874
NAS-10	141.3506
NAS-11	140.6694
NAS-12	140.7778
NAS-13	144.2983
NAS-14	149.3309
NAS-15	148.9351
NAS-16	150.5189
NAS-17	114.779
NAS-18	122.9535
NAS-19	120.7002
NAS-20	119.6384
NAS-21	122.5377

The statistical software JMP[®] was used to fit a model of log K as a function of [Na⁺], [Al(OH)₄⁻], and the inverse of the temperature in Kelvin.

Sodium was chosen because it is the major component of the solutions. Aluminate was chosen because, when added to a starting solution, it had a major impact on solubility. The inverse temperature was chosen because the log of an equilibrium constant is typically proportional to the inverse temperature. Nitrate and nitrite were not used because they had little direct impact on solubility. Hydroxide was not chosen because it is calculated from a charge balance, and highly correlated to the sodium concentration.

The resulting model is given in the following equation.

$$\log K = 9.125 \cdot \log[Na^+] + 7.003 \cdot \log[Al(OH)_4^-] + \frac{5.277 \cdot 10^4}{T} - 14.54 \quad B-5$$

$R^2 = 0.99$

Using the above model (Equation B-5), log K values were calculated at 8.5 m Na⁺, 0.2 m Al(OH)₄⁻, and the following temperatures: 0, 25, 60, 100, 150, 200, 250, and 300°C. Table B-4 lists the log K values calculated using Equation B-5. These values were then input into the GWB thermodynamic database.

Table B-10. NAS_{gel} log K Values for Input into GWB Thermodynamic Database

Temperature (°C)	log K
0	182.3431
25	166.1269
60	147.5148
100	130.5209
150	113.7981
200	100.6108
250	89.9449
300	81.1405

Figure B-1 shows a comparison between the log K values derived from Ejaz solubility data (see Evaporator Report Part I)³ and values derived from the Mensah data.

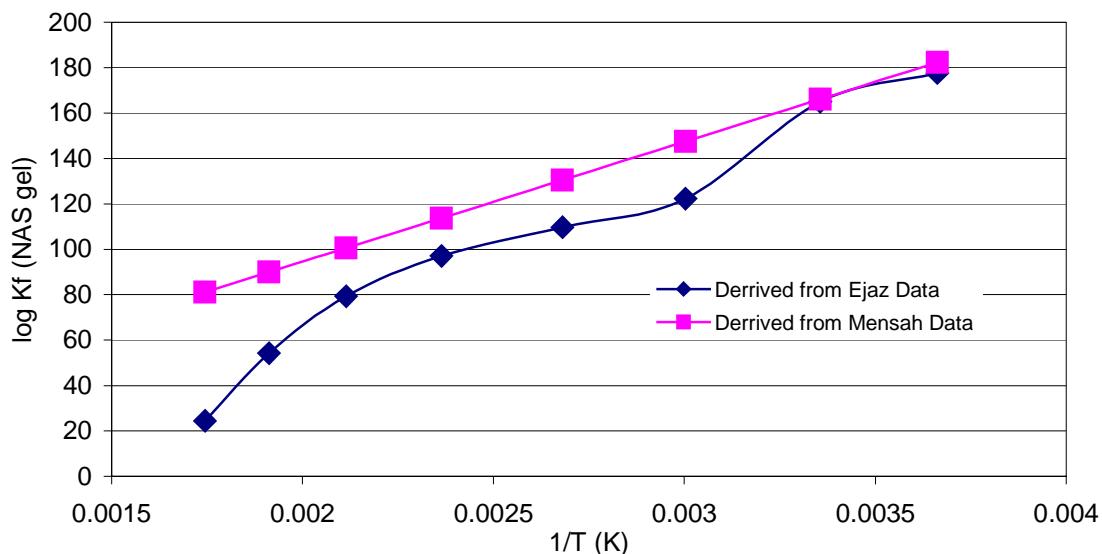
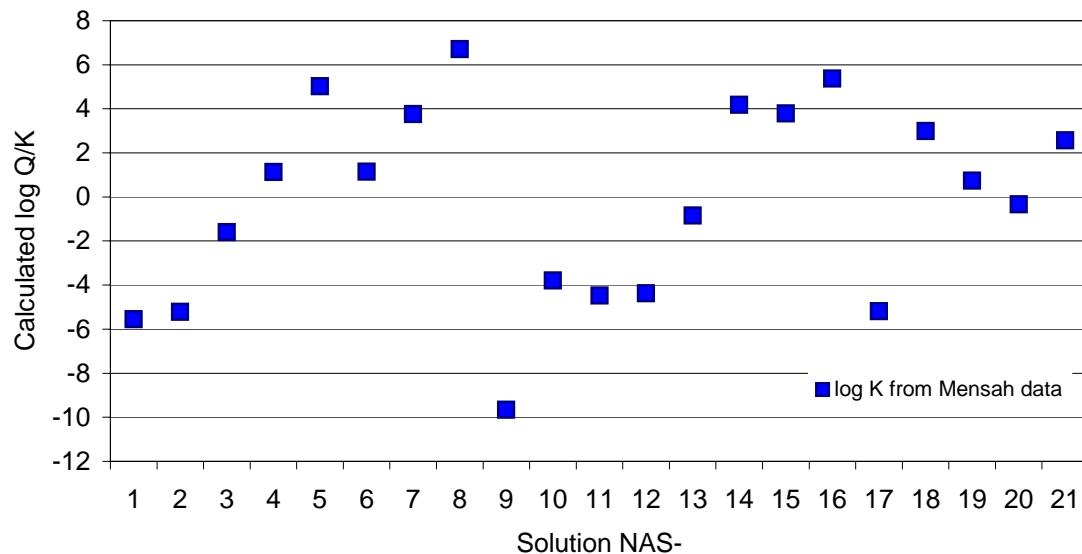
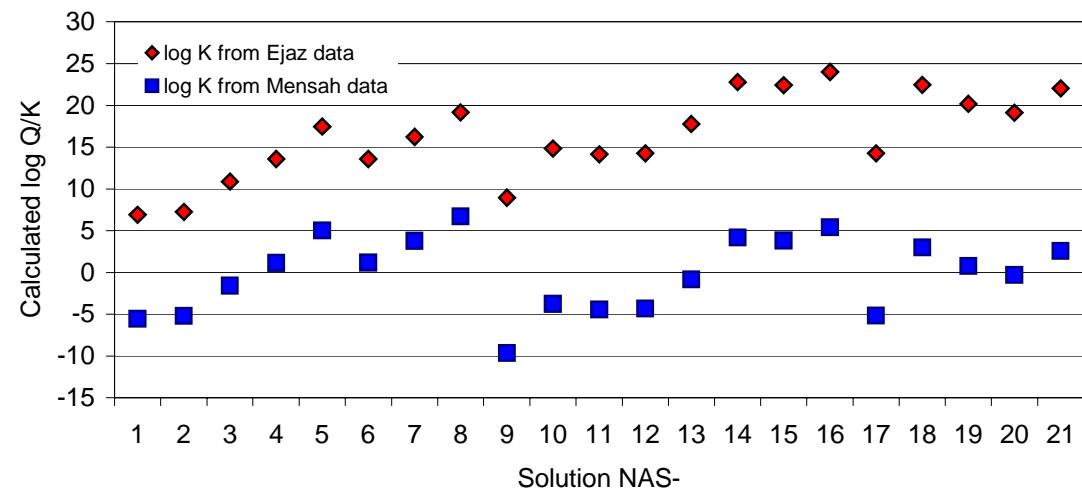


Figure B-3. Comparison of log K Values Used in GWB

From Figure B-1, it can be seen that the Mensah data predicts higher solubilities than the Ejaz solubility data. This is shown more graphically in Figure B-2. In this figure, calculated log Q/K values (using React.exe of GWB) are plotted for the solutions given in Table B-3. Because these solutions are saturated, their log Q/K values are, by definition, zero. However, in all cases, using the Ejaz derived log K values, the calculated log Q/K is much greater than zero. Using the Mensah derived log K values, there is an almost even scattering about log Q/K = 0. Thus, based on the Mensah solutions, using the Ejaz derived log K values tends to over estimate the saturation of these solutions relative to NAS_{gel} .



(a)



(b)

Figure B-4. Calculated log Q/K values for Mensah NAS_{gel} Saturated Solutions

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